

DEVELOPMENT OF AN ECONOMIC MODEL TO ASSESS THE FEASIBILITY OF
THE NUCLEAR INDUSTRY TO PRODUCE, HANDLE, AND OPERATE
COMMERCIAL FUEL WITH ENRICHMENTS GREATER THAN 5-WITH U^{235} FOR
PWRs IN THE UNITED STATES

By

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This work is dedicated to my wife, Karen.

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Abstract of Dissertation Presented to the Graduate School
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**DEVELOPMENT OF AN ECONOMIC MODEL TO ASSESS THE FEASIBILITY
OF THE NUCLEAR INDUSTRY TO PRODUCE, HANDLE, AND OPERATE
COMMERCIAL FUEL WITH ENRICHMENTS GREATER THAN 5 WTH U^{235}
FUELS IN THE UNITED STATES**

By
Robert M Smith

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The nuclear power industry in the United States is currently limited to 5-wth U^{235} fuel. Increasing the enrichment level would enable utilities to decrease the number of spent fuel assemblies, allow upgrades in reactor power, have more flexibility in fuel cycle lengths, and allow for the development of advanced fuel designs. Any increase in fuel enrichment requires an extensive analysis of the entire fuel cycle including mining, conversion, manufacturing, shipping, and storage of enriched fuel. The cost of the detailed analysis, licensing, and modifications to existing facilities or the construction of new facilities appears to justify the use of higher enriched fuel. The purpose of this study was to develop an economic model to determine the feasibility of using greater than 5-wth U^{235} commercial fuel. The study focused on evaluating typical fuel processing operations in enriched fuels on current facilities and cost penalties for the required modifications for processing, fabricating, shipping, and storage of higher enriched fuel.

The results of this study indicate that incentives to increase enrollments depended on the cycle length adopted. For reactors on an 18-month cycle there was little incentive to increase enrollment. However, potentially millions of dollars per year could be saved by reactors on a 24-month cycle if they increased enrollments up to 4.3-wt% U^{235} .

Larger incentives occurred for reactors using longer cycles.

The fuel-purchase interest rate was the dominant factor in determining the cost savings at using higher than 3.8-wt% fuel. Increases in interest rates alone could result in significant losses if higher enrichments were used. The other dominant factor affecting savings is the operations work charge. However, this cost appears to be stable with new facilities planned. Thus, although interest rates are volatile, the potential gain appears to outweigh any loss that could be seen by increased enrollments beyond the current bounding level of 4.3-wt% U^{235} for plants on a 24-month or longer cycle.

CHAPTER 1 INTRODUCTION

Motivation and Objective

In the United States there is a strong nuclear industry incentive for increasing fuel cycle enrichment for several reasons. First and most importantly, the industry, with the 3-wt% limit on fuel enrichment, is finding current fuel cycle flexibility greatly restricted. The spreading of reactor power at nearly every plant is creating a demand for even higher enrichment to increase the two year cycle length. Fuel cycles with higher burnups are desirable in order to decrease energy costs and the number of spent fuel assemblies. Higher burnups require higher enrichment than the currently licensed maximum of 3 wt% U²³⁵. Whether the industry is able to move to increased fuel enrichment beyond 3-wt% depends on the greatest concern on the cost of required equipment and process modifications to the current infrastructure to meet licensing requirements versus the economic benefits of the increased burnup and cycle length. Additionally, new incentives such as a reduced waste charge for higher burnups would also encourage higher enrichment to become a reality. An incentive directly associated with processing higher enrichment will prevent reactor fleet going to higher enriched fuels. There is an industry concern that the required modifications and licensing costs of higher enrichment may negate any fuel cycle advantages. This study is intended to address these questions.

The factors which have both economic and noneconomic measures to increase burnup are: 1) lower burning intervals as a result of lower refueling due to the longer cycle lengths that can be achieved from higher enriched fuels, 2) increase in availability and capacity factor due to longer cycles, 3) upgrade in reactor power, 4) reduced need for high cost of replacement power during refueling outages, 5) lower radiation exposure to operating personnel, 6) a decrease in the number of spent nuclear fuel assemblies, and 7) a decrease in expensive waste cost (SWU) loss resulting from disposition of weapons-grade uranium, and 8) improved fuel designs. Additionally, as a result of new and improved reactor designs being proposed as part of the Nuclear Engineering Education Research (NEER) and Nuclear Energy Research Initiative (NERI) research programs to improve reactor safety and performance, such as International Reactor Innovation and Reactor (IIR) and Pebble-Bed Gas-Cooled Fast Reactor (PB-GCFR), new core and fuel designs requiring higher burnups are being proposed.

Any search by industry to increase burnups will depend on the cost of changing the front end of the fuel cycle to higher burnups and its effects on the back end of the fuel cycle. The licensing process for higher burnups for fuel processing, transport, and handling will require sufficient criticality data in the higher burnup range to satisfy the Nuclear Regulatory Commission of the accuracy of the codes being used to quantify the process. Some economic disadvantages for going to increased burnups would be additional costs due to 1) required changes to the manufacturing process to ensure criticality safety, resulting in smaller batches, 2) a requirement for more personnel in the processing and handling equipment, 3) excessive licensing requirements for higher enriched fuel, 4) requirements for excessive modifications to fuel manufacturing

facilities, shipping containers, and utility fuel storage tanks to receive, store, and dispose of the higher enrichment fuel, and (3) licensing requirements for extensive reliability test data. For increased enrichment to be economically viable, the penalty for the processing, transporting, handling, and storage must be relatively small compared to current costs. The primary purpose of this research is to develop a model of the fuel cycle and examine the feasibility and the cost impact of increasing fuel enrichment to the range of 5 to 18 with U^{235} .

Previous Research

Currently there are only a few operating experiments in the five to ten weight percent enriched range [1]. There is one experimental set from Great Britain with seven percent enriched uranium as UO_2 rods, several sodium systems documented by the Japanese and some US metal-experiments starting at nine percent enriched and higher. There are five Russian UO_2 light water reactor experiments. The first experiment, LBL-COMP-TREHM-025, was titled "Uniform Water-Moderated Hexagonally Packed Lattices of Rods with $U(10\%)O_2$ Fuel" and composed of seven critical experiments for uniform fully flooded hexagonal lattices with pitch values of 0.7, 0.8, 1.0, 1.22, 1.45, and 1.652 cm. The second experiment, LBL-COMP-026, was titled "Partially Flooded Uniform Lattices of Rods with $U(10\%)O_2$ Fuel", and composed of six critical experiments for different levels of water on the lattice core. The pitch value of the lattice was 1.4 cm. Water levels were varied from 22.38 cm to 64.38 cm as the number of rods was decreased. The third experiment, LBL-COMP-028, was titled "Water Moderated Square-Packed Uniform Lattices of Rods with $U(10\%)O_2$ Fuel" and composed of two critical experiments for two square-pitched lattices of fuel rods. The pitch values of the lattices were 0.62 and 0.676

cm. The fourth experiment, LBU-COMP-025, was titled "Uniform-Moderated Hexagonally Packed Lattices of UO_2 THQOX Stainless Steel-Clad Fuel Rods" and composed of four fully flooded critical configurations with hexagonal lattices with pitch values of 7, 8, 10, and 12.2 cm. The fifth experiment, LBU-COMP-003, was titled "Uniform Water-Moderated Lattices of Rods with UO_2 THQOX Fuel in Range From 20 °C to 274 °C" and composed of nine critical experiments for uniform fully flooded hexagonal lattices with pitch values of 0.7, 1.4, and 2.832 cm at three different temperatures ranging from 20 °C to 274 °C for each lattice. All experiments were brought to a k_{eff} value of 1.000. The experiments were modeled in MCNP4a and ran 500 generations, dropping the first 50, 1000-iteration gas generations for a total of 450,000 iterations. The results of the MCNP models of the critical experiments with one standard deviation as well as the uncertainty of the benchmark models are given in the following tables.

Table 1-1 Results of MCNP4a sample calculations from LBU-COMP-THERM-003 (7)

pitch (cm)	k_{eff}	σ	Uncertainty of the Benchmark
1	1.0087	0.0011	0.0040
2	1.0055	0.0011	0.0040
3	1.0070	0.0010	0.0030
4	1.0060	0.0010	0.0037
5	1.0040	0.0011	0.0030
6	1.0050	0.0010	0.0040
7	1.0047	0.0009	0.0040

Table 1-2: Results of MCNP-6 sample calculations from LRU-COMF-TR0904-025 [1]

case no.	k_{eff}	β	Uncertainty of the Benchmark Model k_{eff}
1	0.0070	0.0011	0.0004
2	0.0000	0.0011	0.0000
3	1.0070	0.0011	0.0000
4	1.0070	0.0011	0.0000
5	1.0000	0.0011	0.0000
6	1.0000	0.0010	0.0000

Table 1-3: Results of MCNP-6 sample calculations from LRU-COMF-TR0904-026 [1]

case no.	k_{eff}	β	Uncertainty of the Benchmark Model k_{eff}
1	0.0000	0.0010	0.0000
2	1.0070	0.0010	0.0000

Table 1-4: Results of MCNP-6 sample calculations from LRU-COMF-TR0904-027 [1]

case no.	k_{eff}	β	Uncertainty of the Benchmark Model k_{eff}
1	0.0040	0.0010	0.0001
2	1.0000	0.0011	0.0000
3	0.0000	0.0011	0.0000
4	1.0000	0.0010	0.0000

Table 1-5: Results of MCNP-6 sample calculations from LRU-COMF-TR0904-028 [1]

case no.	k_{eff}	β	Uncertainty of the Benchmark Model k_{eff}
1	1.0000	0.0010	0.0000
2	0.0000	0.0011	0.0001
3	1.0044	0.0011	0.0000
4	1.0004	0.0010	0.0000
5	1.0000	0.0011	0.0000
6	1.0000	0.0010	0.0000
7	1.0000	0.0010	0.0000
8	1.0000	0.0010	0.0000
9	1.0044	0.0010	0.0000

The University of Florida with Sandia National Laboratories, Princeton, and Oak Ridge National Laboratory are currently setting up a critical experiment to obtain additional high-meshness-criticality data at k_{eff} with U^{235} as benchmark: the Russian and English data. Current computer codes such as MCNP and CASH/MINIMATE have been evaluated by the Nuclear Regulatory Commission and have been certified as being capable of calculating systems up to the five percent enrichment range. Further critical experiments in the future to test weight percent range will allow the benchmarking of these codes and validate them for higher enrichments.

The International Criticality Safety Benchmark Evaluation Project (ICSBEP) was initiated in October of 1982 by the Department of Energy Defense Programs Systems Engineering Division. This project is managed through the Idaho National Engineering and Environmental Laboratory (INELL) and involves nationally known criticality safety experts from Los Alamos National Laboratory, Lawrence Livermore National Laboratory, Savannah River Technology Center, Oak Ridge National Laboratory and the Y-12 Plant, Hanford, Argonne National Laboratory, and the Rocky Flats Plant. An International Criticality Safety Data Exchange component was added to the project in 1984. Representatives from the United Kingdom, France, Japan, the Russian Federation, Hungary, Korea, Morocco, Yugoslavia, Spain, and Israel are now participating in the project. The ICSBEP is an official activity of the OECD-NEA.

The work of the ICSBEP is documented in an International Handbook of Evaluated Criticality Safety Benchmark Experiments. Currently, the handbook spans over 22,000 pages and contains 80 evaluations representing 240 critical configurations. The

handbook is intended for use by university safety students to perform secondary evaluations of their educational techniques.

Description of the Nations Food Cycle

Mining

The first three steps in the food cycle, mining, milling, and conversion, will not be affected in a university safety course by an increase in equipment. However, in order to develop an economic model, they will be included to quantify the entire food process. Mining is higher-mechanistic than change the food requirements in relation to processing. Over half the world's production of uranium comes from Canada and Australia [2]. In 1950 33% of world production came from underground mines, but this dropped dramatically to 33% in 1999. From 2000, the percentage increased due to new Canadian mines. In 2009, production was as follows: open pit 34%, underground 66%, in situ leach (ISL) 14%, and by product 17%.

There are three methods used to mine uranium ore; open pit mining, underground mining, and solution mining (also called in-situ leaching). Back in 1960 about 97% of uranium ore came from surface mining. In open pit mining, holes are drilled to define the ore body. The topsoil is then removed and pit made so it can be used later to refill the pit. Waste rock and other overburden are removed by large trucks and loaded out by trucks. Technicians use G-45 counters to locate uranium ore. Once the uranium ore has been marked, the ore is dug using small front-end loaders and loaded into ore hauling trucks to be transported to the surface and stockpiled. The ore is then taken to the mill by "mobile" over-the-road trucks.

The ore in an underground mine may be below ground level by almost a mile. Both tunnels are cut into the ore deposits and the ore is removed, either on the surface or using carts, and hauled by trucks to the mill. Some disadvantages to this type of mining are as follows: part of the ore is left behind to support the roof of the mine, there is a potential for cave-ins, and radon gas (^{222}Rn) from the uranium ore imparts radon to water made in the ore processing activities of the mine, as well as radon discharges to minimize the radon/radon progeny dose. High ventilation flow, tens of cubic feet per hour, is required to reduce the radon to manageable levels. An advantage of underground mining is that the surface area over the mine is left undisturbed. The Environmental Protection Agency (EPA) limit on radon concentration has made underground mining in the U.S. totally uneconomical.

Today approximately 80% of the U.S. uranium production is from in-situ leaching (ISL). About 12 such ISL facilities exist in the United States. Of these, ten are licensed by the NRC as shown in Table 1.4 and the rest are licensed by Texas. The largest uranium production facilities in the United States are Cameco's South Forks and Highland facilities in Wyoming. The productive life of an individual ISL well pattern is usually less than 3 years, typically 4-16 months. Most of the uranium is recovered during the first 4 months of the operation. The most successful operations have achieved a total overall recovery of about 80% of the ore. This process is also used to mine copper and gold.

In a typical ISL well five holes are drilled about 30 ft apart [2]. The middle and outside holes (deposition wells) are used to inject the leaching solution (pregnant and acidified groundwater) close to the ore where it dissolves the uranium. If there is

significant column in the antibody (such as hexamine or glycine, sodium carbonate) loading must be used. Otherwise, solid (partially) loading is used. The other two buffer (external) solutions used to maintain up the dissolved ammonium solution and carry it up in a reverse ion exchange (IX) or liquid ion exchange (solvent extraction - (SX)) system (Figure 1-1). The choice is largely determined by the solubility of the groundwater. IX is better with high solubility. The ammonium is then stripped from the ion-exchange resin and precipitated chemically, usually with hydrogen peroxide. The ammonium slurry is decanted and dried to give hydrated ammonium peroxide ($\text{UO}_2 \cdot 2\text{H}_2\text{O}_2$) product. Low temperature drying will yield U_2O_8 .

Before the remaining process solution is evaporated, it is cryoprecipitated and if necessary exchanged with sodium acid to maintain a pH of about 2.5 to 3.5. Most of the solution is returned to the injection wells, but a very small flow (about 1%) is bleed off to maintain a pressure gradient in the well-field and also, with some solutions from surface precipitation, is treated as waste. This waste stream contains various dissolved minerals such as sodium, sodium and iron from the antibody and is transported into approved disposal wells as a depleted portion of the antibody. This bleed off process solution ensures that there is a steady flow into the wellfield from the surrounding aquifer and serves to correct the flow of many solutions away from the loading area.

Some advantages to in-situ loading are the elimination of the unloading, grinding, and loading of ore, transportation of large-scale excavations, a reduction of risks to miners from working underground, and a very small footprint (less than 1%) of the solubility of the ore relative the surface. One disadvantage is the potential for contamination of the groundwater.

Table 1-4 In-situ leach and conventional uranium milling facilities licensed by the NRC^a

Licensee	Site Name/Location
In-Situ Leach Facilities	
Copper Mountain, Inc.	Copper/CMB, Wyoming
Power Resources, Inc.	Highlands, Wyoming
Crow Butte Resources, Inc.	Crow Butte, Nebraska
Rio Algom Mining Corp.	Smith Ranch, Wyoming
Hydro Resources, Inc.	Crown Point, New Mexico
Power Resources, Inc.	East and North Forks, Wyoming
Conventional Uranium Milling Facilities	
International Uranium Corp.	Alpha-Rose, Utah
Atlantic Uranium Corp.	Greene, Wyoming
Western Nuclear Inc.	Spill Fork, Wyoming
Tennessee Valley Authority ^b	Paducah, South Dakota
Fullbrook Uranium Corp.	Lusk, WY, Wyoming
American Nuclear Corp.	ARC, Wyoming
Fullbrook Uranium Corp.	Shirley Basin, Wyoming
Potomac Electric Co.	Shirley Basin, Wyoming
Rio Algom Mining Corp.	Lusk, Utah
Eastern Utah Corp.	Highlands, Wyoming
Rock Creek Uranium Co.	Rock Creek, Wyoming
Rockwell Uranium Co.	Swanton, Wyoming
Potomac Resources Ltd.	Brookings, Utah
Homestake Mining Co.	Homestake, New Mexico
Kennecott Mining Co.	A, T-1, New Mexico
Rio Algom-Magma Ltd.	Alamosa, Utah, New Mexico
ORR Mining & Milling	Chauvin, New Mexico
Atlantic Richfield Co. ^c	Alamosa, New Mexico

^aPhysically, uranium mined, stored, and/or milled under general license to the U.S. Department of Energy for long-term sales.

Conversion to UF_6

The two processes used to convert the purified U_3O_8 are the dry hydrogenation process shown in Figure 1-2 and the wet solvent extraction process. In the dry hydrogenation process the U_3O_8 is first ground into a fine powder. Then the ground material enters a fluidized bed reactor where it is maintained at a temperature of 800 to 1200 °F and reduced by hydrogen. The resulting product consists mainly of uranium trioxide (UO_3) which is a brown oxide. The chemical reaction follows:



Next the oxide (UO_3) is passed to or two successive hydrofluorination fluidized-bed reactors, where interaction occurs with anhydrous hydrogen fluoride (HF) at a temperature of 500 to 600 °F. The chemical reaction that takes place is



The resulting uranium hexafluoride (UF_6) is green salt, is a crystalline solid with a high melting point (1500 to 1600 °F). It is isolated at high temperatures with fluorine gas to form UF_6 according to the reaction



Since some volatile impurities do follow the UF_6 , it must be further purified by fractional distillation, resulting in a purified liquid. This liquid UF_6 is distilled over 14-ton steel cylindrical reboilers, after cooling for 3 days, the UF_6 crystallizes [4]. The one conversion plant operating in the United States is the dry conversion plant owned by Honeywell International, Inc. and is located in Minnetonka, Illinois [6]. Other countries that have conversion plants are Canada, France, United Kingdom, China, and the Russian Federation.



Figure 1-2. Flow chart of the dry hydrofluoric process to convert U_3O_8 to UF_6 [3, 4]

The wet solvent extraction process (not used in the US) also uses solvents, hydrofluorination, and fluorination steps but they are preceded by solvent extraction to remove impurities. Thus, fractional-distillation is unnecessary since the UF_6 produced by the process is pure. This process is shown in Figure 1-3.



Figure 1-3. Flow chart of the wet solvent extraction-fluorination process to convert U_3O_8 to $UF_6(g)$.

UF_6 is a solid when vented at room temperature, within the transport container. During transport the pressure inside the container is kept below the outside atmospheric pressure. UF_6 is not flammable, not explosive and inert in dry air. It does, however, react with water. The humidity of the air is sufficient to cause it to undergo a rapid conversion into water soluble anhydrous fluoride (UO_2F_2) and hydrogen fluoride (HF). In the presence of excess water, hydrogen fluoride forms hydrofluoric acid, which is a deadly material and causes serious burns on contact. But even at very low concentrations, long before a possible health threat, HF is clearly visible as a gray-white fog.

Enriching

The isotope found in uranium which most readily splits (fissions) is a commercial nuclear reactor is U^{235} , but only 0.711-wt% of naturally occurring uranium is U^{235} . Commercial fuel is currently enriched to 3-5% U^{235} for use in commercial nuclear reactors. Natural occurring uranium contains three isotopes, uranium 234 (U^{234}), uranium 235 (U^{235}), and uranium 238 (U^{238}). Natural uranium contains 0.0044-wt% U^{234} which exists as part of the decay chain of U^{238} . The greater part of the radioactivity of uranium results from U^{238} . All three isotopes have identical chemical properties so the only way they can be separated is by their mass. U^{235} is heavier than U^{234} and U^{238} . Although the U^{234} is not desired in the enriched fuel, increased concentrations of it are a by-product of the enriching process.

The Paducah Gaseous Diffusion Plant in Paducah, Kentucky, is currently the only operating uranium enrichment facility in the United States [7, 8]. Owned by the U.S. Department of Energy, it is leased and operated by the United States Enrichment

Corporation, a wholly owned subsidiary of USEC, Inc. The plant was opened in 1952 as part of a U.S. government program to produce highly enriched uranium for military reactors and produce nuclear weapons. Enrichment at Paducah originally was limited to low levels, and the plant served as a "feed facility" (producing 3 to 4 wt% U^{235}) for other enrichment plants at Oak Ridge, Tennessee, and Portsmouth, Ohio, where the enriched uranium was processed to higher levels. That mission changed in the 1980s, when Paducah, along with its sister plant at Portsmouth began to enrich uranium for use in commercial nuclear reactors to generate electricity. The Portsmouth plant began production in 1954 and operated almost exclusively for national defense purposes until 1964. In July 2008, enrichment operations at Portsmouth were discontinued and consolidated at the Paducah plant which was upgraded to handle 5 wt% U^{235} . The Paducah plant currently has a design capacity of approximately 11 million separative work units (SWU) per year. The USEC is also currently planning construction of a new large enrichment plant with a partner and has exclusive rights to a new enrichment technology called MELIX that is being developed by Selen Systems Ltd. of Australia.

The selection of the Paducah enrichment facility for continued operation and production of higher weight dual represents a major challenge in the effort to license higher enriched nuclear fuel.

For the gaseous diffusion process, the transport container and the contained UF_6 are heated in a chamber just prior to loading into the plant. UF_6 is a solid at room temperature but becomes a gas when heated above 122 degrees Fahrenheit. First the pressure of the UF_6 vapor increases as it separates from the solid UF_6 at 145 °F. UF_6 becomes a liquid and the pressure continues to 1.1 bar. Before the UF_6 is piped into the

consider the pressure is lowered to 50 mbar (1/20 of normal atmospheric pressure). At this pressure, UF₆ remains gaseous within the paper even at environmental room temperature. The gas is forced through a series of porous membranes with microscopic openings (with a pressure differential). This process separates the lighter U²³⁵ and U²³⁸ isotopes from the heavier U²³⁸. Because the U²³⁵ and U²³⁸ are lighter and energy is conserved, they strike the barriers more often and thereby have a greater chance of moving through the barrier. As the gas diffuses, the isotopes are separated, increasing the U²³⁵ and U²³⁸ concentrations and decreasing the concentration of U²³⁸. The enriched and depleted UF₆ leaving the plant is solidified again to transport containers.

In May 1999 USMC decided to abandon the Advanced Vapor Laser Isotope Separation (AVLIS) enrichment process as its future technology. The AVLIS process used lasers passing through high-temperature uranium metal vapor to selectively excite the U²³⁵ isotopes, ionize it, and separate the U²³⁵ in order to produce enriched uranium. There were reports that although the physics of atomic laser separation was quite effective, the engineering obstacles associated with handling extremely corrosive metal may have been too difficult or costly to overcome. The decision to terminate AVLIS forced USMC with essentially two long-term technology options, the Selen process, under early-stage development in Australia, or centrifuge separation, long used by Russia and the European consortium Urenco. The Selen process also employs lasers to separate isotopes, but the feed is in molecular (UCl₄) form, which is relatively easy to handle at low temperatures and is the industry standard for enrichment. The effectiveness of this process at commercial scale is unknown at present.

On February 03, 2003, URSI submitted a license application for a gas centrifuge uranium enrichment test facility or "test cascade" [3]. The test cascade will be based on U.S. Department of Energy's (DOE) advanced gas-centrifuge technology. The URSI objective is to replicate the existing technology and reduce costs using advances in carbon fiber and other material and manufacturing technologies. The URSI program would be performed in the following three phases: (I) A demonstration program under DOE regulatory and regulatory control, (II) the test cascade phase, and (III) the commercial deployment phase.

The demonstration phase is intended to obtain detailed test data for the gas centrifuge machines. The test cascade phase is intended to provide reliability information on the machines auxiliary systems as it would be used in commercial operations. The test cascade, consisting of 340-centrifuges, will recycle the enriched and depleted uranium it produces. The only uranium withdrawal from the cascade will be in the form of scrap. In the commercial deployment phase, the commercial plant would have a capacity of 3.3 million SWU per year, with up to 10% enrichment. In a letter dated January 27, 2004, to the NRC, URSI Inc. stated its intent to submit a license application to the NRC in August 2004, for the American Centrifuge Plant (ACP), to be located in Phoenix, OH.

Lawrence Energy Services (LES) submitted a license application on December 12, 2003, to construct and operate a gas centrifuge uranium enrichment facility [4]. The LES partnership is made up of limited and general partners currently consisting of Unicom, Enbridge, Duke Power, Entergy, and Westinghouse. The partnership intends to use Unicom's multi generation gas centrifuge technology that is currently being used at

Europe. Currently, Ureco has a capacity of about 15 percent of the world's urethane market. Full capacity of 3 million FWH/yr is proposed to be in 2010 or 2011 depending on market demand. On September 2, 2008, LRS announced its final site selection to be Exton, New Mexico.

The gas centrifuge method was developed in Germany during the second world war, but its actual application only started in the 80s and 90s. The advantage over the gas diffusion method is that this technique separates isotopes more efficiently using less energy (one unit here is to be compared to a cascade to reach the same enrichment). However, a very high technology is necessary to manufacture the machines (precision and reliable bearings, corrosion resistant rotating parts of sufficient endurance). The gas centrifuge uranium enrichment process uses a large number of rotating cylinders in series in much amount, in an U^{235} isotope. These series of centrifuge machines, called trains, are interconnected in four cascades. The gas centrifuge is essentially a bowl, in which there is a rotor spinning round at a very high speed. The gas (UF_6) dissolved in the centrifuge is forced to spin by the rotor. Due to the centrifugal force the heavier molecules (those which include U^{238}) will accumulate near the wall of the bowl, while the lighter molecules containing U^{235} and U^{233} will stay closer to the center of the centrifuge. A diffusion plant typically uses 2,400 isotopic stages per separative work unit (SWU/SWU) while a modern centrifuge plant requires 40 to 100 SWU/SWU.

One other source of enriched uranium is the downblending of high-enriched weapons grade uranium. BWX Technologies (BWXT) and the U. S. Enrichment Corporation have a contract for BWXT to downblend 30 metric tons of high enriched uranium demand across to the civilian weapons program [11]. The downblending will be

performed over a six-year period and will produce low-correlated uranium suitable for use in light water reactors. The Nuclear Regulatory Commission (NRC) staff received license support on August 3, 2000, and a license to that subchapter dated December 18, 2001. The support was to amend their license to authorize the installation and use of the Metal Disolution Facility (MDF) for the dissolution of high enriched uranium (HEU) metal to support BWXT's downblending operations. The BWXT facility is Lynchburg, VA, is authorized to process nuclear materials for the fabrication and assembly of nuclear fuel components. The facility supports the U.S. naval reactor program, submarine research and university reactor components, and manufacturers compact reactor fuel elements. The facility also performs recovery of scrap uranium. Research and development activities related to the fabrication of nuclear fuel components are also conducted. The MDF will be used to receive, store, and dissolve HEU metal ranging from 28 to 92 percent U^{235} . The MDF will support after processing work and will be located within the Bay 15A, Mineral Access Area (MAAA). The building is already in place, so there will be no new construction in the BWXT site. The purpose of the MDF is to produce a homogeneous nitric nitrate solution with a uranium concentration of approximately 400 grams/liter (g/L). The first step in the MDF is the weighing out of an appropriate amount of HEU in a charging basket in a ventilated glove box. The charging basket is then transferred via a lift to a dissolver digester. Measured quantities of nitric acid and deionized water are added to the dissolver to dissolve the HEU. The resulting solution is then heated to approximately 140 degrees Fahrenheit and circulated until a homogeneous nitric nitrate solution is made. This homogeneous nitric/nitrate solution is then pumped through tubes into a gamma-monitoring column where the solution is circulated, weighed, and

simplified the U^{235} concentration. The solution is then transferred from a specially designed pump to one of five storage tanks where it is retained until required for blending with depleted or low enriched uranium.

A noted source of enriched uranium from the downsizing of high-enriched weapons grade uranium will be the Nuclear Fuel Services, Inc. (NFS) facility located in Evans, TN [12]. NFS is currently manufacturing high enriched nuclear reactor fuel at this facility. NFS is constructing a new complex at the Evans site to manufacture low-enriched nuclear reactor fuel. They also have requested authorization to their license to perform activities associated with the preparation of blended low-enriched uranium (LEU) from surplus highly-enriched uranium from the U.S. Department of Energy. These activities would be performed under a contract with Tennessee Valley Authority (TVA) to provide low-enriched fuel to be used in TVA's Browns Ferry Nuclear Plant in Alabama. NFS has requested authorization to perform dissolution of highly-enriched commercial/defense alloy and uranium metal and downsizing of the resulting solution into low enriched uranyl nitrate solution, manufacturing of more low-enriched uranyl nitrate solution at a new bulk storage facility on the NFS plant site, and authorization to perform conversion of the low-enriched uranyl nitrate solution into uranium dioxide powder.

Fuel Processing and Fabrication

Currently there are three U.S. fuel fabrication facilities which are capable of converting the UO_2 gas to solid UO_2 [13]. Fluoratomic ANP Fuelcoat Division, Inc. (formerly Nuclear Fuels Corporation) has its Engineering and Manufacturing Facility located in Richland, Washington. The Engineering and Manufacturing Facility holds a

license from the NRC (50NM-1237, Docket No. 76-1237) authorizing the following activities: manufacture of nuclear fuel, including all operational steps from UF_6 to UO_2 conversion through packaging finished fuel elements with uranium compounds up to 3 wt% U^{235} , all operational steps of dry UF_6 to UO_2 conversion and UO_2 powder preparation for uranium compounds up to 3 wt% U^{235} , storage of a phase series of dried constituents of uranium oxide (up to 3 wt% U^{235}) pellets that are externally free of significant contaminants, including those shipping containers and storage of containers of uranium compounds up to 3 wt% U^{235} (product, scrap and waste materials), outside storage of up to 3 wt% U^{235} enriched UF_6 cylinders (full and empty), outside storage of fuel UO_2 up to 3 wt% U^{235} , packed for shipment, and UF_6 (solid and in waste solution up to 3 wt% U^{235}) cylinder requalification activities. Uranium is processed using dry conversion as shown in Figures 1-4. The dry process changes UF_6 into a ceramic grade uranium dioxide powder in a single step by reacting it with steam and hydrogen in a kiln. The UF_6 is reduced to UF_4 by adding hydrogen in great excess, then water reacts with the UF_4 to produce UO_2 and HF. The UO_2 powder goes through a classifier and then into one of two storage hoppers. Two different constituents from the storage hoppers are mixed into the blender to make the required mixtures. The powder then flows through a horizontal, roll compressor, quad-roll and then into a 45-gallon storage drum. The storage drum is then transferred to the packaging area. The powder is compacted into a rotary press where it is pressed into cylindrical pellets and put into boats. The boats go through a walking beam screening system. The pellets are then ground to a finished size using a grinding wheel and placed on trays. The fuel pellets are shipped to Framatome's Lynchburg facility where they are loaded into ceramic tubes in which one end plug has

Westinghouse Electric Company LLC Columbia Fuel Fabrication Facility is located in Columbia, South Carolina. The Columbia Fuel Fabrication Facility (CFFF) is primarily engaged in the manufacture of fuel assemblies for commercial nuclear reactors. Two processes are installed at the CFFF for converting UF_6 to UO_2 powder: the ammonium diuranate (ADU) process and the integrated dry route process (IDR). However, the integrated dry route process has been mothballed. The CFFF has a current operating capacity of 3,700 metric tons UF_6 /yr or 1,150 metric tons heavy metal (per annum) and is limited to no more than 75,000 kg of U^{235} in any chemical nuclear physical form of uranium (except metal) that has been enriched to no more than 5 wt%. The CFFF holds a license from the U.S. Nuclear Regulatory Commission (NRC) (NRC-1103, Docket No. 30-111) authorizing, among others, the following activities: (1) Low enriched (less than or equal to 5 wt% by weight) U^{235} is received in the form of UF_6 . This portion of the plant receives the UF_6 containers which are stored outside of the plant until used. (2) UF_6 is converted to UO_2 powder. In this process the UF_6 containers are placed into a reactor where the UF_6 is subjected into the process line where it is dissolved in H_2O to form a UO_2F_2 solution which is mixed with NH_4OH to form an ammonium diuranate (ADU) slurry. The slurry is then centrifuged to separate the ADU and the wet ADU is then dried and calcined (heated at high temperature) to form UO_2 . This is further reduced with hydrogen to form UO_2 powder which is then milled and blended in preparation for the pelletizing operation. (3) The UO_2 powder is then pressed and sintered into pellets. (4) The pellets are loaded into fuel rods and sealed. (5) The rods are then loaded into fuel assemblies. Figure 1-5 presents a flow chart of the ADU process used by Westinghouse and Global Nuclear Fuel for UO_2 conversion to UO_2 .

Global Nuclear Fuel (Formerly General Electric) – Amerinc (GNF-A), LLC is located in Wilmington, North Carolina. The GNF-A license license from the NRC (SNM-0017, Docket No. 70-4113) authorizing it to conduct the following activities among other conversion of UF₆ to uranium oxides by the ADO process and the dry conversion process, operation of process technology for the purpose of converting UF₆ to UF₄ and other intermediate compounds by chemical and dry processes, storage of unenriched fuel assemblies and uranium compounds and minerals in areas arranged specifically for maintenance of integrity and radiological safety, and design, fabrication, and testing of uranium prototype processing equipment. GNF-A has a current operating capacity of 1,200 metric tons HM/yr (3,735 metric tons UF₆/yr) and is licensed to no more than 50,000 kg of U²³⁵ contained in-reactors (in any chemical and/or physical form) contained in no more than 3 wet U²³⁵. The location of GNF-A as well as the other major fuel cycle facilities are shown in Figure 1-6.

When the fuel fabrication facility is finished assembling the fuel assemblies, they are shipped to the reactor. Typically, two fuel assemblies are stored in a transport cask, and are shipped by truck, with each truck carrying 4 casks.

Exterior Storage and Fuel Disposal

When the utility receives the fresh fuel assemblies they are inspected and moved into the spent fuel pool for temporary storage until they can be placed into the reactor. Anywhere from one-fourth to one-half of the total fuel load is removed from the reactor every 12 to 24 months and replaced with fresh fuel. The spent fuel is placed into a spent fuel pool for temporary storage. The spent fuel pool must always have the capacity to offload the entire reactor core. The pool is a concrete reinforced structure designed to



Licensee	Location
Uranium Fuel Production Facilities	
Global Nuclear Fuel Services, LLC	Wilmington, North Carolina
Westinghouse Electric Company, LLC	Columbia, South Carolina
Wuclear Fuel Services, Inc.	Brainerd, Tennessee
Prism Uranium ASP, Inc.	Lynchburg, Virginia
BECH Technologies, Inc.	Lynchburg, Virginia
Prism Uranium ASP, Inc.	Richland, West Virginia
Uranium Hexafluoride Production (Enrichment) Facility	
Urocyte International, Inc.	Petersburg, Illinois
Gaseous Diffusion Enrichment Facilities	
B G Enrichment Corporation	Paducah, Kentucky
B G Enrichment Corporation	Paducah, KY

Figure 1-4: Locations of major fuel cycle facilities (4)

withstand various events and with a minimum steel liner to prevent leakage. Approximately 23 feet of water is contained in the pool above the level of fuel to provide radiation shielding. A typical cooling system has two pumps and two heat exchangers. Both the suction and discharge of that system are arranged rather high in the pool or with some anti-siphon features, so that the water in the pool cannot be drained out down to the level where the fuel is.

An important safety function of the spent fuel pool is submersion control. This is controlled by the geometry itself, separation of the fuel assemblies by analysis of the reactivity of the individual fuel assemblies and by fixed neutron absorbing material which in some designs is attached to the fuel rack itself. Submersion is not used to guarantee subcriticality of the fuel in the rack itself but it provides additional margin for conditions such as inadvertently loading the fuel in an unexpected arrangement or condition, for example, if a fuel assembly were to be dropped and be lying across the top of the racks, that would be a most adverse configuration. In the past it was necessary to show that the fuel remained 3 percent subcritical with no credit for boron. Today, boron is credited so that the pool only needs to remain subcritical. It must be shown that if there were loss of boron in the pool, the fuel would remain subcritical. Such an event could be caused by putting fire water or service water or some other water into the spent fuel pool.

A second option for spent fuel storage is dry cask storage. This storage can be used to increase spent fuel storage capacity. Dry cask storage allows spent fuel that has already been cooled in the spent fuel pool for at least one year and usually five to ten years to be transferred by inert gas inside a container called a cask. The casks are typically steel cylinders that are either welded or bolted closed. The spent fuel water

provides a leak-tight containment of the spent fuel. Each cylinder is surrounded by additional steel, concrete, or other material to provide radiation shielding to workers and members of the public. Some of the cask designs can be used for both storage and transportation.

There are various dry storage cask system designs. With some designs, the steel cylinder containing the fuel are placed vertically in a concrete vault, other designs orient the cylinders horizontally. The concrete vaults provide the radiation shielding. Other cask designs orient the steel cylinder vertically on a concrete pad at a dry cask storage site and use lead metal and concrete outer cylinders for radiation shielding. The first dry storage installation was licensed by the NRC in 1966 at the Samp Nuclear Power Plant in Virginia. Spent fuel is currently stored in dry cask systems at a growing number of power plant sites as shown in Figures 1-3, and at an interim facility located at the Idaho National Environmental and Engineering Laboratory near Idaho Falls, Idaho. A listing of NRC approved designs for dry spent fuel storage is shown in Table 1-3.

The current proposed US strategy for final disposal of spent nuclear fuel is to store the spent fuel assemblies in Yucca Mountain. A 1 mile-wide, 600 ft deep cavern in the fuel waste is being leased on the mountain to pay for the eventual long term storage. The U.S. Department of Energy's (DOE) high-level radioactive waste repository is not expected to begin receiving spent fuel until approximately 2015, at the earliest.

Reprocessing of spent fuel in the United States is not a viable alternative at this time since there are no operating or planned commercial reprocessing facilities in the United States. Therefore, spent fuel would have to be shipped to an overseas facility for reprocessing. However, this approach has never been used and it would require approval

by the Department of State as well as other entities. Additionally, the cost of spent fuel reprocessing is not offset by the salvage value of the residual plutonium and uranium. Thus, reprocessing represents an added cost over disposal.

Table 1-7 Day spent fuel storage designs approved by the NRC for general use (34)

Vendor	Storage Design Model	Certificate of Compliance Issue Date	Expiry
General Nuclear Systems, Incorporated	CASTOR 6C1	08/11/2006	12/1/2008
Westinghouse WND/6	MC 12	08/11/2006	12/1/2005
NAC International, Inc.	NAC S/T	08/11/2006	12/1/2007
NAC International, Inc.	NAC-CBR S/T	08/11/2006	12/1/2007
Transnuclear, Incorporated	TR-24	11/04/1993	12/1/2005
BNFL Fuel Solutions Corp.	WBC 24	03/03/1993	12/1/2007
Transnuclear West, Inc.	BRIDGEPORT BURNING 24P NACORIS 12P	04/26/1993	12/1/2006
Palfric International	HI-STRAK 100	10/04/1999	12/1/2008
Palfric International	HI-STORM 100	09/11/2000	12/1/2010
Transnuclear, Inc.	TR-32	04/07/2000	12/1/2011
NAC International	NAC-LWB	11/06/2000	12/1/2010
NAC International	NAC-MPC	04/06/2000	12/1/2009
BNFL Fuel Solutions	Autonomous	03/07/2000	12/1/2008
Transnuclear, Inc.	TR-34	05/06/2000	12/1/2007



Figure 1-7 Locations of independent open fire alarm monitoring stations [11]

CHAPTER 2 DETERMINATION OF CRITICALITY LIMITS

Overview of Modeling

In this report, the entire fuel cycle was studied and evaluated for effects of going to higher enrichment for secondary safety. The secondary constraint is considered the limiting constraint for the estimation of enrichment greater than 3 wt% ^{235}U . Traditionally in secondary safety analysis, natural configurations have been considered safe from a criticality standpoint if the predicted value of k_{eff} is less than 0.95. Two standard secondary codes, MCNP6a2 and MCNP5 were used [14]. MCNP is a general purpose Monte Carlo N-Particle code that can be used for neutrons, photons, electrons, or mixed neutron/photon/electron transport, including the capability to estimate eigenvalues for critical systems. The code treats an arbitrary three-dimensional configuration of materials in geometric cells bounded by first and second-degree surfaces and some special fourth-degree surfaces. Freeform or multipatch cross-section data are used. For neutrons, all reactions given in a particular cross-section evaluation (such as ENDF/B-VI) are accounted for. Thermal neutrons are described by both the free gas and $(\lambda/\lambda_0)(E_0/E)$ models.

To carry out this study criticality models of fuel processing equipment, fuel manifold, cladding container, and fuel storage were developed using MCNP. Enrichments of 3-wt% to 33-wt% ^{235}U in increments of 1 wt% were examined. The results from these analyses were used to judge equipment priorities in each report of the

nuclear fuel cycle for increasing the allowable U^{235} wt% in each increment. The economic problems were assigned the restrictions or costs incurred at each point in the fuel cycle in order to maintain consistency safety.

U^{235} HSL Shipping Container

The initial fuel processing operation is the receiving of the uranium either as a *gaseous diffusion plant* or a *gaseous centrifuge plant*. The uranium is processed as UF_6 and is stored and shipped in the commercial nuclear fuel processing facilities as UF_6 . Commercial fuel fabrication facilities typically receive UF_6 in 200 cylinders. A 200 cylinder has a nominal diameter of 30 inches and a nominal length of 81.5 inches [11]. A steel skirt extends 5 inches from the cylinder head to protect the cylinder and the valves. Only 76 inches of the 81.5 inch nominal length of the cylinder contains UF_6 . For the purposes of this analysis, the cylinder was modeled as a right circular cylinder. The maximum permissible cylinder fill weight of UF_6 is 3,277 kg. More material can be physically placed in the cylinder during filling, but adding material beyond that weight limit assumes the possibility of hydraulically rupturing the cylinder on subsequent refilling. During the withdrawal of UF_6 , opening procedures require that condenser pressure and temperature be less than those of saturated UF_6 to ensure that vapors are not present. The gaseous diffusion process consistently produces high-purity UF_6 (\geq 99.3 weight percent UF_6). For nuclear consistency safety purposes, all vapors are conservatively assumed to be UF_6 . Assuming that UF_6 is 99.3 pure weight percent and that the other 0.5 weight percent is H_2O , an H_2O atomic mass of 0.001 is obtained.

A worst case scenario was modeled in which solid UF_6 , moderated by HF (at an H_2O ratio of 0.000) was filled to the top of the 30ft cylinder with a 2 foot water reflector surrounding the cylinder. Further models were developed of an infinite array of 30ft cylinders, stacked one high with interstitial water and a concrete reflector to simulate conditions such as those in a spray-dry system. Various moderators consisting of air, water, or water vapor of varying densities were modeled. Models were also developed of an infinite horizontal array, stacked one high in a rectangular pile, placed on a 1 ft concrete slab and are shown in Figure 2-1.

Figure 2-2 shows the results of the infinite transverse pitch array of 30ft cylinders. The most limiting moderator was the 0.2 and 0.3 g/cc vapor cases. At lower enrichments (below 10 w/o U^{235}) the 0.2 g/cc case is more limiting. At the higher enrichments the 0.3 g/cc case becomes more limiting. These cases show that the 30ft cylinder would be limited to varying enriched UF_6 of 10-w/o or less of U^{235} which would be enough for the commercial gas centrifuge process conducted the United States Enrichment Corporation (USEC) plans to develop and build. The results of all MCNP2 calculations of models of the 30ft cylinders are presented in Tables B-1 through B-13 of Appendix B.

Wet Processing of UF_6 to UO_2

Typical dimensions for plant processing equipment, which will ensure nuclear security safety in the wet processing of up to 20 w/o U^{235} uranium regardless of the values of any other parameters in the system, were modeled. A pipe was modeled conservatively as a cylinder of infinite length. Further conservatism was introduced by assuming that the pipe was surrounded by an insulator thickness of 1 foot of water, providing moderation.



Figure 3-1 Side view of irregular patch array of UFs filled HD concrete

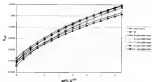


Figure 3-2 Results of MCNPv2 calculations of UFs in HD cylinders in a irregular patch, completely filled, array on a concrete slab

and reflection of neutrons that leak out the side of the pipe. The assumed assumed water homogeneous slurry of $\text{LiO}_2 + \text{H}_2\text{O}$ in a system which does not present structural limitations, a slurry of uranium dioxide provides maximum reactivity [14]. The values of k_{eff} for 4, 8, and 16 inch (where applicable) diameter schedule 40ST SS piping of infinite length surrounded by one foot of water were calculated.

Tables B-28 through B-31 of Appendix B present the cases analyzed using MCNP4C2. The results show that without moderation control, wet processing of UF_6 is viable using standard 4" diameter piping, for concentrations from 5 to 30-wt% U^{235} range. Wet processing of concentrations of greater than 30-wt% range should limit all piping to standard 4" diameter piping.

Dry Conversion Processing of UF_6 to UO_2

In the dry process, UF_6 is changed into a smaller grade uranium dioxide powder in a single stage by mixing it with steam and hydrogen in a kiln. An original KENO model of the kiln used at a vendor site was obtained (Calver-Manning, Fennema, ANP, personal communication, March 11, 2002). Using this as a base model, MCNP models were developed. The MCNP models consisted of an upper section of 2.122 g/cc uranium-water slurry with the dimensions of 11.43 cm by 76.20 cm by 121.91 cm. The lower section was 11.43 cm by 84.34 cm by 196.11 cm and filled with a denser 2.8175 g/cc uranium-water slurry. Both sections were surrounded by 5.431 cm thick insulation, and placed into a "box" of moderation of the dimensions 46.8 cm by 115.24 cm by 330.47 cm. Various moderators consisting of air, water, or water vapor of varying densities were included in order to determine the optimum moderation. Insulation 11-cm thick around the moderator was modeled as a 0.2085 g/cc mixture of 51.5% SiO_2 and 48%

Altho: The results shown in Figure 3-3 and Tables B-32 through B-35 of Appendix B indicate that the current hole would be lowered to approximately 8-inch U^{crit} . An increase of roughness beyond this point would require replacement of the current hole with one that possessed smaller geometric dimensions in order to ensure criticality safety.

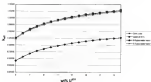


Figure 3-3 Results of MCNP4c2 models of a dry cask vent hole

Model of the Caskcase

An original KENO model for the caskcase from a representative vendor (Calvert Mission, Framingham, MA) (personal communication, March 13, 2002) was obtained and an MCNP model was developed using 5-wt% U^{235} fuel and an accident scenario with water moderator. The caskcase was modeled as a cylinder 618 cm in length with a radius of 12.7 cm containing a 1.014 g/cc uranium-water slurry. The caskcase wall was composed of 7.87 g/cc carbon steel and was 1.27 cm thick. The cylinder was surrounded by a 48.26 cm by 48.26 cm by 418 cm shell, the upper half of which was filled with air and the lower half modeled as a 1.222 g/cc uranium-water slurry. Two 7.62 cm thick basins were modeled on the front and back of the caskcase and were composed of 8.1280

g/cc mixture of 51% FeO_3 and 49% Al_2O_3 . This same mixture at a density of 5.0961 g/cc was used as the model in the 13.475 cm thick insulation around the caliche. An additional 30 cm of insulation was added to simulate worst-case conditions. No further models were developed as this case showed that the current caliche was at the 8.53 kg limit under worst-case conditions. This lesson was confirmed with discussions with the caliche manufacturer (D. Robinson, ALUCHEM, personal communication, May 20, 2004) and it is concluded that the caliche model here is replaced with another model with a smaller diameter (8 or 9 inches as opposed to the current diameter of 10 inches) to ensure critically safety.

45-Gallon UO_2 Powder Storage Drums

Once the UO_2 is converted to powder it is typically stored in 45-gallon containers until it is used to form pellets. These drums are modeled as a cylinder with an outer radius of 28.375 cm, a height of 86.638 cm and with 0.1431 cm thick stainless steel walls, bottom, and lid (Calvin Manning, Fluorocore ANP, personal communication, March 13, 2004). The powder in the barrels was assumed to be composed of 6.3 g/cc UO_2 and 0.2055 g/cc water. Models were developed of a single barrel completely filled with powder and reflected on all sides by water at 28 °C. Additional models were developed of an infinite array of these barrels of one vendor design consisting two rings of 8 UO_2 powder rods with one powder rod in the center and is shown in Figure 3-6. The powder rods were 2.2114 cm in radius with 0.1621-cm thick air gap inside a 8.1450 cm thick steel clad. Various moderator zones consisting of air, water, or water vapor of varying duration were modeled in order to define the optimum moderator.

The results of the infinite array of UO_2 filled 45-gallon containers are shown in Figure 3-5. The most limiting mechanism was the O₂ gas vaporizer. These results show that the quarter 45-gallon container would be limited to enriched UO_2 of 11-wt% or less of U^{235} which is sufficient for the UMFC commercial gas centrifuge enrichment facility. The results of the MCNP6 calculations of models of the 45-gallon containers are presented in Tables B-16 through B-23 of Appendix B.



Figure 3-4 Top view of one element of an infinite array of UO_2 filled 45-gallon containers showing corner and two rings of poison rods

Molybdenum Pellet Boats and Storage Shelves

Once the UO_2 powder is formed into pellets, they are placed into molybdenum boats and go through a sintering furnace. Afterwards the boats are typically placed on stainless steel shelves. An original KENO model of the molybdenum boats used by a representative vendor was obtained (Chris Manning, Trane name AMP, personal communication, May 17, 2006). Using this as a base model, MCNP models were developed. The first models developed were single boats filled with UO_2 pellets and water at 28 °C. Two sets of elementary models were developed to bound the potential U^{235}

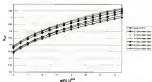


Figure 3-3 Results of H&N/F&2 models of infinite array of UO_2 -filled 40-gallon containers

ratio. One set assumed 97% water and 93% UO_2 by volume, the maximum amount of UO_2 that would be able to be put into a heat-generating cylindrical pellet. The 2nd set of models assumed a 2 to 1 ratio of water to UO_2 . Results show that the 2nd set of models are more limiting for the single heat case. Next, a model was developed using a 2 to 1 ratio of water to UO_2 of an infinite array of tests stacked one high on a 1/4 inch stainless steel shelf, with 1 foot of water or water vapor moderator on all sides, with reflective boundaries. The results shown in Figure 3-4 and in Tables 3-13 through 3-17 indicate that the tests would be limited to approximately 13-wt% UO_2 . This is greater than the 12-wt% limit of the USBC commercial gas centrifuge uranium enrichment in development.

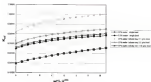


Figure 3-4: Radius of MCNP6d calculations for multiphysics pellet bins

Single Assembly Models

After the UO_2 powder is formed into pellets, these pellets are loaded into rods and inserted into assemblies. MCNP decks of single 15x15 and 17x17 fuel assemblies were developed. For both assembly types the maximum theoretical UO_2 density of 18.96 g/cc was used. For the 15x15-assembly, the fuel pin outer diameter was assumed to be 9.1432 inches, with an inner clad diameter of 8.17 inches, outer clad diameter of 9.014 inches, and a pin pitch of 9.583 inches [11]. The 17x17 assembly was modeled with a fuel pin diameter of 9.7332 inches, inner clad diameter of 8.506 inches, an outer clad diameter of 9.572 inches, and a pin pitch of 9.583 inches. Both models used an active fuel length of 144 inches and enveloped the single assemblies inside a right circular cylinder of 29.6 inches with a radius of 14.8 inches and a height of 144 inches. In single assembly runs it was shown that the 15x15 assembly is slightly more reactive than the 17x17 assembly so all later models used the 15x15 assembly. Further models were developed with addition of random material rods or GdPEAs placed in the guide tubes. Single assembly

must show that assemblies must have some sort of acceleration control above 5-m/s U^{ref} . This would require either the addition of steel rods, BFRAs, or some other structure when the assembly is accelerated, during transportation, and placement into the spent fuel pool. As shown in Figure 2-7, the addition of steel rods would allow assemblies up to approximately 6.5-m/s U^{ref} and BFRAs would increase that limit to approximately 13-m/s U^{ref} . The results of all MCNP4c calculations of models of single assembly models are presented in Tables B-43 through B-56 of Appendix B.

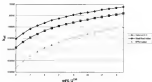


Figure 2-7 Results of MCNP4c models of a single 15x15 assembly in water at 20°C

Frank Fuel Stopping Casks

The assemblies are slow stopped from a reactor to the cooling plants at stopping racks. Using the known specifications of the Model B package [15, Barry Huxley, Transatomic AMP, personal communications, January 27, 2004] infinite arrays of stopping racks were modeled. These racks were modeled as a cylinder with an outer radius of 58.374 cm, a height of 540.347 cm and wall 8.3115 cm thick stainless steel walls, bottom, and lid. Two assemblies were placed in the center of the barrel on a steel plate,

with two horizontal steel plates supporting them. The distance between the two horizontal steel plates is 5.12 cm. The cables were reflected on four sides with 60% cut of water above and below the cables. This model is shown in Figure 2-4. In single assembly case it was shown that the 15a15 assembly is slightly more reactive than the 17a17 assembly so all core models used the 15a15 assembly. Various moderation ratios consisting of air, water, or water vapor of varying densities were modeled in order to define the optimum moderation. The results of the infinite array of shipping containers are shown in Figure 2-5. The most limiting moderator was the water at 30°C case. These cases show that the selected risk would be limited to enriched ^{235}U of 4-wt% or less of 10^{23} . In addition, models were developed with stainless steel rods or BFRAs placed on the guide tubes. The results of these runs, shown in Figure 2-10, indicate that the addition of steel rods would allow shipping of fuel enriched up to 4-wt% 10^{23} and BFRAs would increase that limit up to 15-wt% 10^{23} . The steel plate supporting the two assemblies and the two horizontal plates supporting them allow for a less critical situation than one assembly by itself with no plates present. The results of all MCNP5 ray calculations of models of the Model B assembly shipping container are presented in Tables B-61 through B-75 of Appendix B.

Spent Fuel Pool

A typical spent fuel pool limiting configuration for Black Rail bundles [26] was modeled as shown in Figure 3-11. The fresh fuel locations, shown in gray, are modeled as the 15a15 assemblies in the previous report. Each assembly location is surrounded by 0.2821 cm of water in a 0.1981 cm thick steel sheath. Each sheath is separated by 2.429 cm of water. The entire spent fuel pool rack was surrounded by 68.94 cm of water. Two criteria are typically used in criticality safety analysis for the spent fuel pool. The first



Figure 2-4 Top view of one channel of an infinite array of 15x15 assembly shipping containers

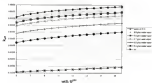


Figure 2-5 Results of MCHPac2 models of infinite array of 15x15 assembly shipping containers in various water depths and air

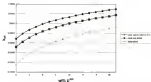


Figure 3-10 Results of 3D-CFD models of infinite array of 15x15 assembly stripping containers at water at 30 °C, with DPLAs, steel, and/or resin

so that the k_{L0} must be less than 1.8 with no soluble boron. The second is that k_{L0} must be less than 1.93 with soluble boron. The spent fuel pool was modeled with steel without 300 ppm boron and also with and without the addition of DPLAs to the fresh fuel assemblies. The results of the spent fuel pool calculations are shown in Figure 3-12 and Tables B-248 through B-252 of Appendix B. For the 1st criterion, the spent fuel pool would be limited to 4-wt% U^{235} or less without the use of DPLAs. The 2nd criterion limits the pool to 9.5-wt% U^{235} or less. The addition of DPLAs would increase the limits of fresh uranium to 20-wt% U^{235} .

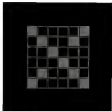


Figure 2-11 Top view of MCNP5 nps model of a spent fuel pool

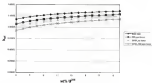


Figure 2-12 Results of MCNP5 nps models of a spent fuel pool

CHAPTER 3 BATCH AND BURNUP CALCULATIONS FOR SPECIFIC CYCLE LENGTHS

CASMO-3 and CASFRD-4 Codes

In order to develop a model to be used to estimate the feasibility and the cost impact of increasing fuel enrichment in the range of 3 to 18 wt% ^{235}U , burnup and batch sizes for each enrichment and cycle length must be calculated. These variables are used in determining the final fuel-cycle costs. A batch is a group of assemblies, composed of the same fuel type and enrichment, entering and leaving the reactor at the same time. Burnup is the power produced per unit mass of fuel used and for the purposes of this analysis is expressed as gigawatt-days per metric ton of uranium (GWd/MTU).

Discharge burnups for the various fuel cycles were determined using the CASMO-3 and CASFRD-4 codes. CASMO-3 is a two-dimensional transport theory code used for burnup calculations on BWR and PWR fuel assemblies [21]. CASMO-3 calculates the two-dimensional neutron and gamma flux distributions and isotopic compositions versus burnup within fuel assemblies using high order transport theory models. The program calculates the nuclear properties of the fuel in the core in order to generate continuous data banks to be used by three-dimensional core simulators. CASMO-3 can also be used for sensitivity analysis and the calculation of isotopic inventory as depleted fuel.

The CASFIND-4 code was developed by Mr. M. Wilson as part of his master's work at the University of Florida. CASFIND-4 was written in FORTRAN-77 and has been designed to extract information from CASMO-3 outputs and to perform various calculations to determine discharge burnups, the time that it is on core, average width of spent fuel, and fuel cycle costs. The program utilizes a technique that uses the Least Mean Square Method to determine the quadratic equation that represents the behavior of k_{eff} vs. burnup. The method of Least Mean Squares states that the line represented by the equation should be fitted through the given points so that the sum of the squares of the distances of those points from the line is a minimum [21]. The following equation [22] is used:

$$\text{minimize cost is the } \sum_{i=1}^N (y_i - (a_0 + a_1x_i + a_2x_i^2))^2 \quad (3-1)$$

The model used to represent the relationship of k_{eff} vs. burnup is a quadratic equation of the form:

$$k_{eff} = a_0 + a_1^*B + a_2^*B^2 \quad (3-2)$$

where a_0 , a_1 , and a_2 are weighting functions and B is the burnup.

Three equations are generated by setting the first derivatives equal to zero with respect to the weights. These three equations are then solved with Cramer's rule to determine the coefficients a_0 , a_1 , and a_2 . The discharge burnup is then calculated using the fitted equation.

Block and Burnup Results

A typical 13x17 PWR assembly with varying enrichment from 3.0 to 19.0% U^{235} was modeled and entered into CASMO-3. The outputs from CASMO-3 were entered into CASFIND-4 to determine core burnups and cycle lengths for the fuel. CASFIND-4

only determines the burning and cycle length for a whole number of batches. The burning and cycle times were determined for the varying randomness and are presented in Figures 3-1 and 3-2. These data were entered into EXCEL, and linear interpolation was used to determine the number of batches required and the corresponding burning. Two sets of outage lengths were used, a 15-day outage length, typical of Indian outages and a 30-day outage, which is the current average. All PWR's in the United States are currently either using the 18 or 24 month cycle. The shutdown time is determined in accordance with the replacement power costs being the cheapest. Data was calculated for the 12, 18, 24, 30, 36, and 42 month cycles. The cycle length includes the outage time. The results of these calculations are presented in Figures 3-1 and 3-2 and in Appendix D in Tables D-1 through D-6. These results will be used to determine fuel cycle costs.

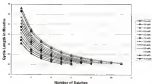


Figure 3-1 Cycle length vs. number of batches results from CASMO-3 and CASPER-3

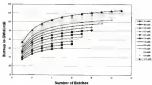


Figure 3-2 Runup vs. number of swatches results from CASMO-3 and CASMO-4

CHAPTER 4 ECONOMIC MODEL OF THE NUCLEAR FUEL CYCLE

Overview of Economic Model

In order for increased enrichment to be economically feasible, the increased costs due to licensing, modification and replacement of equipment due to reliability issues must not outweigh the potential cost savings from higher burnups, smaller batch sizes, and construction of fewer dry cask storage units. The effects of potential variations in individual fuel cycle costs or potential cost savings or losses must be examined. An economic model was developed to determine feasibility and the cost impact of increasing fuel enrichments in the range of 3 to 10-wt% U^{235} under a base set of conditions. The model has the capability of varying the individual fuel cycle costs to determine not only if increasing enrichment is viable under current economic conditions, but also under any combination of increases or decreases of individual fuel cycle costs or interest rates. The fuel cycle costs included the following: 1) The natural uranium feed charges, 2) the enrichment charge, 3) the separative work charge, 4) the fabrication charge, which includes a charge for the inclusion of stainless steel rods in the guide thimble at concentrations greater than 8-wt% and the replacement of the steel rods with DIFILs at concentrations greater than 8.5-wt%, 5) a charge for replacement of the column at enrichments greater than 5-wt% and the replacement of the dry cask service life at enrichments greater than 8-wt%, both replacements are required due to reliability issues documented in Chapter 2. If a cost penalty for licensing the 10% enrichment, the

filtration facility, and the spent feed cost for enrichments greater than 1-wt% U^{235} feed, T) the cost of filtering the mixed feed spent, R) an in-cost capital cost charge, N) a charge for the conversion of dry dock storage tanks for spent feed assemblies, E) the current $\frac{\text{mill}}{\text{kW} \cdot \text{day}}$ fee for final feed disposal cost, and U) replacement power and enrichment costs during outage times

Start-Cost Calculations

The start-(present and) cost (S_0) includes the cost of the core, conversion, enrichment, fabrication (including a cost penalty associated with the addition of stainless steel or Inconel probe rods to reflect probability issues of assemblies with greater than 1-wt% U^{235} feed), the costs of new equipment and licensing for higher enrichments at the fabrication facility, and the cost of mixed burning. The nuclear weapons base feed cost was set to \$40 per kilogram of uranium [26]. The total uranium feed charge (TDFC) or $\frac{\text{mill}}{\text{kW} \cdot \text{day}}$ was calculated as shown in Equation 4-1.

$$TDFC = (1 + F)(1 - \beta + C_1) + \left(\frac{S_0 - S_1}{\alpha_1 - \alpha_2} \right) + FP \left(1 + \frac{R}{\beta} \right)^{P^m} \left(1 - \frac{N}{C_2} \right) \left(\frac{1}{24 \cdot \text{day} \cdot Q^d} \right) \quad (4-1)$$

F is the fabrication loss (0-11%), C_1 is the uranium conversion loss (0-8%), S_0 is the desired enrichment, α_1 is the tails enrichment (0-80%), α_2 is the feed enrichment (0-80%), FP is the price of the feed in dollars per kilogram, β is the interest rate used to purchase the feed, U_{py} is the payment schedule for the core (24 months or more), N is the outage length in days (24 days is assumed) for both the 18 and 24-month cycle, C_2 is the cycle length in days, day is the burnup in GWd/tonU and an off-charge (4000-10,000) was assumed.

The initial price for urethane conversion was set at \$1 per kilogram of urethane.

(25) The conversion charge (CC) in $\frac{\text{mk}}{\text{kg}} \cdot \frac{\text{kg}}{\text{kg}}$ was calculated as shown in Equation 4-2

$$CC = (1 + F_1) \cdot \left(\frac{P_1 + P_2}{P_2 - P_1} \right) \cdot CP \cdot \left(1 + \frac{R}{12} \right)^{12n} \cdot \left(1 - \frac{OR}{C_{12}} \right) \cdot \left(\frac{1}{24 \cdot \ln 2 \cdot \text{eff}} \right) \quad (4-2)$$

CP is the price of the conversion in dollars per kilogram and C₁₂ is the payment schedule for the conversion, assumed to be 12 months.

The base cost of a separation work unit (SWU) was set at \$110 per SWU [26].

The number of SWUs needed for the desired enrichment per kilogram of product was calculated as shown in Equation 4-3 [3]

$$SWU = F(x_2) + \frac{W}{F} \cdot F(x_1) = \frac{F}{F} \cdot F(x_2) \quad (4-3)$$

F is the number of kilograms of uranium in the waste stream (mk), P is the number of kilograms of enriched product, and F is the number of kilograms of feed material. The quantities F(x) are known as separation potentials and are calculated as shown in Equation 4-4.

$$F(x_2) = (2 - x_2 - 1) \cdot \ln \left(\frac{2 - x_2}{1 - x_2} \right) \quad (4-4)$$

Once the number of SWUs was determined, the enrichment charge (EC) in $\frac{\text{mk}}{\text{kg}} \cdot \frac{\text{kg}}{\text{kg}}$ was calculated as shown in Equation 4-5

$$EC = SWU \cdot (1 + F_2) \cdot EC \cdot \left(1 + \frac{R}{12} \right)^{12n} \cdot \left(1 - \frac{OR}{C_{12}} \right) \cdot \left(\frac{1}{24 \cdot \ln 2 \cdot \text{eff}} \right) \quad (4-5)$$

JC is the cost per kW_e and the payment schedule for the encasement (J_{pe}) was assumed to be 12 months.

A base cost of 250 dollars per kilogram (J. Malcom, Exelon, personal communication, April, 2004) was assigned for fabrication (FBC). An additional charge of \$3.84 (multiplied by 8.3) per kilogram was included for encasements greater than 3-wt% up to and including 6.5-wt% for the enclosure of stainless steel rods in half of the assemblies in order to ship and store fuel assemblies. For all encasements there was an inclusion of \$28.79 per kilogram for the additional cost of NP&As for half of the assemblies in a batch (B. Seeliger, Southern Nuclear Operating Company, personal communication, April 12, 2004). This charge was increased to \$37.58 per kilogram and the \$3.84 per kilogram dropped for encasements greater than 6.5-wt% due to the need to replace the steel rods with NP&As in all the assemblies for safety by function decreased in Chapter 2 in the fabrication, shipment, and storage of new assemblies. The fabrication charge (FC) is $\frac{m_{FA}}{W_{FA} - W_{C}}$ was calculated as shown in Equation 4-6

$$FC = FBC \left(1 + \frac{8}{12} f^{0.75} \right) \left(1 - \frac{GB}{C_{FA}} \right) \left(\frac{1}{24 \text{ new } f^{0.75}} \right) \quad (4-6)$$

A payment schedule for the fabrication (F_{pe}) of 8 months was assumed.

The model utilized the dry fabrication process applied by the Braidwood plant of Ameren/Transcon-AMP. There is little incentive for a fuel fabricator to encourage utilities to encase encasements. Greater encasements require smaller batch sizes and thus fewer assemblies to be built. Changing from 3-wt% to 6-wt% by a utility using a two year cycle could result in a 33% reduction in the number of fuel assemblies purchased. Westinghouse, which built the majority of PWR fuel fabrication systems in the United

States, uses a wet process to convert the CFI gas to powder. For Westinghouse to increase enrichment would require either substantial replacement of much of the piping or scrapping the wet process altogether and going to the simpler, wet stop-process by the purchase of a dry conversion kit. It is probable that any consortium of utilities that contracted Westinghouse to go to higher enrichments would be expected to carry the financial burden for the cleanup and disposal of the wet processing equipment. As well, contract-AEP's dry conversion process does not appear to require any major equipment changes until the required enrichment is greater than 5-wt% ^{235}U , then their current dry conversion kit would have to be replaced. Since Fluorstone has a much smaller fraction of the PWR fuel fabrication contracts, not only is it more likely they would be willing to redesign the financial risk of inventing a dry modification and bearing costs for the fabrication of greater than 5-wt% ^{235}U fuel in return for additional fuel fabrication contracts, but it is probable that the pricing of these contracts would be more competitive.

The total cost to the fabrication facility (T_{tot}) for the equipment upgrade was calculated as shown in Equation 4-7

$$T_{\text{tot}} = EU \left(1 + \left(\frac{r}{i} \right)^n \right) \quad (4-7)$$

EU is the base cost of equipment replacement, r is the interest rate the fabrication plant pays on the loan taken out to pay for the upgrade and n is the number of years a loan is taken out to repay for these costs. The base interest rate used was 10% (an order-of-magnitude profit for the fabricator's company) and the number of years was set to 5. A base cost of \$390,000 for replacement of the column (D. Beckman, A18702M, personal communication, May 21, 2004) was included at enrichments greater than 5-wt% ^{235}U and \$200,000 was charged for replacement of the dry conversion kits at enrichments greater

then 5-wt%. The change in the utility for the equipment replacement (C_{eq}) is

$\frac{\text{unit}}{\text{year}} \cdot \Delta c_e$ was calculated as shown in Equation 4-3

$$C_{eq} = \left(\frac{F_{eq} \cdot C_e \cdot \left(1 + \frac{1}{12} \right)^{12n}}{F - r_{eq} \cdot n_e} \right) \cdot D = \left(\frac{\$8}{C_{eq}} \right) \cdot \left(\frac{1}{12 + 12n \cdot \frac{1}{12}} \right) \quad (4-3)$$

C_e is the cycle length, n is the number of batches, n_e is the number of batches the material are ordered before they are used, r_{eq} is the amount of fuel at the rest and n_e is the number of power plants involved in the equation. This change would be typically on the order of 0.1% of the fuel cycle cost. An additional cost of \$12 million in order to clean up Wrentham's wet processing facility and much more to a dry process [18] would still represent only 0.4% of the total fuel cycle cost.

The total cost to the facility (C_{tot}) for licensing the NRC container for non-nuclear greater than 5-wt% was calculated as shown in Equation 4-4.

$$C_{tot} = LF \cdot \left(\frac{1}{f} \right) + \left(\frac{1}{f} \right)^2 \quad (4-4)$$

LF , the cost of the licensing units, was calculated to be \$134,700. The base license cost was 15% (to include profit for the contractor plus licensing the technology) and the number of years was set to 5. A breakdown of the licensing and review costs is given in Table 4-1 and Table 4-2 [18].

Table 4-1 Cost estimates for licensing of the NRC container for greater than 5-wt% fuel

Type of System	Estimated Duration	Cost
Conceptual Analysis	25d	\$ 100,000
Environmental Document	40	\$ 100,000
Radwaste Provision	40	Major
Final Approval	100	\$ 100,000

Table 4-3. Cost estimates for a 3 percent NSC increase of the HSB containers for greater than 3-wt% fuel

Expense Type	Cost per Month	Total Cost
Salaries	\$400	\$1.1M
Supplies/Fuel	\$400	\$1.1M
Other	\$4,000	\$11,000

The change to the salaries for increasing the HSB containers for enrichment greater than 3-

wt% (C_{LS}) is $\frac{\partial C_{LS}}{\partial F} \frac{\partial F}{\partial \delta_0}$ was calculated as shown in Equation 4-10

$$C_{LS} = \left(\frac{T_{LS} \cdot C_L \cdot \left(\left(1 + F_1 \right) \cdot \left(1 + \frac{\delta_0}{12} \right)^{12} \right)}{F \cdot C_{LS} \cdot \delta_0} \right) \cdot \left(1 - \frac{\partial C_L}{\partial F} \cdot \left(\frac{1}{24 \cdot \ln(1 + \delta_0)} \right) \right) \quad (4-10)$$

The payment schedule for the financing (LF_{LS}) for the base model was assumed to be at the time the enriched UF₆ was to be ordered, which is 12 months. The base model assumes the HSB containers is financed by USBC during the construction of their gas enrichment plant and the cost is passed on to the utilities. In the case in which the utilities do not bear the burden, T_{LS} would be set to 0. If the fuel fabricator bears the burden of refinancing the HSB containers and must pass through this cost, LF_{LS} would be set to 1 month. This change would be typically on the order of 0.1% of the fuel cycle cost.

The total cost to the fabrication facility (F_{LS}) for the financing costs to provide fuel enrichment greater than 3-wt% was calculated as shown in Equation 4-11

$$F_{LS} = LF \cdot \left(\frac{1}{\delta} + \frac{1}{\delta^2} \right) \quad (4-11)$$

LF , the sum of the financing costs, was calculated to be \$402,400. The base interest rate, δ , used was 12% and the number of years was set to 3. A breakdown of the financing and review costs are given in Table 4-3 and Table 4-4 [18].

Table 4-3 Cost estimates for licensing of a fuel fabrication facility to process greater than 3-mtU fuel

Type of Activity	Estimated Months	Cost
Construction	240	\$1,000,000
Operational, Construction	60	\$0.500,000
Radiological Control	48	\$0.000
Safe Analysis	278	\$0.000,000
Other, Licensing	100	\$0.000,000

Table 4-4 Cost estimates for first cycle of a process NRC review of a fuel fabrication plant to process greater than 3-mtU fuel

Expense Type	Expense Period	Expense Cost
Analysis		\$1,000,000
Licensing/First		\$0.500,000
Other		\$0.000,000

The charge to the utilities for licensing the fabrication facility for assemblies greater

than 3-mtU (C_{L2}) as $\frac{\text{mtU}}{\text{MW} \cdot \text{yr}}$ was calculated as shown in Equation 4-12

$$C_{L2} = \left(\frac{C_{L1} - C_1 - B - \beta + \frac{\beta}{12} \gamma^m}{\gamma - C_{L1} - \beta_1} \right) \left(1 - \frac{C_{L1}}{C_{L2}} \right) \left(\frac{1}{24 \text{ hrs} \cdot \text{yr}} \right) \quad (4-12)$$

This charge is typically on the order of .02 to 0.03% of the fuel cycle cost

The initial licensing cost (C_L) as $\frac{\text{mtU}}{\text{MW} \cdot \text{yr}}$ was calculated as shown in Equation 4-

13

$$C_L = \frac{R_L + G + \frac{\beta}{12} \gamma^m}{C_{L1} - 1000} \left(1 - \frac{C_{L1}}{C_{L2}} \right) \left(\frac{1}{24 \text{ hrs} \cdot \text{yr}} \right) \quad (4-13)$$

R_L is the base cost of initial licensing, which was set to 1 million dollars (7) Malone,

San Jose, personal communication, April, 2007. The start (first-cycle) cost (C_L) was then

calculated as shown in Equation 4-14

$$B_1 = \text{FDPC} + CC + AC + PC + C_{\text{top}} + C_{\text{up}} + C_{\text{down}} + B_2 \quad (4-14)$$

In-Core Capital Use Charge, Storage, and Disposal Charge Calculations

The in-core capital use charge (KC) is $\frac{\text{mils}}{\text{dollar} \cdot \text{yr}}$ was calculated as shown in

Equation 4-15

$$\begin{aligned} KC = & (L_1 L_2) \left(\frac{R}{2} \right) \left(\frac{1}{\beta} + \frac{1}{\beta} F^{\beta-1} \right) + \left(\frac{R}{2} \right) \beta + (L_1 L_2) \left(\frac{R}{2} \right) \left(\frac{1}{\beta} + \frac{1}{\beta} F^{\beta-1} \right) + \left(\frac{R}{2} \right) \beta \\ & \left(1 - \frac{DK}{C_u} \right) \left(1 + \frac{1}{24 \cdot \text{hrs}} \frac{1}{\text{dollar} \cdot \text{yr}} \right) \quad (4-15) \end{aligned}$$

The variables β_u and β_d are the corresponding fractions of the number of assemblies which reach the upper and lower bounds for the lengths of time in months the fuel is in the core, KTC_u and KTC_d , for a specific cycle length. For example, if enrichment x used 3.4 batches to reach a two-year cycle, 40% of the assemblies would be in the core for 3 cycles and β_u would be 0.4. KTC_u would be 3 times 36 months for a total of 72 months. KTC_d would be 48 months and β_d would be 2.0.

The cost of financing the spent fuel (SL_u) is $\frac{\text{mils}}{\text{dollar} \cdot \text{yr}}$ was calculated as shown in

Equation 4-16

$$SL_u = \left(\frac{BBL_u - C_u \cdot \beta_u}{x \cdot n_{\text{fuel}}} \right) \left(\beta_u - \frac{DK}{C_u} \right) \left(1 + \frac{1}{24 \cdot \text{hrs}} \frac{1}{\text{dollar} \cdot \text{yr}} \right) \quad (4-16)$$

BBL_u is the base cost of financing spent fuel pool for enrichments beyond 3-wth U²³⁵. A summary of calculations of these costs is given in Tables 4-3 and 4-4.

The disposal fee (DF) is $\frac{\text{mils}}{\text{dollar} \cdot \text{yr}}$ was calculated as shown in Equation 4-17

Table 4-3: Cost estimates for handling of a spent fuel pool to store greater than 3-wt% fuel

Type of Analysis	Estimated Method	Cost
Industry Analysis	330	\$52,500
Governmental Estimates	10	\$15,000
Balance Estimate	40	\$3,500
Risk Analysis	220	\$11,500

Table 4-4: Cost estimates for a 3 percent HfO₂ version of a spent fuel pool for the storage of greater than 3-wt% fuel

Expense Type	Estimated Price	Total Cost
Reflex	\$100	\$4,500
Leakage/Heat	\$400	\$1,500
Other	\$5,100	\$21,000

$$REP = REP' \left(1 - \frac{OE}{C_{fu}} \right) \quad (4-17)$$

REP' is the base government charge to reflect an $\int \frac{dw}{REP' dt}$ for the final disposal of

molten fuel [20]. The dry cask storage cost (DCSC) was calculated as shown in Equation

4-18

$$DCSC = \frac{1200 \text{ per kg}}{24 \text{ eff} \text{ hrs}} \left(1 - \frac{OE}{C_{fu}} \right) \quad (4-18)$$

A recent cost case indicates that the dry cask storage charges may be picked up by the Department of Energy. This decision would transfer the cost savings from Equation 4-18 to the Department of Energy.

Replacement Power and Fuel Cycle Cost Calculations

The replacement power (RP) in kW/ha, needed during the storage was calculated as shown in Equation 4-19

$$RP = RP' \text{ eff } 24 \text{ hrs } 1000 \quad (4-19)$$

TP is the thermal power, modeled as $3000 \pm 100 \text{ MW}_{th}$, and Q_L is the outage length in days, which was assigned base values of 15 and 30 days [14]. The labor cost (\dot{LC}) in $\frac{\text{mkd}}{\text{day}}$ during an outage was calculated as shown in Equation 4-20.

$$LC = (CPD \cdot Q_L \cdot 1000) \quad (4-20)$$

CPD is the cost per day and was assigned a base value of $5660 \frac{\text{mkd}}{\text{day}}$ (Makana, Erection, general construction, April, 2001). The outage cost (\dot{OC}) in $\frac{\text{mkd}}{\text{MW} \cdot \text{yr}}$ is calculated as shown in equation 4-21.

$$\dot{OC} = \left(\frac{TP - RPC + LC}{TP} \right) \cdot \left(\frac{Q_L}{Q_{L0}} \right) \quad (4-21)$$

RPC is the replacement power cost, which is set as $25 \cdot \frac{\text{mkd}}{\text{MW} \cdot \text{yr}}$. The fixed capital cost

(FCC) in $\frac{\text{mkd}}{\text{MW} \cdot \text{yr}}$ is calculated as shown in Equation 4-22.

$$FCC = S_0 + RVC + S_0 + \Delta F + \Delta CMC + OC \quad (4-22)$$

CHAPTER 5 RESULTS AND DISCUSSION

Base Model Case

For the base model case with a 15-day outage, the maximum fuel-cycle cost is at 4.5-wt% for the 12-month cycle, 6.0-wt% for the 18-month cycle, 6.5-wt% for the 24-month cycle, 7.5-wt% for the 30-month cycle, 8.0-wt% for the 36-month cycle, and 9.0-wt% for the 42-month cycle. For the base model case with a 30-day outage, the maximum fuel cycle cost is at 4.5-wt% for the 12-month cycle, 5.5-wt% for the 18-month cycle, 6.5-wt% for the 24-month cycle, 7.5-wt% for the 30-month cycle, 7.5-wt% for the 36-month cycle, and 9.0-wt% for the 42-month cycle. The cost savings or penalty in dollars per year per 1000 MW_e plant is determined by multiplying the difference fuel cycle cost as $\frac{\text{cents}}{10^6 \text{ Btu}} \times \text{kg}$ between two enrichment by a factor of 8.76×10^6 . Assuming a

15-day outage length, the savings in fuel cycle costs in going from 5-wt% to 6.5-wt% for plants on an 18-month cycle is only \$91,000 a year per 1000 MW_e plant. If the outage length is increased to 30 days, the cost savings is reduced to \$13,000 a year. For the 24-month cycle with 15-day outages, the savings in fuel cycle costs in going from 5-wt% to 6.5-wt% is $9.812 \times \frac{\text{cents}}{10^6 \text{ Btu}} \times \text{kg}$, approximately \$1,195,000 a year per 1000 MW_e plant. An increase of outage length to 30 days would decrease the cost savings to \$7,119,000 per year. A nuclear plant using a 30-month cycle with a 15-day outage would save

\$5,871,000 per year by going from 5.0-wt% to 7.5-wt%. For a 30-day outage the savings would decrease to \$4,541,000 per year. The 12-month cycle has a fuel cycle cost minimum below the currently licensed 5-wt% enrichment limit and is not competitive under the base model economics. The 36 and 42-month cycles can not be achieved using 5-wt% fuel and therefore no cost savings are calculated.

All previous costs are calculated for the first five-year period in which the plants would have to pay for the licensing and equipment modifications to process and accept greater than 5 wt% fuel. After the first five years, 36-month cycle plants with 15-day outage lengths would save \$140,000 per year by increasing their enrichment from 5.0-wt% to 5.5-wt%. An outage length of 30 days would decrease the savings to \$89,000 per year. Plants on a 36-month cycle with 10-day outage lengths would save \$1,716,000 per year by increasing their enrichment from 5.0-wt% to 5.5-wt%. This amount is decreased to \$1,399,000 per year if the outage length is increased to 30 days. A 36-month cycle plant with 5-day outage would save \$1,155,000 per year by increasing its enrichment from 5.0-wt% to 7.5-wt%. A 30-day outage would lower this savings to \$4,827,000 per year. The results for the base case calculations are presented in Figures 3-1 through 3-4 and in Tables 3-1 and 3-2.

Effect of Variation in Participating Number of Nuclear Plants

Variations in the number of nuclear plants which participate in a program for increasing fuel enrichment will reflect the charges to each plant for the licensing and equipment replacement at the fabrication facility. If the number of participating plants is

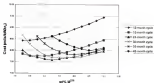


Figure 5-1 Fuel cycle cost comparison of varying cycle lengths with 13-day outages for the first 3 years

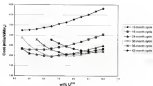


Figure 5-2 Fuel cycle cost comparison of varying cycle lengths with 10-day outages for the first 3 years

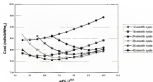


Figure 3-3: Fuel cycle cost comparison of varying cycle lengths with 3-day outage after the first 3 years

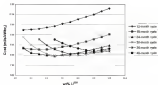


Figure 3-4: Fuel cycle cost comparison of varying cycle lengths with 30-day outage after the first 3 years

increased to 15, the savings for reactors for the first 3 years on a 36-month cycle with a 13-day outage changing from 3-wt% to 7.5-wt% fuel would increase by 0.2% to \$3,888,000 a year for each plant. For the 36-month cycle, changing from 3-wt% to 6.5-wt% fuel would increase savings to approximately \$3,642,000 (0.7%) and the 36-month cycle plants would only increase savings to \$300,000 (0.4%) per year each. Increasing the number of participating plants from 15 to 20 only increases the cost savings to \$3,060,000 (0.4%) a year per each 36-month cycle plant, \$1,673,000 (3.4%) for the 24-month cycle plants, and \$13,000 (0.0%) for the 18-month-cycle. The savings for reactors on a 36-month cycle and 36-day outage would increase to \$4,560,000 (8.7%) per year if the number of participating plants were increased from 18 to 15. The 24-month cycle would increase to \$1,334,000 (3.7%) and the 18-month cycle plants would increase to \$77,000 (117.4%). If the number of participating plants were increased to 20, the cost savings would increase to \$4,560,000 (8.7%), \$1,540,000 (3.4%), and \$34,000 (145.9%) for the 36-month, 24-month, and 18-month cycle plants respectively. Increasing the number of participating plants beyond this point results in diminishing returns. In general, increasing the number of plants by ten beyond 15 results in an increase of profits of approximately 35% of that seen by the previous increase of 5.

If the number of plants is decreased from the base model of 18 to 5, the 36-month cycle plants with 11-day outages would decrease savings to \$3,610,000 (-1.7%), the 24-month cycle plants to \$1,373,000 (-3.7%), and the 18-month cycle plants to \$35,000 (-64.1%) per year. If the outage length is 36 days, the 36-month cycle plants savings would decrease to \$4,480,000 (-1.4%) and the 24-month to \$1,263,000 (-4.4%). The 18-month cycle's maximum fuel cycle cost along with a 3-wt% and plants with this cycle

length, would see a net loss of \$46,000 (-46.1 1%) a year if they increased their treatments to 3-5-wt%. If only two plants participate in an increased treatments program, each plant would see a net loss of \$205,000 (-19.1 2%) per year going from 3-wt% to 6-8-wt% if they went only on an 18-month cycle with 15-day outages. The same two plants could save \$1,218,000 (12.4 1%) by increasing treatments from 3-5-wt% to 6-8-wt% if they went on a 24-month cycle, or \$4,698,000 (-7.4 1%) per year if they went using a 36-month cycle. For 30-day outages, the 18-month cycle would lose \$342,000 (-3.4 1%); a year, the 24-month cycle would decrease savings to \$963,000 (-21.0 1%), and the 36-month cycle would see increased savings to \$3,047,000 (-4.1 1%) per year for the first 3 years. If only one 15-day outage plant were to participate in an increased treatments program, it would see a net loss of \$1,173,000 (-1,145.9 1%) per year by going from 3-5-wt% to 6-8-wt% on an 18-month cycle, reduced savings of \$134,000 (-19.1 1%) a year going from 3-5-wt% to 6-8-wt% on a 24-month cycle, and reduced savings to \$3,775,000 (-36.1 1%) per year for plants using a 36-month cycle. The same plant with a 30-day outage would experience a loss of \$1,345,000 (-9,914.7 1%) for the 18-month cycle, reduced savings to \$23,000 (-46.1 1%) for the 24-month cycle, and a savings of \$1,208,000 (-29.1 1%) per year for the first 3 years for plants on a 36-month cycle. The results of the calculations for varying the number of participating plants are shown in Tables E-3 through E-16 and Figures 5-5 through 5-16.

Effect of Fluctuations in Uranium Ore Prices

The price of uranium has shown significant variation over the last 12 years as displayed in Figure 5-17 (29). In the last 18 months it has increased from \$18 to \$33-40 per kilogram. The base economic model projects a cost of \$40 per kilogram. Figure 5-

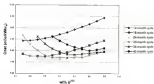


Figure 5-3: Fuel cycle cost comparison of varying cycle lengths with 15-day outages for the first 3 years with 11 participating reactors

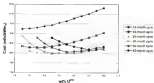


Figure 5-4: Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 8 years with 15 participating reactors

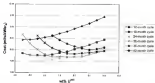


Figure 3-7. Fuel cycle cost comparison of varying cycle lengths with 15-day outages for the first 3 years with 20 participating reactors

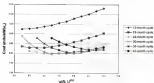


Figure 3-8. Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with 30 participating reactors

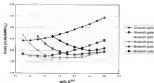


Figure 5-9 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 3 years with 23 participating reactors

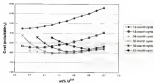


Figure 5-10 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 6 years with 23 participating reactors

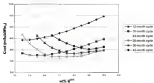


Figure 3-11. Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 3 years with 5 participating reactors.

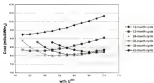


Figure 3-12. Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 3 years with 5 participating reactors.

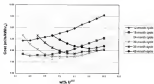


Figure 5-13 Fuel cycle cost comparison of varying cycle lengths with 21-day outages for the first 5 years with 2 participating reactors

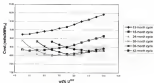


Figure 5-14 Fuel cycle cost comparison of varying cycle lengths with 18-day outages for the first 5 years with 2 participating reactors

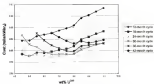


Figure 5-15 Fuel cycle cost comparison of varying cycle lengths with 18-day outage for the first 5 years with one participating reactor

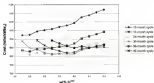


Figure 5-16 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with one participating reactor

18 through 3-37 show the individual fuel cycle costs for the various cycle lengths at 3.6 wt% as well as at their maximum fuel cycle cost configurations. As shown in these figures the fuel represents between 8% and 44% of the total fuel cycle costs. The percentage that the fuel represents of the fuel cycle cost increases with longer cycle times and shorter outages. An increase of unit costs to \$60 per kilogram would decrease cost savings to \$12,800 (-21.0%) and \$4,800 (-44.7%) a year per plant for the 18-month-cycle with 15 and 30-day outages lengths. The cost savings for the 24-month cycle would increase to \$1,347,000 (-9.5%) and \$1,431,000 (-9.9%) for the 24-month cycle. The 36-month-cycle plants would require more cost savings to \$5,000,000 (-11.4%) and \$1,067,000 (-1.7%). A further increase to \$80 a kilogram would result in a further reduction of cost savings to \$23,800 (-42.3%) a year for 18-month cycle plants with 15-day outages. The 30-day outage plants would experience loss of \$1,000 (-13.7%) a year. Reactors using 36-month cycle and 15-day and 30-day outages would increase savings to \$1,899,000 (-1.4%) and \$1,553,000 (-1.7%). The 36-month cycle plants would increase savings to \$4,347,000 (-11.2%) and \$1,568,000 (-2.0%) for 15 and 30-day outages, respectively. In general, for every \$20 increase per kilogram from the \$40 per kg base cost, the cost savings is reduced by \$15,000 (-3.0 9%) and \$3,000 (-0.6 9%) per year for 18-month cycle plants with 15 and 30-day outages, increased by \$152,000 (-5.3 9%) and \$118,000 (-0.9 9%) for 24-month cycle reactors, and increased by \$348,000 (-3.1 6%) and \$521,000 (-2.1 8%) per year for 36-month cycle plants. A reduction of unit costs from \$40 to \$20 a kilogram would result in equal but opposite change. The reason for the opposite trends for the 18-month-cycle vs the 24 and 36-month cycles can be shown by plotting a 2nd order polynomial trendline for the fuel cycle costs for the three cycles at

the base costs and also increased feed cost of 148 per kilogram. The equations for the feedlines for the base costs with 15-day savings and the increased feed costs of 150 per kilogram are presented in Equations 3-1 through 3-6. Equations 3-7 through 3-12 are the 30-day savings calculations.

$$FCCF(15 - \text{day})_{\text{base}} = 0.4558 \cdot \text{cost}^2 - 0.3482 \cdot \text{cost} + 8.3804 \quad (3-1)$$

$$FCCF(15 - \text{day})_{\text{inc}} = 0.6519 \cdot \text{cost}^2 - 0.7134 \cdot \text{cost} + 10.166 \quad (3-2)$$

$$FCCF(15 - \text{day})_{\text{inc}} = 0.3834 \cdot \text{cost}^2 - 1.1042 \cdot \text{cost} + 12.838 \quad (3-3)$$

$$FCCF(15 - \text{day})_{\text{inc,24}} = 0.8416 \cdot \text{cost}^2 - 0.4482 \cdot \text{cost} + 10.139 \quad (3-4)$$

$$FCCF(15 - \text{day})_{\text{inc,30}} = 0.6442 \cdot \text{cost}^2 - 0.8811 \cdot \text{cost} + 11.941 \quad (3-5)$$

$$FCCF(30 - \text{day})_{\text{base}} = 0.1863 \cdot \text{cost}^2 - 1.4338 \cdot \text{cost} + 15.436 \quad (3-6)$$

$$FCCF(30 - \text{day})_{\text{inc}} = 0.4036 \cdot \text{cost}^2 - 0.3208 \cdot \text{cost} + 5.2163 \quad (3-7)$$

$$FCCF(30 - \text{day})_{\text{inc}} = 0.649 \cdot \text{cost}^2 - 0.4292 \cdot \text{cost} + 10.234 \quad (3-8)$$

$$FCCF(30 - \text{day})_{\text{inc}} = 0.6811 \cdot \text{cost}^2 - 0.2588 \cdot \text{cost} + 12.238 \quad (3-9)$$

$$FCCF(30 - \text{day})_{\text{inc,24}} = 0.6814 \cdot \text{cost}^2 - 0.425 \cdot \text{cost} + 10.821 \quad (3-10)$$

$$FCCF(30 - \text{day})_{\text{inc,30}} = 0.6608 \cdot \text{cost}^2 - 0.8098 \cdot \text{cost} + 11.978 \quad (3-11)$$

$$FCCF(30 - \text{day})_{\text{inc,30}} = 0.6803 \cdot \text{cost}^2 - 1.5494 \cdot \text{cost} + 15.268 \quad (3-12)$$

If the first three equations for the 15-day savings are differentiated and set to zero, the minimum for the 18-month cycle is 3.43-wt%, the 24-month is 6.91-wt% and the 30-month is 7.78-wt%. Equations 3-4 through 3-6 have minimums at 5.24-wt%, 6.47-wt%, and 7.78-wt%. In the case of the 30-month cycle, the first case actual minimum is lower than the proposed change is 6.8-wt%. For the 24 and 30-month cycles, the minimum for

the base case is higher than the proposed changes to 6.0 and 6.3-wt% respectively. An increase in ore price lowers the enrichment at which the fuel cycle cost is maximum for all three cycles, but is slowing that enrichment away from the examined 18-month cycle minimum because it lies to the left of curves and so return drives it towards the proposed 18 and 30-month-cycle enrichment changes. The same trends can be seen for the 30-day outage cycles. The minimums of the base cost of \$-66 per kilogram of uranium-235, 4.7%, and 7.71-wt% for the 18, 24, and 30-month cycles. When the ore cost is increased to \$40 per kilogram, the maximum fuel cycle costs for the 18, 24, and 30-month cycles are at lower enrichments of 5.13, 6.68, and 7.65-wt%. The results of fuel-cycle cost calculations for varying uranium feed prices are presented in Figures 3-18 through 3-27 and in Tables E-17 through E-22 of Appendix E.

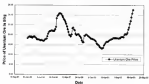


Figure 3-17 Historical price data of uranium ore from The Ux-Chemical Company, LLC (28)

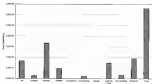


Figure 5-18 Individual fuel cycle costs for the 12-month cycle with a 12-day outage at 3.0-refd/LWR enrichment

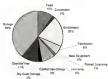


Figure 5-19 Individual fuel cycle cost percentages for the 12-month cycle with a 12-day outage at 3.0-refd/LWR enrichment

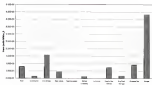


Figure 3-20 Individual fuel cycle costs for the 12-month cycle with a 30-day outage at 3.0-wt% U^{235} enrichment

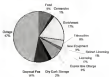


Figure 3-21 Individual fuel cycle cost percentages for the 12-month cycle with a 30-day outage at 3.0-wt% U^{235} enrichment

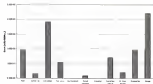


Figure S-22 Individual fuel cycle costs for the 18-month cycle with a 15-day outage at 3.5-ref% LWR enrichment

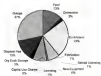


Figure S-23 Individual fuel cycle cost percentages for the 18-month cycle with a 15-day outage at 3.5-ref% LWR enrichment

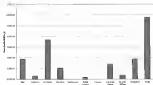


Figure 3-24 Individual full-cycle costs for the 18-month cycle with a 70-day outage at 3.6-meth U^{235} enrichment

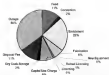


Figure 3-25 Individual full-cycle cost percentages for the 18-month cycle with a 70-day outage at 3.6-meth U^{235} enrichment

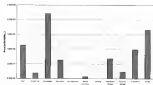


Figure 3-26 Individual fuel cycle costs for the 24-month cycle with a 13-day outage at 1.0-meth 10^{18} enrichment

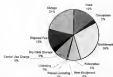


Figure 3-27 Individual fuel cycle cost percentages for the 24-month cycle with a 13-day outage at 1.0-meth 10^{18} enrichment

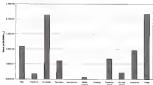


Figure 3-28 Individual life cycle costs for the 24-month cycle with a 30-day outage at 3.0-yr/10% U^{max} enrichment

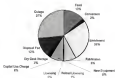


Figure 3-29 Individual life cycle cost percentages for the 24-month cycle with a 30-day outage at 3.0-yr/10% U^{max} enrichment

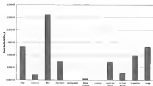


Figure S-30 Individual fuel cycle costs for the 36-month cycle with a 13-day outage at 5 6-month 1000 MW outages

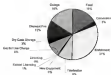


Figure S-31 Individual fuel cycle cost percentages for the 36-month cycle with a 13-day outage at 5 6-month 1000 MW outages

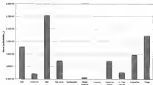


Figure 3-12 Individual full-cycle costs for the 30-month cycle with a 30-day outage at 3-B with U^{235} enrichment

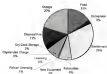


Figure 3-13 Individual full-cycle cost percentages for the 30-month cycle with a 30-day outage at 3-B with U^{235} enrichment

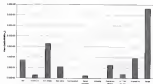


Figure S-34 Individual fuel cycle costs for the 12-month cycle with a 15-day outage at 4.5 with UO_2 enrichment

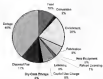


Figure S-35 Individual fuel cycle cost percentages for the 12-month cycle with a 15-day outage at 4.5 with UO_2 enrichment

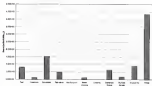


Figure S-16 Individual fuel cycle costs for the 12-month cycle with a 30-day outage at 4.5-wt% UO_2 enrichment

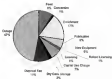


Figure S-17 Individual fuel cycle cost percentages for the 12-month cycle with a 30-day outage at 4.5-wt% UO_2 enrichment

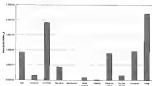


Figure S-18 Individual fuel cycle costs for the 18-month cycle with a 15-day outage at 6.0-eu% LWR enrichment

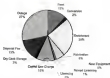


Figure S-19 Individual fuel cycle cost percentages for the 18-month cycle with a 15-day outage at 6.0-eu% LWR enrichment

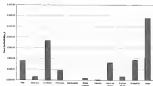


Figure 3-40 Individual fuel cycle costs for the 18-month cycle with a 50-day outage at S 3 with U-235 enrichment

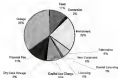


Figure 3-41 Estimated fuel cycle cost percentages for the 18-month cycle with a 50-day outage at S 3 with U-235 enrichment

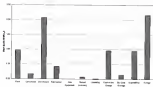


Figure 3-44 Individual fuel-cycle costs for the 24-month cycle with a 20-day outage at 6.5-wt% U^{235} enrichment

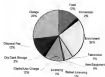


Figure 3-45 Individual fuel-cycle cost percentages for the 24-month cycle with a 20-day outage at 6.5-wt% U^{235} enrichment

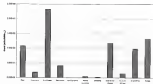


Figure 5-46 Individual fuel cycle costs for the 30-month cycle with a 15-day outage at 7.9 with U^{235} enrichment



Figure 5-47 Individual fuel cycle cost percentages for the 30-month cycle with a 15-day outage at 7.9 with U^{235} enrichment

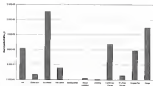


Figure 3-48 Individual fuel cycle costs for the 30-month cycle with a 30-day outage at 7.5-wt% U^{235} enrichment.



Figure 3-49 Individual fuel cycle cost percentages for the 30-month cycle with a 30-day outage at 7.5-wt% U^{235} enrichment.

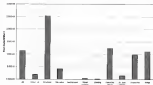


Figure 3-50 Individual fuel cycle costs for the 16-month cycle with a 13-day outage at 8.6-mt/yr LWR2000

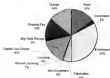


Figure 3-51 Individual fuel cycle cost percentages for the 16-month cycle with a 13-day outage at 8.6-mt/yr LWR2000

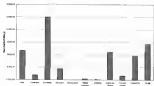


Figure 3-52 Individual fuel cycle costs for the 18-month cycle with a 10-day outage at 7.5-mt% U^{235} enrichment.



Figure 3-53 Individual fuel cycle cost percentages for the 18-month cycle with a 10-day outage at 7.5-mt% U^{235} enrichment.

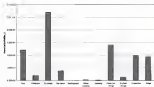


Figure 5-54 Individual Fuel Cycle Costs for the 42-month cycle with a 15-day outage at 9.8 with 1% enrichment

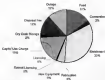


Figure 5-55 Individual Fuel Cycle Cost Percentages for the 42-month cycle with a 15-day outage at 9.8 with 1% enrichment

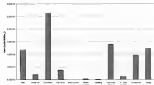


Figure 5-56 Individual Fuel cycle costs for the 42-month cycle with a 30-day outage at 9.44% U^{235} enrichment

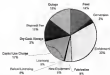


Figure 5-57 Individual Fuel cycle cost percentages for the 42-month cycle with a 30-day outage at 9.44% U^{235} enrichment

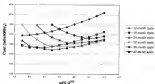


Figure 3-38 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 3 years with one core increased to 100% utilization

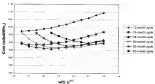


Figure 3-39 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 3 years with one core increased to 50% utilization

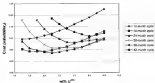


Figure 5-55 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with ore cost increased to \$40 a kilogram

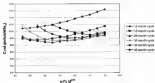


Figure 5-56 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with ore cost increased to \$40 a kilogram

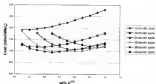


Figure 3-62. Fuel cycle cost comparison of varying cycle lengths with 14-day outages for the first 3 years with core costs decreased to \$28 a kilogram.

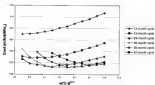


Figure 3-63. Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with core costs decreased to \$28 a kilogram.

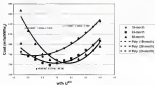


Figure 3-44 Base feed cycle cost comparison with baselines of the 18, 24, and 30-month cycle with 15-day outage length

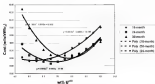


Figure 3-45 Feed cycle cost comparison with baselines of the 18, 24, and 30-month cycle with 15-day outage length and are increased to \$40 per kilogram

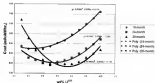


Figure 3-56 Fuel cycle cost comparison with breakeven of the 18, 24, and 36-month cycle with 30-day outage length

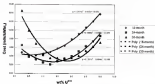


Figure 3-57 Fuel cycle cost comparison with breakeven of the 18, 24, and 36-month cycle with 30-day outage length and are increased to 500-gal hydrogen

Effect of Variation in Conversion Prices

Over the last 30 years the price of conversion has varied from a low of \$2.25 per kg in June of 2000 to the current price of \$7.20 per kg [25]. The base economic model projects a cost of \$7 per kilogram. As shown in Figures 5-18 through 5-23, the conversion process represents only 1 to 3% of the fuel cycle costs. An increase of conversion costs to \$10 per kilogram would decrease cost savings to \$45,000 (-3.0%) and \$11,000 (-0.8%) a year per plant for the 18-month cycle with 15 and 30-day outage lengths. The cost savings for the 24-month cycle would increase to \$1,407,000 (3.4%) and \$1,117,000 (3.3%) for the 24-month cycle. The 30-month cycle plants would increase their cost savings to \$5,117,000 (3.7%) and \$5,620,000 (3.7%). A further increase to \$12 a kilogram would result in a further reduction of cost savings to \$45,000 (-0.1%) a year for 18-month cycle plants with 15-day outages. The 30-day outage plants would reduce savings to (\$18,000 (-0.07%) a year. Savings using 24-month cycle and 15-day and 30-day outages would increase savings to \$1,459,000 (3.7%) and \$1,303,000 (3.4%). The 30-month cycle plants would increase savings to \$5,241,000 (3.9%) and \$4,651,000 (3.3%) for 15 and 30-day outages, respectively. In general, for every \$3 increase per kilogram from the \$7 per kilogram base cost, the cost savings is reduced by \$2,000 (-0.03%) and \$1,000 (-0.01%) per year for 18-month cycle plants with 15 and 30-day outages, increased by \$22,000 (0.4%) and \$34,000 (0.3%) for 24-month cycle reactors, and increased by \$83,000 (0.7%) and \$75,000 (0.7%) per year for 30-month cycle plants. A reduction of conversion costs from \$7 to \$5 a kilogram would result in equal but opposite changes. As with the fuel cost variations, the reason for the opposite results can be shown by plotting a 3rd order polynomial equation for the fuel cycle costs for

the three cycle lengths at an increased conversion cost of \$13 per kilogram. The equations for the tendlines for the increased conversion cost of \$13 per kilogram are presented in Equations 3-13 through 3-18.

$$FCCF[3 - \text{day}]_{\$13/\text{kg}} = 0.0551 \cdot \text{wt}^2 - 0.5795 \cdot \text{wt} + 4.476 \quad (3-13)$$

$$FCCF[3 - \text{day}]_{\$13/\text{kg}} = 0.0537 \cdot \text{wt}^2 - 0.5411 \cdot \text{wt} + 3.530 \quad (3-14)$$

$$FCCF[3 - \text{day}]_{\$13/\text{kg}} = 0.0489 \cdot \text{wt}^2 - 1.1003 \cdot \text{wt} + 12.204 \quad (3-15)$$

$$FCCF[10 - \text{day}]_{\$13/\text{kg}} = 0.1047 \cdot \text{wt}^2 - 0.1616 \cdot \text{wt} + 9.4045 \quad (3-16)$$

$$FCCF[10 - \text{day}]_{\$13/\text{kg}} = 0.2507 \cdot \text{wt}^2 - 0.403 \cdot \text{wt} + 10.403 \quad (3-17)$$

$$FCCF[30 - \text{day}]_{\$13/\text{kg}} = 0.384 \cdot \text{wt}^2 - 1.2839 \cdot \text{wt} + 13.177 \quad (3-18)$$

Differentiating the equations and setting them to zero yields a minimum for the 10-month cycle at 3.41-wt%, 4.30-wt% for the 24-month cycle, and 5.79-wt% for the 30-month cycle plots with 13-day outages. For 30-day outage plots the minimums become 3.27-wt%, 4.72-wt%, and 7.70-wt% for the 10, 24, and 30-month cycles. An increase in conversion price lowers the enrichment at which the fuel cycle cost is minimum for all three cycles, but as well-cost of increased fuel costs, the new minimum for the 10-month cycle is further from the assumed minimum because it lies to the left of curve. In the case of the 24 and 30-month cycles, the new minimum becomes closer to the original 4.3 and 5.5-wt% enrichment changes. The results of fuel cycle cost calculations for varying conversion prices are presented in Figures 3-48 through 3-75 and in Tables E-23 through E-24 of Appendix E.

Effect of Variations in Enrichment Prices

The price of SWU's for the United States has varied in the last 10 years from \$80

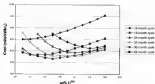


Figure 5-68 Fuel cycle cost comparison of varying cycle lengths with 14-day outages for the first 3 years with conversion costs increased to \$10 a kilogram.

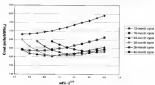


Figure 5-69 Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with conversion costs increased to \$10 a kilogram.

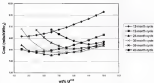


Figure 5-76 Fuel-cycle cost comparison of varying cycle lengths with 18-day outages for the first 3 years with conversion costs increased to \$12.5/kilogram

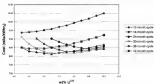


Figure 5-77 Fuel-cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with conversion costs increased to \$12.5/kilogram

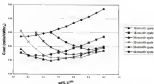


Figure 3-72. Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with conversion costs decreased to \$4 a kilogram

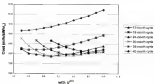


Figure 3-73. Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with conversion costs decreased to \$4 a kilogram

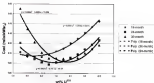


Figure 5-24 Fuel cycle cost comparison with breakevens at the 18, 24, and 30-month cycle with 33-day outage length and conversion costs increased to \$13 per kilogram.

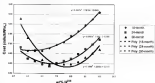


Figure 5-25 Fuel cycle cost comparison with breakevens at the 18, 24, and 30-month cycle with 30-day outage length and conversion costs increased to \$15 per kilogram.

per \$/Btu to the current high of \$118 per \$/Btu (28) as shown in Figure 3-26). The base economic model used a value of \$118 per \$/Btu. Figures 3-18 through 3-27 show that enrichment ranges from 17% to 33% of the total fuel cycle costs. The percentages increase with longer cycle times and shorter outages. A decrease in price of \$/Btu to \$90 per \$/Btu from the advent of a mixed enrichment facility built in the U.S. would increase cost savings to \$283,000 (285.9%) and \$111,000 (71.4%) a year per plant for the 18-month cycle with 15 and 30-day outage lengths if enrichment was increased to 8.5-wt% and 9.5-wt%, respectively. Decreases in the price of \$/Btu of this magnitude increase the enrichment for minimum fuel cycle costs for the 30-day outage plants to 8.5-wt% from 5.5-wt%. Raising the enrichment to 8.5-wt% increases cost savings to \$195,000 (1,448.7%) per year. The cost savings for the 24-month cycle would increase to \$1,760,000 (26.1%) and \$1,594,000 (13.4%) for the 24-month cycle. The 30-month-cycle plants would increase their cost savings to \$1,083,000 (9.4%) and \$4,686,000 (1.3%). A further decrease to \$80 a \$/Btu would increase cost savings to \$378,000 (304.8%) a year for 18-month cycle plants with 15-day outages. The 30-day outage plants would increase savings to \$340,000 (1.173.4%) a year if they increased enrichment to 5.5-wt% and \$283,000 (1,218.4%) if they used 9.5-wt% fuel. Reactors using 24-month-cycle and 15-day and 30-day outages would increase savings to \$1,843,000 (1.1.7%) and \$1,583,000 (28.7%). The 30 month cycle plants would increase savings to \$5,808,000 (3.6%) and \$4,636,000 (2.0%) for 15 and 30-day outages, respectively. In general, for every \$10 decrease per \$/Btu from the \$118 per \$/Btu base cost, the cost savings is increased by \$95,000 (100.2%) and \$49,000 (34.3%) (\$14,000 (773.0%) if modeling to 8.5-wt% instead of 5.5-wt%) per year for 18-month cycle plants with 15 and 30-day outages.

increased by \$11,800 (1.2%) and \$11,000 (0.9%) for 18-month cycle reactors, and increased by \$ 13,800 (0.2%) and \$11,000 (0.7%) per year for 30-month cycle plants. An increase of SWU costs by \$10-a SWU would result in equal but opposite changes. The results of fuel cycle cost calculations with varying SWU prices are presented in Figures 3-77 through 3-84 and Tables E-29 through E-36 of Appendix E.

A 2nd order polynomial (baseline) for the fuel-cycle costs for the 18, 24, and 30-month cycles at a decreased SWU cost of \$10 per SWU is presented in Figures 3-85 and 3-86. The equations for the baselines for the decreased SWU cost of \$10 per SWU are presented in Equations 3-18 through 3-24.

$$FCCT[18 - day]_{baseline} = 0.0344 \cdot year^2 - 0.3761 \cdot year + 0.2360 \quad (3-18)$$

$$FCCT[24 - day]_{baseline} = 0.0473 \cdot year^2 - 0.6647 \cdot year + 0.3493 \quad (3-19)$$

$$FCCT[30 - day]_{baseline} = 0.0772 \cdot year^2 - 1.2381 \cdot year + 0.6383 \quad (3-20)$$

$$FCCT[18 - day]_{baseline} = 0.0344 \cdot year^2 - 0.3766 \cdot year + 0.2099 \quad (3-21)$$

$$FCCT[24 - day]_{baseline} = 0.0468 \cdot year^2 - 0.6332 \cdot year + 0.3192 \quad (3-22)$$

$$FCCT[30 - day]_{baseline} = 0.0752 \cdot year^2 - 1.154 \cdot year + 0.619 \quad (3-23)$$

Differentiating the equations and setting them to zero yields a minimum for the 18-month cycle at 5.50-wt%, 7.21-wt% for the 24-month-cycle, and 7.95-wt% for 30-month-cycle plants with 15-day outages. For 30-day outage plants the minimums become 5.75-wt%, 7.46-wt%, and 7.88-wt% for the 18, 24 and 30 month cycles. A decrease in SWU cost moves the minimum at which the fuel cycle cost is maximum for all these cycles.

In order to fully understand the impact of variations of the SWU costs, the individual fuel cycle costs are plotted in Figures 3-87 through 3-106. As shown in these

figures, the SFWL change using the least cost model is one of the major decrease changes in the fuel cycle cost. Not including outage costs, the in-core capital cost change becomes second only to the SFWL change in contribution greater than 4.1-cent for the 18-month cycle and 24-month cycles and at 3.0-cent for the 30-month-cycle. The in-core capital cost change is very dependent on the cost of SFWLs. Decreasing the SFWL costs from \$118 to \$88 a SFWL, lowers the slope of the plotted in-core capital cost change trendline from 8.2181 for the 18-month cycle, 9.2112 for the 24-month-cycle, and 8.3048 for the 30-month cycle to 0.1800, 0.1740, and 0.1831 for the respective cycle lengths using a 15-day outage. For plants with 30-day outages the slope is lowered from 0.2230 to 0.0840 for the 18-month cycle, from 0.2130 to 0.1712 for the 24-month cycle, and from 0.2818 to 0.1890 for the 30-month cycle. This also increases the threshold value at which the in-core capital cost change begins to decrease over all other changes (excluding SFWL and outage) by approximately 1.0-cent for all three cycles.

The individual fuel cycle costs for the same relative decrease (27%) in fixed costs from \$40 to \$29 are plotted in Figures 5-103 through 5-110. In this case the slopes of the plotted in-core capital cost change trendline is only lowered to 5.3026, 9.2568, and 8.1881 for the 18, 24, and 30-month cycles with 15-day outages. The slope is lowered to 8.2072, 9.1596, and 8.1918 for the 18, 24, and 30-month cycle plants with 30-day outages. A 27% decrease in SFWL costs corresponds to a 17.18% decrease in the slope of the line for the in-core capital cost changes while a similar decrease in uranium fixed costs only lowers the slope by approximately 7%. Table 5-17 presents a listing of the individual fuel cycle contributors to the in-core capital cost change with the percent decrease in its slope for a corresponding 27% decrease in the contributor's base value.

As shown in this table, the in-core capital rate change is strongly coupled to the interest changes. This in-core capital rate change is the strongest contributor to the change of fuel cycle cost curves, which in turn determines the enrichment at which the fuel cycle costs reach a minimum. Figures 5-111 through 5-114 present the individual fuel cycle costs for the 18, 24, and 36-month cycles with 12 and 30-day outages when the conversion costs, fabrication costs, reload licensing costs, and interest rates are reduced by 20%.

Figures 5-115 through 5-118 show the individual fuel cycle costs for the 18, 24, and 36-month cycles when the interest on fuel purchases is set to zero (eliminating the in-core capital rate change) and when the interest rate is increased to 10%. The corresponding fuel cycle cost graphs are shown in Figures 5-119 through 5-122. As shown in these figures, the shape is that of a parabola. Increasing the interest and thus the in-core capital rate change shifts the minimum to the left (lower enrichments) and tightens the parabola, increasing the slope of the endpoints, which would in turn increase the difference in price of fuel cycle costs as the enrichment is varied. A decrease in the in-core capital rate changes shifts the minimum to the right (higher enrichments), decreasing the slope of the endpoints which decreases the relative change of fuel cycle costs as the enrichment is varied.

Effect of Variations in the Cost of Fabrication

A base value of \$250 per kg for fabrication costs was used in the model. As shown in Figures 5-19 through 5-22, this typically represents 1 to 5% of the fuel cycle cost at the optimum fuel cycle enrichment. A 10% increase in fabrication costs increases cost savings for the 18, 24, and 36-month cycles with 12-day outages to \$24,000 (10.8%), \$1,749,000 (13.8%), and \$5,340,000 (17.7%) a year if a switch is made from 5-

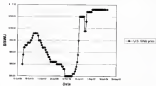


Figure 3-76. Historical price data of NWTs in the United States from The Un-Counting Company, LLC [30].

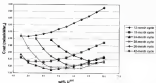


Figure 3-77. Fuel cycle cost component of varying cycle lengths with 15-day outage for the first 3 years with 3%/yr and decreased to 1% p. 3%/yr.

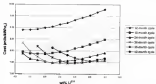


Figure 5-75 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with FNU cost decreased to 50¢ x \$/Btu

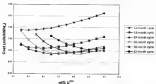


Figure 5-76 Fuel cycle cost comparison of varying cycle lengths with 12-day outage for the first 5 years with FNU cost decreased to 20¢ x \$/Btu

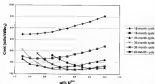


Figure 4-80 Fuel cycle cost comparison of varying cycle lengths with 10-day outages for the first 5 years with SWU cost decreased to \$333 a SWU

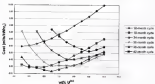


Figure 5-81 Fuel cycle cost comparison of varying cycle lengths with 10-day outages for the first 5 years with SWU cost increased to \$168 a SWU

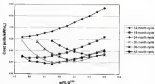


Figure 3-42 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 5 years with SWU cost increased to \$130/gSWU

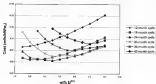


Figure 3-43 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 5 years with SWU cost increased to \$150/gSWU

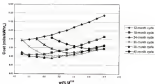


Figure 3-84 Fuel cycle cost component of varying cycle lengths with 30-day outage for the first 3 years with SWU cost increased to \$150 a SWU

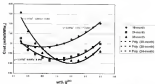


Figure 3-85 Fuel cycle cost comparison with breakeven of the 18-, 24- and 30-month cycle with 15-day outage length and SWU cost decreased to \$80 per SWU

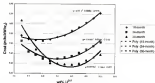


Figure 3-86. Fuel cycle cost comparison with breakeven of the 18, 24, and 36-month cycle with 30-day outage length and SWU cost decreased to \$40 per SWU.

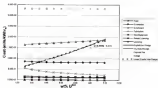


Figure 3-87. Individual cost variations for the 18-month fuel cycle with 15-day outages.

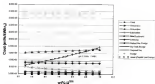


Figure 5-44 Individual cost variations for the 12-month fuel cycle with 30-day outages

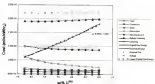


Figure 5-45 Individual cost variations for the 12-month fuel cycle with 15-day outages

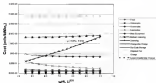


Figure S-98. Individual cost variations for the 18-month fuel cycle with 30-day outages

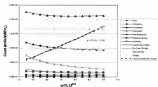


Figure S-99. Individual cost variations for the 24-month fuel cycle with 12-day outages

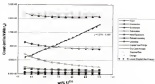


Figure 5-82. Individual cost variations for the 36-month fuel cycle with 30-day outage

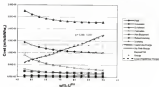


Figure 5-83. Individual cost variations for the 36-month fuel cycle with 15-day outage

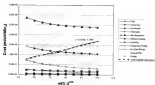


Figure 3-16 Individual cost variations for the 26-month fuel cycle with 30-day margin

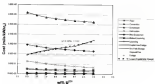


Figure 3-17 Individual cost variations for the 42-month fuel cycle with 30-day margin

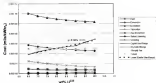


Figure 3-58 Individual cost variations for the 42-month fuel cycle with 30-day outages

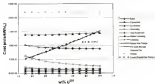


Figure 3-59 Individual cost variations for the 18-month fuel cycle with 15-day outages with 50% cost reduction in 180 a. 50%

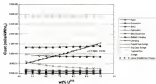


Figure 3-100. Individual cost envelopes for the 18-month fuel cycle with 10-day outage with 54% cost reduced to 540 ± 54%.

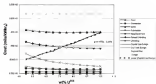


Figure 3-101. Individual cost envelopes for the 24-month fuel cycle with 10-day outage with 54% cost reduced to 540 ± 54%.

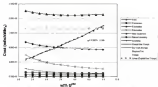


Figure S-112 Individual cost variations for the 36-month fuel cycle with 12-day outage with conversion costs reduced by 20%

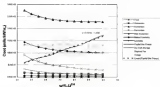


Figure S-113 Individual cost variations for the 36-month fuel cycle with 12-day outage with conversion costs reduced by 20%

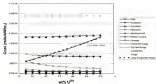


Figure 5-114 Individual cost variations for the 18-month fuel cycle with 30-day outage with construction costs reduced by 33%

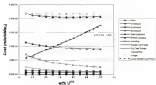


Figure 5-115 Individual cost variations for the 24-month fuel cycle with 30-day outage with construction costs reduced by 33%

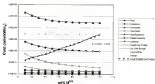


Figure 3-114 Individual cost variations for the 30-month fuel cycle with 30-day outages with decommissioning costs reduced by 25%

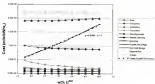


Figure 3-115 Individual cost variations for the 18-month fuel cycle with 15-day outages with decommissioning costs reduced by 25%

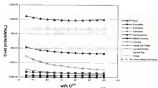


Figure 5-136 Individual cost variations for the 24-month fuel cycle with 15-day outage with interest rate for fuel purchases reduced to zero

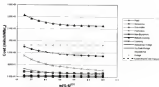


Figure 5-137 Individual cost variations for the 30-month fuel cycle with 15-day outage with interest rate for fuel purchases reduced to zero

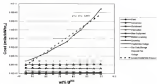


Figure 5-144 Individual cost variations for the 18-month fuel cycle with 30-day outages with interest rate for fuel purchases increased to 20%.

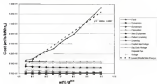


Figure 5-145 Individual cost variations for the 24-month fuel cycle with 30-day outages with interest rate for fuel purchases increased to 20%.

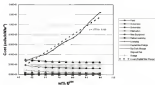


Figure 3-146 Individual cost components for the 30-month fuel cycle with 30-day outage with interest rate for fuel purchases increased to 30%

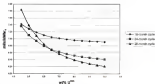


Figure 3-147 Fuel cycle cost comparisons of the 18, 24, and 30-month cycles with 15-day outage length and interest rate on fuel purchases set to zero

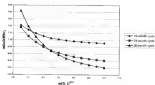


Figure 5-148 Fuel cycle cost comparison of the 18, 24, and 36-month cycles with 18-day outage length and interest rate on fuel purchases set to zero

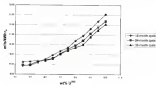


Figure 5-149 Fuel cycle cost comparison of the 18, 24, and 36-month cycles with 18-day outage length and interest rate on fuel purchases set to 30%

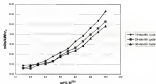


Figure 3-100 Fuel cycle cost comparison of the 18, 24, and 30-month cycles with 30-day outage length and interest rate on fuel purchases set to 30%

with to the respective constant outages. For the 30-day outages, the cost savings are increased to \$9,600 (0.77%), \$1,473,000 (11.4%), and \$4,333,000 (3.1%) with the constant outages for the 18-month cycle increasing to 4.0-with. An increase of 30% in fabrication costs increases cost savings to \$173,000 (20.4%), \$1,811,000 (30.4%), and \$1,498,000 (11.4%) per year for the 18, 24, and 30-month cycles with 15-day outages and \$180,000 (1.32%), \$1,811,000 (31.7%) and \$1,099,000 (12.3%) per year for 30-day outages if a switch is made to the constant of which fuel cycle costs are a minimum for each respective case. In general, for every 10% increase of fabrication costs, the cost savings are increased by \$83,000 (32.4%), \$1,498,000 (30.4%), and \$288,000 (5.7%) per year for 18, 24, and 30-month cycles with 15-day outages. For the 30-day outage plants the savings are increased by \$30,000 (33.3%) for an increase to 3.5-with or \$80,000 (17.7%) if 4.0-with instead of 3.5-with is chosen for the 18-month

cycle \$153,000 (0.4%) for the 24-month cycle, and \$271,000 (0.1%) per year for the 36-month cycle. Decreases of the same magnitude in fabrication costs would result in equal but opposite changes. The results from these calculations are presented in Figures 5-150 through 5-158 and in Tables E-28 through E-30 of Appendix E.

A 3rd order polynomial trendline for the fixed cycle costs for the 18-, 24-, and 36-month cycles with a 20% increase in fabrication costs is presented in Figures 5-159 and 5-160. The equations for the trendlines for increased fabrication costs are presented in Equations 5-25 through 5-30.

$$FCCT[18 - day]_{20\%+cost} = 0.0363 \cdot cost^3 - 0.4143 \cdot cost + 5.0767 \quad (5-25)$$

$$FCCT[24 - day]_{20\%+cost} = 0.0031 \cdot cost^3 - 0.7315 \cdot cost + 10.474 \quad (5-26)$$

$$FCCT[36 - day]_{20\%+cost} = 0.0004 \cdot cost^3 - 1.4387 \cdot cost + 13.385 \quad (5-27)$$

$$FCCT[18 - day]_{20\%+cost} = 0.0099 \cdot cost^3 - 0.7349 \cdot cost + 9.9613 \quad (5-28)$$

$$FCCT[24 - day]_{20\%+cost} = 0.002 \cdot cost^3 - 0.7134 \cdot cost + 10.187 \quad (5-29)$$

$$FCCT[36 - day]_{20\%+cost} = 0.0003 \cdot cost^3 - 1.3218 \cdot cost + 11.266 \quad (5-30)$$

Differentiating the equations and setting them to zero yields a minimum for the 18-month cycle at 3.71-wt%, 7.08-wt% for the 24-month-cycle, and 7.87-wt% for 36-month cycle plants with 15-day outages. For 30-day outage plants the minimums become 3.50-wt%, 6.90-wt%, and 7.79-wt% for the 18-, 24-, and 36-month cycles. As increases in fabrication costs raises the enrichment at which the fixed cycle cost is minimum for all three cycles.

Effect of Variations in Refuel Loading Costs

A base cost of \$1,000,000 for refuel loading was used in the model. As shown

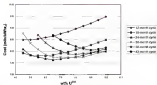


Figure 3-131 First cycle cost comparisons of varying cycle lengths with 13-day outage for the first 3 years with fabrication costs increased by 10%

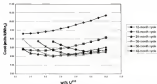


Figure 3-132 First cycle cost comparisons of varying cycle lengths with 24-day outage for the first 3 years with fabrication costs increased by 10%

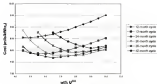


Figure 5-133 Fuel cycle cost comparison of varying cycle lengths with 15-day outages for the first 5 years with fabrication costs increased by 20%

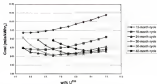


Figure 5-134 Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 5 years with fabrication costs increased by 20%

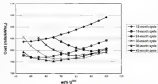


Figure 5-153: Fuel cycle-cost comparison of varying cycle lengths with 33-day outage for the first 3 years with fabrication costs decreased by 10%.

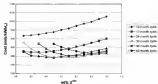


Figure 5-156: Fuel cycle-cost comparison of varying cycle lengths with 30-day outage for the first 3 years with fabrication costs decreased by 10%.

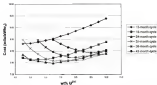


Figure 3-137 Fuel cycle cost comparison of varying cycle lengths with 13-day outage for the first 3 years with fabrication costs decreased by 20%.

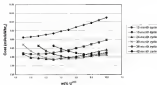


Figure 3-138 Fuel cycle cost comparison of varying cycle lengths with 34-day outage for the first 3 years with fabrication costs decreased by 20%.

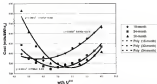


Figure 5-129 Fuel cycle cost comparison with breakevens of the 18, 24, and 36-month cycle with 15-day outage length and fabrication costs increased by 20%.

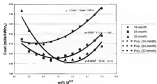


Figure 5-130 Fuel cycle cost comparison with breakevens of the 18, 24, and 36-month cycle with 18-day outage length and fabrication costs increased by 20%.

in Figures 3-18 through 3-21, this typically represents only 1% of the fuel-cycle cost of the respective fuel cycle systems. If reloid licensing costs are decreased by 25%, cost savings for the 18, 24, and 36-month cycles with 15-day outages are increased for \$105,800 (12.7%), \$1,609,000 (8.7%), and \$5,043,000 (8.7%) a year if a credit is made from 5-yr to the respective enrichment minimums. Plants with a 30-day outage increase cost savings to \$29,000 (3.1%), \$1,334,000 (1.1%), and \$4,977,000 (6.5%) per year. A 50% decrease in reloid licensing costs increases the cost savings to \$115,000 (12.7%), \$1,622,000 (1.7%), and \$5,095,000 (8.7%) per year for 15-day outages. Plants with 30-day outages would increase cost savings to \$29,800 (1.2%), \$1,349,000 (1.7%), and \$4,948,000 (6.5%) per year. In general, for every 10% decrease in reloid licensing costs, the cost savings for 15-day outage plants are increased by \$12,000 (1.27%), \$11,000 (0.8%), and \$11,000 (0.27%) for the 18, 24, and 36-month cycles. Plants with 30-day outages would increase their savings by \$4,000 (34.1%), \$74,000 (1.7%), and \$11,000 (8.7%) increases to the reloid licensing costs of the same magnitude would have equal but opposite changes. The results from these calculations are presented in Figures 3-181 through 3-188 and in Tables E-46 through E-53 of Appendix E.

A 2nd order polynomial trendline for the fuel cycle costs for the 18, 24, and 36-month cycles with an increase of 50% in reloid licensing costs is presented in Figures 3-169 and 3-170. The equations for the trendlines for a 20% increase in reloid licensing costs are presented in Equations 3-31 through 3-34.

$$FCC7(5\text{-day})_{\text{fuel},20\%} = 0.004 \text{ } \text{mcr}^2 + 0.347 \text{ } \text{mcr} + 0.8214 \quad (3-31)$$

$$FCC7(18\text{-day})_{\text{fuel},20\%} = 0.002 \text{ } \text{mcr}^2 + 0.7167 \text{ } \text{mcr} + 10.137 \quad (3-32)$$

$$FCCCT(15 - day)_{best-fit} = 0.0017 \cdot cost^2 - 1.1362 \cdot cost + 12.636 \quad (5-13)$$

$$FCCCT(25 - day)_{best-fit} = 0.0034 \cdot cost^2 - 0.3802 \cdot cost + 9.2996 \quad (5-14)$$

$$FCCCT(40 - day)_{best-fit} = 0.0061 \cdot cost^2 - 0.6562 \cdot cost + 10.264 \quad (5-15)$$

$$FCCCT(60 - day)_{best-fit} = 0.0012 \cdot cost^2 - 1.291 \cdot cost + 12.336 \quad (5-16)$$

Differentiating the equations and setting them to zero yields a maximum for the 15-month cycle at 5.47-wt%, 4.93-wt% for the 25-month cycle, and 7.80-wt% for 35-month cycle plants with 15-day outages. For 30-day outage plants the maximum becomes 5.25-wt%, 4.73-wt%, and 7.73-wt% for the 15, 25, and 35 month cycles. Increases in refuel increasing costs result in very small increases in the enrichment at which the fuel cycle cost is minimum for all three cycles.

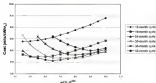


Figure 5-18 Fuel cycle cost comparison of varying cycle lengths with 15-day outages for the first 3 years with refuel increasing costs decreased by 33%.

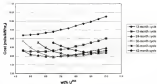


Figure 5-162. Feed-cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with related licensing costs decreased by 25%.

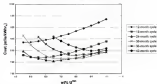


Figure 5-163. Feed-cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with related licensing costs decreased by 25%.

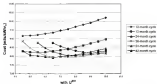


Figure 3-164 Fuel cycle cost comparison of varying cycle lengths with 16-day outages for the first 5 years with initial financing costs decreased by 50%

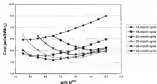


Figure 3-165 Fuel cycle cost comparison of varying cycle lengths with 13-day outages for the first 5 years with initial financing costs increased by 25%

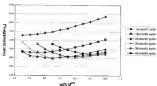


Figure 3-36A Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with varied (increasing) loads increased by 25%.

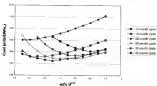


Figure 3-36B Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with varied (increasing) loads increased by 50%.

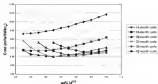


Figure 5-144. Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with reload forming costs increased by 50%.

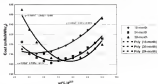


Figure 5-145. Fuel cycle cost comparison with median of the 18, 24, and 30-month cycle with 15-day outage length and reload forming costs increased by 50%.

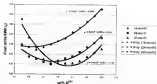


Figure 5-136 Fuel cycle cost comparison with breakevens of the 18-, 24-, and 30-month cycle with 30-day outage length and relaxed licensing costs increased by 50%.

Effect of Variations in the Cost of Replacement Power

A base cost of $25 \frac{\text{mils}}{\text{kWh}} \frac{\text{hr}}{\text{day}}$ for replacement power was used in the model. As

shown in Figures 5-18 through 5-17, the outage ratio (which includes 330 million in labor) represents from 12 to 47% of the fuel cycle cost at three respective replacement cost rates. The percentage increases as the outage length increases and the cycle length decreases. The equations for the breakeven for a 50% increase in replacement power costs are presented in Equations 5-27 through 5-32.

$$FCCT(18-\text{day})_{\text{breakeven}} = 0.0158 \text{ } \text{mils}^2 - 0.1681 \text{ } \text{mils} + 0.663 \quad (5-27)$$

$$FCCT(24-\text{day})_{\text{breakeven}} = 0.0018 \text{ } \text{mils}^2 - 0.0734 \text{ } \text{mils} + 0.42 \quad (5-28)$$

$$FCCT(30-\text{day})_{\text{breakeven}} = 0.0008 \text{ } \text{mils}^2 - 0.1142 \text{ } \text{mils} + 0.219 \quad (5-29)$$

$$FCCP[30 - day]_{\text{opt},\text{opt}} = 0.0046 \text{ } \omega^2 - 0.2509 \text{ } \omega + 14.346 \quad (3-40)$$

$$FCCP[30 - day]_{\text{opt},\text{opt}} = 0.0495 \text{ } \omega^2 - 0.0292 \text{ } \omega + 11.262 \quad (3-41)$$

$$FCCP[30 - day]_{\text{opt},\text{opt}} = 0.0811 \text{ } \omega^2 - 1.2808 \text{ } \omega + 13.38 \quad (3-42)$$

Differentiating the equations and setting them to zero yields the same minimum.

minimum in the base economic model. Variations of the replacement power cost do not affect the minimum at which specific cycle lengths have their minimum fuel cycle cost.

Variations in the replacement power costs do, however, affect the cost savings or loss

from switching to one-cycle lengths or another. Using the base model values: a reactor

with an 18-month cycle using 3.0-yr/1 fuel and 15-day outages would lose \$29,800 a year

if it were to switch to a 24-month cycle. Reactors with a 30-day outage would save

\$1,543,800 if they switched from an 18-month to 24-month cycle. An increase of

replacement power costs to $30 \frac{\text{mills}}{\text{kWh} \cdot \text{hr}}$ results in a gain of \$271,000 (3.4 %) saved per

year for the 18-month-cycle with 15-day outages by switching to a 24-month-cycle. For

30-day outages, the cost savings is increased to \$2,143,000 (28.7%) per year. If the

replacement power cost is doubled to $50 \frac{\text{mills}}{\text{kWh} \cdot \text{hr}}$, the cost savings are increased to

\$3,471,000 (4,972.4%) and \$4,343,000 (3.84-4%) a year for the 15-day and 30-day-outage

lengths. A reduction of replacement power costs to $10 \frac{\text{mills}}{\text{kWh} \cdot \text{hr}}$ would result in a loss of

\$29,800 (-1.134.7%) and a gain of \$943,800 (-38.7%) a year. A further reduction to 5

$\frac{\text{mills}}{\text{kWh} \cdot \text{hr}}$ yields a loss of \$629,000 (-22,889.0%) a year for the 15-day outage and a

reduced savings to \$343,000 (-7.77%) a year for the 30-day outage. In general, the every

3 $\frac{\text{mills}}{\text{dollar}} \frac{\text{dollar}}{\text{dollar}}$ for replacement power cost is increased), the savings are increased by

\$300,000 (1034.3%) per year for 15-day storage plants by going from an 18-month cycle to 24 months, and \$450,000 (2118%) per year if the storage length is 30 days. The results from these calculations are presented in Figures 5-17i through 5-180 and in Tables E-34 through E-61 of Appendix E.

Effect of Variations in the Cost of Dry-Cask Storage

A base charge of \$100 per kg for dry cask storage was used in the model. As shown in Figures 5-19 through 5-57, this typically represents only 2 or 3% of the fuel cycle cost at the negative fuel cycle maximums. A 10% increase in the cost of dry cask storage increases cost savings for the 18, 24, and 30-month cycles with 15-day storage to \$115,000 (41.2%), \$1,460,000 (4.0%), and \$1,181,000 (2.2%) a year if they replace them 3-month to their respective enrichment maximums. For the 30-day storage the cost savings

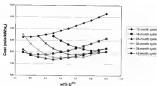


Figure 5-17i Fuel cycle cost comparison of varying cycle lengths with 15-day storage for the first 3 years with replacement power costs increased to 18 $\frac{\text{mills}}{\text{dollar}} \frac{\text{dollar}}{\text{dollar}}$

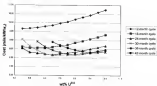


Figure 3-131 Fuel cycle cost comparison of varying cycle lengths with 30-day outage

for the first 5 years with replacement power costs increased to $20 \frac{\text{cents}}{\text{Btu} \cdot \text{day}}$

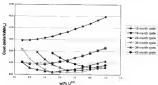


Figure 3-133 Fuel cycle cost comparison of varying cycle lengths with 15-day outage

for the first 5 years with replacement power costs increased to $50 \frac{\text{cents}}{\text{Btu} \cdot \text{day}}$

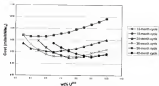


Figure S-134 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with replacement power costs increased to 50 $\frac{\text{mills}}{\text{kWh}}$ ΔC_r

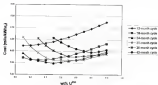


Figure S-175 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with replacement power costs decreased to 20 $\frac{\text{mills}}{\text{kWh}}$ ΔC_r

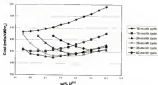


Figure 3-176. Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with replacement power costs decreased to $20 \frac{\text{mills}}{\text{kWh} \cdot \text{day}}$

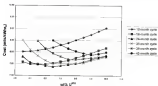


Figure 3-177. Fuel cycle cost comparison of varying cycle lengths with 15-day outages for the first 3 years with replacement power costs decreased to $15 \frac{\text{mills}}{\text{kWh} \cdot \text{day}}$

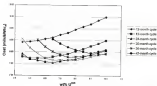


Figure 3-175: Fuel cycle cost-comparison of varying cycle lengths with 30-day outage for the first 5 years with replacement; power costs decreased to $15 \frac{\text{mil}}{\text{MWh}} \cdot \text{yr}$.

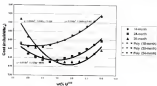


Figure 3-176: Fuel cycle cost-comparison with breakeven of the 18, 24, and 36-month cycle with 30-day outage lengths and replacement power costs increased to $30 \frac{\text{mil}}{\text{MWh}} \cdot \text{yr}$.

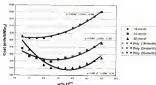


Figure 5-140 Fuel cycle cost comparison with trendlines of the 18, 24, and 30-month cycle with 30-day outage length and replacement power costs increased to $10 \frac{\text{mills}}{\text{kWh}}$

are increased to \$71,860 (160.4%), \$1,381,008 (4.7%), and \$4,654,008 (2.4%) with the replacement minimum for the 18-month cycle increasing to 6.8-mills. An increase of 30% to dry stack storage costs increases cost savings to \$166,500 (32.4%), \$1,734,000 (8.1%), and \$3,398,000 (8.3%) per year for the 18, 24, and 30-month cycles with 15-day outages and \$71,000 (477.4%), \$1,443,000 (8.3%), and \$4,754,000 (4.8%) per year for 30-day outages. In general, for every 10% increase, the cost savings are increased by \$34,500 (4.1%), \$64,000 (4.0%), and \$113,000 (2.7%) per year for 18, 24, and 30-month cycles with 15-day outages. For the 30-day outage plans the savings are increased by \$26,800 (110.4%), 46.8 mills instead of 6.8-mills is chosen for the 18-month cycle, \$62,000 (4.7%) for the 24-month cycle, and \$88,000 (2.4%) per year for the 30-month cycle. Decreases of the same magnitude in dry stack storage costs would result in equal but opposite changes. The results from these calculations are presented in Figure 5-141.

through 3-690 and in Tables E-42 through E-71 of Appendix E.

A 2nd order polynomial trendline for the fuel cycle costs for the 18, 24, and 30-month cycles with a 30% increase in the cost of dry cask storage is presented in Figures 3-183 and 3-482. The equations for the trendlines for increased-dry cask storage costs are given in Equations 3-43 through 3-48.

$$FCCT[18 - dry]_{\text{increased}} = 0.0362 \cdot \text{wtf}^2 - 0.4120 \cdot \text{wtf} + 9.6503 \quad (3-43)$$

$$FCCT[24 - dry]_{\text{increased}} = 0.0331 \cdot \text{wtf}^2 - 0.3768 \cdot \text{wtf} + 10.445 \quad (3-44)$$

$$FCCT[18 - dry]_{\text{increased}} = 0.0499 \cdot \text{wtf}^2 - 1.4257 \cdot \text{wtf} + 13.268 \quad (3-45)$$

$$FCCT[24 - dry]_{\text{increased}} = 0.0458 \cdot \text{wtf}^2 - 1.3933 \cdot \text{wtf} + 9.4747 \quad (3-46)$$

$$FCCT[30 - dry]_{\text{increased}} = 0.0319 \cdot \text{wtf}^2 - 0.3162 \cdot \text{wtf} + 10.239 \quad (3-47)$$

$$FCCT[30 - dry]_{\text{increased}} = 0.0432 \cdot \text{wtf}^2 - 1.3284 \cdot \text{wtf} + 12.181 \quad (3-48)$$

Differentiating the equations and setting them to zero yields a minimum for the 18-month cycle at 5.73-wtf, 7.86-wtf for the 24-month cycle, and 7.87-wtf for 30-month cycle plants with 15-day wetlegs. For 30-day caskage plants the minimums become 3.50-wtf, 6.76-wtf, and 7.82-wtf for the 18, 24, and 30-month cycles. An increase in dry cask storage costs raises the enrichment at which the fuel cycle cost is minimum for all three cycles.

Effect of Variations in the Final Disposal Fee

A base fee of $\frac{\text{wtf}}{200}$ was used in this model. This is a flat rate fee charged to

utilities on the amount of electricity generated and sold from nuclear plants. This fee is used to finance nuclear waste fund to provide for the permanent disposal of civilian

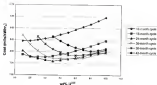


Figure 5-181: Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 3 years with dry cask storage costs increased by 10%.

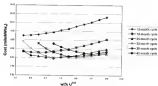


Figure 5-182: Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 3 years with dry cask storage costs increased by 10%.

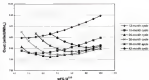


Figure 3-443 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with dry waste storage costs increased by 30%

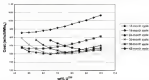


Figure 3-444 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with dry waste storage costs increased by 30%

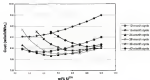


Figure 5-183 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with dry cask storage costs increased by 100%

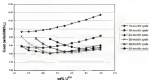


Figure 5-184 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with dry cask storage costs increased by 100%

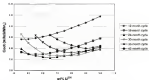


Figure 3-187 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with dry cask storage costs decreased by 10%.

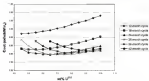


Figure 3-188 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with dry cask storage costs decreased by 10%.

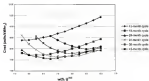


Figure 5-185 Post cycle cost comparison of varying cycle lengths with 12-day outage for the first 5 years with dry-cask storage costs decreased by 30%

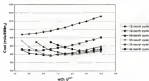


Figure 5-190 Post cycle cost comparison of varying cycle lengths with 24-day outage for the first 5 years with dry-cask storage costs decreased by 30%

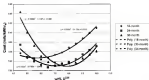


Figure 5-151. Fuel-cycle cost comparison with goodness of the 18, 24, and 36-month cycle with 15-day average length and dry oak storage costs decreased by 30%.

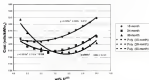


Figure 5-152. Fuel-cycle cost comparison with goodness of the 18, 24, and 36-month cycle with 30-day average length and dry oak storage costs increased by 30%.

nuclear waste. Because β is a flat fee, increases or decreases in the flat fee have no effect on the number of assemblies at which individual fuel cycles have their minimums nor is there any incentive to use a greater number of assemblies. In order to see the possible effects of a change in the way flat fee is assessed, a sample calculation is done. The waste disposal fee is modified so that it is based on the number of batches used. The new fee, DF_{β} , is calculated as shown in Equation 3-49:

$$DF_{\beta} = \beta \left(\frac{LDF}{\text{batches}} \right) \left(1 - \frac{DF}{L_f} \right) \quad (3-49)$$

The only modification to the original disposal fee calculation is the multiplication by a factor of β and the division of the number of batches in the term. A 3 batch-core would still be assessed a $\beta \left(\frac{LDF}{3} \right) \left(1 - \frac{DF}{L_f} \right)$ disposal fee. Plants using more batches and thus fewer assemblies, would be assessed smaller fees. A fee assessment policy such as this would encourage the use of fewer assemblies and in turn fewer spent fuel assemblies would have to be put into a permanent disposal area.

Under the second fee assessment policy, 18-month cycle plants with a 13 day outage could save \$2,126,000 by increasing their fuel enrichment to 4.5-wt%. The enrichment fuel cycle cost maximum for the 18-month cycle plants are increased to 4.6-wt% and moving to this enrichment would save \$4,579,800 a year. The 30 month cycle would increase its enrichment maximum to 4.5-wt% and would save \$4,277,000 a year. For the 30-day outage plants, the fuel cycle cost maximums occur at the same enrichments and would have cost savings of \$1,757,800, \$5,878,000, and \$1,029,000 a year. The results of the calculations for this second disposal fee assessment are presented in Figures 3-4-93 and 3-4-94 and in Tables E-11 through E-13 of Appendix E.

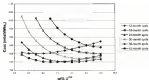


Figure 5-193. Pool-cycle cost comparison of varying cycle lengths with 15-day storage for the first 5 years with annual disposal fee assessment

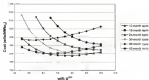


Figure 5-194. Pool-cycle cost comparison of varying cycle lengths with 30-day storage for the first 5 years with annual disposal fee assessment

Effect of Variations in the Fuel Purchase Interest Rate

A fuel purchase loan interest rate of 7% was used in the model. As shown in Figures 3-18 through 3-27, fuel interest rate causes the so-called capital cost charge to be 7 to 10% of the fuel cycle cost at the respective fuel cycle minimums. The percentages increase with longer cycle times and shorter outages. Fuel can be purchased at interest rates in the 3% to 6% range, if short-term interest rates are used. Figures 3-183 through 3-193 compare the fuel cycle costs when the interest rate on fuel purchases is lowered to these rates. A decrease of the interest rates for fuel purchases from the base model of 7% to 6% increases cost savings for the 18, 24, and 30 month-cycles with 15-day outages to \$414,890 (23.4%), \$2,801,008 (28.7%), and \$4,982,000 (34.2%) a year if they reach their 3-wk to their respective maximum minimums, with the minimum for the 30-month cycle now at 6.3-wk. For the 18-day outage the cost savings are increased to \$117,600 (2.14%), \$1,799,800 (21.7%), and \$5,401,008 (31.4%) with the maximum minimum for the 18-month cycle increasing to 6.3-wk and the 30-month maximum minimum increased to 6.0-wk. A further decrease to an interest rate of 5% increases cost savings to \$699,890 (34.6%), \$2,494,008 (36.0%), and \$6,982,000 (38.3%) per year for the 18, 24, and 30 month cycle with 15-day outages. The fuel cycle cost minimums occur at enrichment levels of 6.8-wk, 7.8-wk, and 8.5-wk. If an outage length of 28 days is used, the cost savings are \$106,000 (4.628 3%), \$2,304,008 (37.2%), and \$6,192,000 (34.2%) if enrichment are increased to 6.8-wk, 6.3-wk, and 8.3-wk for the 18, 24, and 30-month cycles.

A 2nd order polynomial equation for the fuel cycle cost for the 18, 24, and 30-month cycles with a decrease of fuel purchase interest rates to 5% is presented in Figure

5-199 and 5-200. The equations for the minimums for the decreased fuel purchase interest rates are given in Equations 5-50 through 5-53.

$$FCCT[15] - \text{dep}_{\text{15-day}}^* = 0.0288 \cdot \text{int}^2 + 0.3820 \cdot \text{int} + 0.6414 \quad (5-50)$$

$$FCCT[15] - \text{dep}_{\text{15-day}}^* = 0.0668 \cdot \text{int}^2 + 0.2234 \cdot \text{int} + 0.8214 \quad (5-51)$$

$$FCCT[15] - \text{dep}_{\text{15-day}}^* = 0.0291 \cdot \text{int}^2 + 0.3148 \cdot \text{int} + 0.2542 \quad (5-52)$$

$$FCCT[16] - \text{dep}_{\text{16-day}}^* = 0.0279 \cdot \text{int}^2 + 0.2211 \cdot \text{int} + 0.6264 \quad (5-53)$$

$$FCCT[16] - \text{dep}_{\text{16-day}}^* = 0.0438 \cdot \text{int}^2 + 0.0476 \cdot \text{int} + 0.6599 \quad (5-54)$$

$$FCCT[16] - \text{dep}_{\text{16-day}}^* = 0.0498 \cdot \text{int}^2 + 0.2152 \cdot \text{int} + 0.2442 \quad (5-55)$$

Differentiating the equations and setting them to zero yields a minimum for the 18-month cycle at 6.66-wt%, 7.73-wt% for the 24-month cycle, and 8.75-wt% for 36-month cycle plants with 15-day outages. For 30-day outage plants the minimums become 5.58-wt%, 6.78-wt%, and 7.88-wt% for the 18-, 24- and 36-month cycles. Further calculations were done with fuel purchase interest rates set to 4, 5, 10, and 12% and are presented in Figures 5-201 through 5-208 and in Tables E-74 through E-85 of Appendix E. The minimums for minimums at the varying interest rates are given in Table E-86. Decreases in the fuel purchase interest rate means the enrichment at which the fuel cycle cost is minimum for all three cycles.

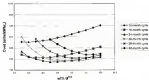


Figure 5-115 Fuel cycle cost comparison of varying cycle lengths with 17-day outages for the first 3 years with fuel purchase interest rate decreased to 6%.

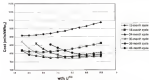


Figure 5-116 Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 3 years with fuel purchase interest rate decreased to 6%.

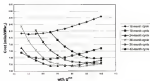


Figure 3-181 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 3 years with fuel purchase interest rate decreased to 3%

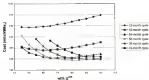


Figure 3-182 Fuel cycle cost comparison of varying cycle lengths with 10-day outage for the first 5 years with fuel purchase interest rate decreased to 3%

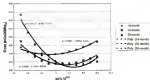


Figure 3-199 Fuel cycle cost comparison with irradiance of the 14-, 24-, and 30-month cycle with 15-day outage length and fuel purchase interest rate decreased to 3%.

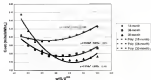


Figure 3-200 Fuel cycle cost comparison with irradiance of the 14-, 24-, and 30-month cycle with 30-day outage length and fuel purchase interest rate decreased to 3%.

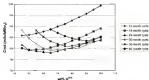


Figure S-104 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with fuel purchase nearest rate removed in 1974

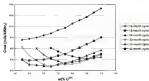


Figure S-105 Fuel cycle cost comparison of varying cycle lengths with 18-day outage for the first 5 years with fuel purchase nearest rate removed in 1974

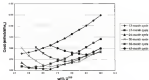


Figure 5-353 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with fuel purchase interest rate increased to 9%.

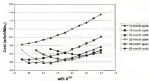


Figure 5-354 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with fuel purchase interest rate increased to 9%.

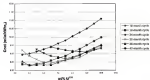


Figure 3-269 Fuel cycle cost comparison of varying cycle lengths with 17-day outages for the first 3 years with fuel purchase interest rate assumed to 10%.

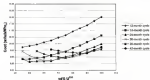


Figure 3-268 Fuel cycle cost comparison of varying cycle lengths with 33-day outages for the first 3 years with fuel purchase interest rate assumed to 10%.

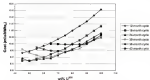


Figure 3-267 Fuel cycle cost comparison of varying cycle lengths with 13-day outage for the first 5 years with fuel purchase interest rate increased to 12%.

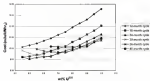


Figure 3-268 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with fuel purchase interest rate increased to 12%.

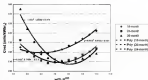


Figure 5-204 Fuel cycle cost comparison with conditions of the 18, 24, and 30 month cycle with 10-day outage length and fuel purchase interest rate decreased to 40%.

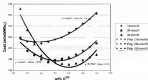


Figure 5-210 Fuel cycle cost comparison with conditions of the 18, 24, and 30 month cycle with 30-day outage length and fuel purchase interest rate decreased to 40%.

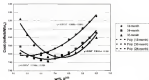


Figure 5-111 Fuel cycle cost comparison with breakevens of the 18, 24, and 30-month cycle with 15-day average length and fuel purchase contract rate increased to 12%.

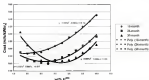


Figure 5-112 Fuel cycle cost comparison with breakevens of the 18, 24, and 30-month cycle with 30-day average length and fuel purchase contract rate increased to 12%.

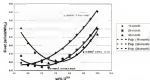


Figure 3-213 Feed cycle cost comparison with feedlines of the 14, 24, and 30-month cycle with 15-day average length and feed purchase increment rate increased to 9%.

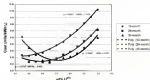


Figure 3-214 Feed cycle cost comparison with feedlines of the 14, 24, and 30-month cycle with 30-day average length and feed purchase increment rate increased to 9%.

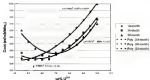


Figure 5-115 Fuel cycle cost comparison with windiness of the 24-, 29-, and 30-month cycle with 15-day outage length and fuel purchase contract rate increased to 100%.

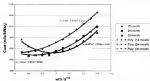


Figure 5-116 Fuel cycle cost comparison with windiness of the 19-, 24-, and 30-month cycle with 30-day outage length and fuel purchase contract rate increased to 100%.

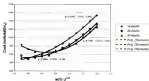


Figure 5-217 Fuel cycle cost comparison with breakeven of the 18-, 24-, and 30-month cycle with 12-day average length and full purchase interest rate assumed to 12%.

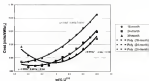


Figure 5-218 Fuel cycle cost comparison with breakeven of the 18-, 24-, and 30-month cycle with 30-day average length and full purchase interest rate assumed to 12%.

CHAPTER 4 CONCLUSIONS

Research indicates that increasing requirements to 10 0-wft/L²⁰⁰ is a viable option for most of today's equipment. The economic model indicates that there is little incentive for plants using the 10-month cycle to increase requirements. For the two-year models, the 20-month cycle is the most competitive. Up to 5 0-wft is an attractive option economically for the 20-month cycle with interest rates up to 5 0%. It is suggested that a minimum of two cycles on a 20-month cycle participate in any program to increase requirements in order for there to be an economic incentive to do so. A single reactor developing a 20-month cycle could see significant savings in such a program. Longer fuel cycles could only be achieved with requirements greater than the currently licensed 3 0-wft/L²⁰⁰ limit. These longer cycles would still have fuel cycle cost requirements in the range of 3 0 to 5 0-wft/L²⁰⁰, and, therefore, it is concluded that increasing fuel equipment modification beyond this point would be unnecessary for current PWR's in the United States.

Increasing core costs lower the enrichment at which the fuel cycle has its minimum fuel cycle cost. Even with a 100% increase in core cost there are still significant savings in going from the 3 0-wft/L²⁰⁰ to higher requirements for the 20 and 30-month cycles. Increasing conversion costs will also lower the requirements for the fuel cycle cost minimum but since conversion is typically only one to three percent of the total fuel cycle costs, its effect on the enrichment minimum and cost savings is relatively minor.

In comparison, changes to the SPW costs have a much greater impact on fuel cycle enrichment requirements and potential cost savings. Figure 6-1 shows a sensitivity study for a typical fuel cycle using enriched enrichment. In this case the enrichment is the largest component and has the greatest effect on the overall fuel cycle cost. As shown in Figures 6-2 and 6-3, a 100% increase in SPW prices would still not eliminate incentives for going to higher enrichments. Although the 24-month cycle would still see some savings, the 18-month cycle becomes the cheapest fuel cycle length and has enrichments of 3-wt% or less. Figures 6-4 and 6-5 show a 50% decrease in SPW costs. In this case, not only is there incentive to increase enrichments, the longer fuel cycles become competitive.

Increases in fabrication cost also move the cost savings from enriched enrichment. Figures 6-6 and 6-7 compare the fuel cycle costs when the fabrication charges are increased by 100%. For the 18-day outage the 24-month cycle remains the most competitive but the 30-day outage has a minimum fuel cycle cost using the 30-month cycle at an enrichment of 3.0-wt%. There is only a 9% difference between the total savings of a 24-month cycle going from 5.0-wt% to 6.0-wt% and the same plant going to the longer 30-month cycle with 6.0-wt% fuel. Increases of dry waste storage costs have a smaller effect but in reverse degree. Figures 6-8 and 6-9 compare the fuel cycle costs when the cost of dry waste storage is increased by 100%. In this case the 24-month cycle is the most cost effective for both outage lengths, but the 30-month cycle is a very close second at 6.0-wt% fuel for the 18-day outage case.

Raised licensing variations have little effect on cost savings for going to higher enrichments. Figures 6-10 and 6-11 compare the fuel cycle costs when the raised licensing costs are increased by 100%. There is little effect seen on the shape of the fuel

cycle cost curves, what is changed is the vertical position of the cycle lengths. As wheel turning costs are reduced, the longer cycles become more competitive. Variations in replacement power costs have a similar effect. An increase in replacement power cost also increases the potential cost savings of going to longer cycle lengths. Variations in the disposal fee have no effect on cost savings of increasing wheelturns or cycle lengths. Modifications to the way the line is assessed in order to encourage the use of lower wheelturns could potentially encourage the use of higher wheelturns by increasing the cost savings by millions per year.

Fuel purchase interest rates are the dominant factor in determining the cost savings or loss in using higher than 3-with fuel. At fuel purchase interest rates of 4 to 7% the economic model shows a potential savings of over 2 million dollars per year for reactors using a 24-month cycle and a savings of 3 to 4 million dollars per year if reactors were to develop a 36-month cycle. Increases in interest rates could result in very large losses if reactors were to go to higher wheelturns. As long as the participating reactors did not contract to use the higher wheelturns but only to pay for the licensing and equipment upgrades for the ability to go to higher wheelturns they could maximize any potential losses. If a program is developed with 10 participating reactors, even if interest rates on purchase of fuel were raised to 10%, reactors on a 24-month cycle could go back to using 3-with fuel and only experience an investment loss of approximately \$100,000 each year for a maximum of 3 years. Any time after that 3 year period, if the interest rates dropped and the utility purchased 4.5-with fuel at 7% interest then each plant could potentially save 1.4 to 1.7 million dollars a year depending on the outage length. Fuel purchase at an interest rate of 7% would mean the 3 year loss is less than a year

While rising interest rates may deter participating plants from using higher commitments, there is a potential savings of millions of dollars per year. Figures 4-12 and 4-13 display the monthly average Federal Funds interest rate over the last 30 years and the yearly average over the last 50 years [34]. The interest rate is currently at 1% but has been as high as 11.50% in the last 30 years and 19.10% (June, 1982) in the last 50 years. The model indicates that in order to see a savings from increased commitments in the first five years, the interest rate on purchases of fuel must be in the range of 5-9% or less. Although interest rates are volatile, the potential gain appears to outweigh any loss that could be seen by increased commitments beyond the current burning limit of 3-mth L^{90%}.

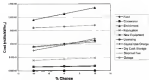


Figure 4-1. Sensitivity study of fuel cycle components to change for typical scenarios: fuel cycle (2% annual, 4-3-mth, 13-day storage).

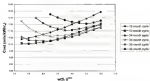


Figure 6-2 Fuel cycle cost comparison of varying cycle lengths with 12-day outages for the first 3 years with SFU cost increased by 100%

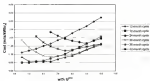


Figure 6-3 Fuel cycle cost comparison of varying cycle lengths with 10-day outages for the first 3 years with SFU cost increased by 100%

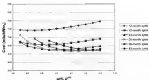


Figure 4-4 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with SNU cost decreased by 50%

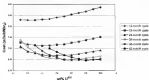


Figure 4-5 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with SNU cost decreased by 50%

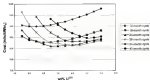


Figure 4-1 Fuel cycle cost comparison of varying cycle lengths with 15-day outage for the first 5 years with fabrication costs increased by 100%

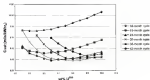


Figure 4-2 Fuel cycle cost comparison of varying cycle lengths with 30-day outage for the first 5 years with fabrication costs increased by 100%

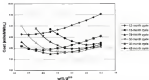


Figure 4-4 Fuel cycle cost comparison of varying cycle lengths with 15 day outages for the first 5 years with the cost of dry waste storage increased by 100%.

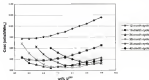


Figure 4-5 Fuel cycle cost comparison of varying cycle lengths with 30-day outages for the first 5 years with the cost of dry waste storage increased by 100%.

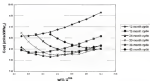


Figure 4-10 Fuel cycle cost comparison of varying cycle lengths with 10-day outages for the first 3 years with reload/burning costs increased by 100%

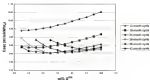


Figure 4-11 Fuel cycle cost comparison of varying cycle lengths with 10-day outages for the first 3 years with reload/burning costs increased by 100%

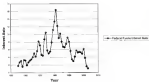


Figure 4-12. Historical Federal Funds interest rate over the last 50 years

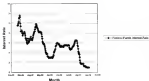


Figure 4-13. Historical Federal Funds interest rate over the last 20 years

APPENDIX A MCTAP INPUT FILES

This appendix contains all of the base-year MCTAP input files used to determine crisscross limitations for exposures and facilities used in the manufacturing, shipping, and storage of nuclear fuel.


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 1977 0.0796e+0
 1978 0.0796e+0

1979
 1980

1990	1991	1992	1993	1994	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	2010	2011	2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022	2023	2024	2025	2026	2027	2028	2029	2030	2031	2032	2033	2034	2035	2036	2037	2038	2039	2040	2041	2042	2043	2044	2045	2046	2047	2048	2049	2050	2051	2052	2053	2054	2055	2056	2057	2058	2059	2060	2061	2062	2063	2064	2065	2066	2067	2068	2069	2070	2071	2072	2073	2074	2075	2076	2077	2078	2079	2080	2081	2082	2083	2084	2085	2086	2087	2088	2089	2090	2091	2092	2093	2094	2095	2096	2097	2098	2099	2100	2101	2102	2103	2104	2105	2106	2107	2108	2109	2110	2111	2112	2113	2114	2115	2116	2117	2118	2119	2120	2121	2122	2123	2124	2125	2126	2127	2128	2129	2130	2131	2132	2133	2134	2135	2136	2137	2138	2139	2140	2141	2142	2143	2144	2145	2146	2147	2148	2149	2150	2151	2152	2153	2154	2155	2156	2157	2158	2159	2160	2161	2162	2163	2164	2165	2166	2167	2168	2169	2170	2171	2172	2173	2174	2175	2176	2177	2178	2179	2180	2181	2182	2183	2184	2185	2186	2187	2188	2189	2190	2191	2192	2193	2194	2195	2196	2197	2198	2199	2200	2201	2202	2203	2204	2205	2206	2207	2208	2209	2210	2211	2212	2213	2214	2215	2216	2217	2218	2219	2220	2221	2222	2223	2224	2225	2226	2227	2228	2229	2230	2231	2232	2233	2234	2235	2236	2237	2238	2239	2240	2241	2242	2243	2244	2245	2246	2247	2248	2249	2250	2251	2252	2253	2254	2255	2256	2257	2258	2259	2260	2261	2262	2263	2264	2265	2266	2267	2268	2269	2270	2271	2272	2273	2274	2275	2276	2277	2278	2279	2280	2281	2282	2283	2284	2285	2286	2287	2288	2289	2290	2291	2292	2293	2294	2295	2296	2297	2298	2299	2300	2301	2302	2303	2304	2305	2306	2307	2308	2309	2310	2311	2312	2313	2314	2315	2316	2317	2318	2319	2320	2321	2322	2323	2324	2325	2326	2327	2328	2329	2330	2331	2332	2333	2334	2335	2336	2337	2338	2339	2340	2341	2342	2343	2344	2345	2346	2347	2348	2349	2350	2351	2352	2353	2354	2355	2356	2357	2358	2359	2360	2361	2362	2363	2364	2365	2366	2367	2368	2369	2370	2371	2372	2373	2374	2375	2376	2377	2378	2379	2380	2381	2382	2383	2384	2385	2386	2387	2388	2389	2390	2391	2392	2393	2394	2395	2396	2397	2398	2399	2400	2401	2402	2403	2404	2405	2406	2407	2408	2409	2410	2411	2412	2413	2414	2415	2416	2417	2418	2419	2420	2421	2422	2423	2424	2425	2426	2427	2428	2429	2430	2431	2432	2433	2434	2435	2436	2437	2438	2439	2440	2441	2442	2443	2444	2445	2446	2447	2448	2449	2450	2451	2452	2453	2454	2455	2456	2457	2458	2459	2460	2461	2462	2463	2464	2465	2466	2467	2468	2469	2470	2471	2472	2473	2474	2475	2476	2477	2478	2479	2480	2481	2482	2483	2484	2485	2486	2487	2488	2489	2490	2491	2492	2493	2494	2495	2496	2497	2498	2499	2500	2501	2502	2503	2504	2505	2506	2507	2508	2509	2510	2511	2512	2513	2514	2515	2516	2517	2518	2519	2520	2521	2522	2523	2524	2525	2526	2527	2528	2529	2530	2531	2532	2533	2534	2535	2536	2537	2538	2539	2540	2541	2542	2543	2544	2545	2546	2547	2548	2549	2550	2551	2552	2553	2554	2555	2556	2557	2558	2559	2560	2561	2562	2563	2564	2565	2566	2567	2568	2569	2570	2571	2572	2573	2574	2575	2576	2577	2578	2579	2580	2581	2582	2583	2584	2585	2586	2587	2588	2589	2590	2591	2592	2593	2594	2595	2596	2597	2598	2599	2600	2601	2602	2603	2604	2605	2606	2607	2608	2609	2610	2611	2612	2613	2614	2615	2616	2617	2618	2619	2620	2621	2622	2623	2624	2625	2626	2627	2628	2629	2630	2631	2632	2633	2634	2635	2636	2637	2638	2639	2640	2641	2642	2643	2644	2645	2646	2647	2648	2649	2650	2651	2652	2653	2654	2655	2656	2657	2658	2659	2660	2661	2662	2663	2664	2665	2666	2667	2668	2669	2670	2671	2672	2673	2674	2675	2676	2677	2678	2679	2680	2681	2682	2683	2684	2685	2686	2687	2688	2689	2690	2691	2692	2693	2694	2695	2696	2697	2698	2699	2700	2701	2702	2703	2704	2705	2706	2707	2708	2709	2710	2711	2712	2713	2714	2715	2716	2717	2718	2719	2720	2721	2722	2723	2724	2725	2726	2727	2728	2729	2730	2731	2732	2733	2734	2735	2736	2737	2738	2739	2740	2741	2742	2743	2744	2745	2746	2747	2748	2749	2750	2751	2752	2753	2754	2755	2756	2757	2758	2759	2760	2761	2762	2763	2764	2765	2766	2767	2768	2769	2770	2771	2772	2773	2774	2775	2776	2777	2778	2779	2780	2781	2782	2783	2784	2785	2786	2787	2788	2789	2790	2791	2792	2793	2794	2795	2796	2797	2798	2799	2800	2801	2802	2803	2804	2805	2806	2807	2808	2809	2810	2811	2812	2813	2814	2815	2816	2817	2818	2819	2820	2821	2822	2823	2824	2825	2826	2827	2828	2829	2830	2831	2832	2833	2834	2835	2836	2837	2838	2839	2840	2841	2842	2843	2844	2845	2846	2847	2848	2849	2850	2851	2852	2853	2854	2855	2856	2857	2858	2859	2860	2861	2862	2863	2864	2865	2866	2867	2868	2869	2870	2871	2872	2873	2874	2875	2876	2877	2878	2879	2880	2881	2882	2883	2884	2885	2886	2887	2888	2889	2890	2891	2892	2893	2894	2895	2896	2897	2898	2899	2900	2901	2902	2903	2904	2905	2906	2907	2908	2909	2910	2911	2912	2913	2914	2915	2916	2917	2918	2919	2920	2921	2922	2923	2924	2925	2926	2927	2928	2929	2930	2931	2932	2933	2934	2935	2936	2937	2938	2939	2940	2941	2942	2943	2944	2945	2946	2947	2948	2949	2950	2951	2952	2953	2954	2955	2956	2957	2958	2959	2960	2961	2962	2963	2964	2965	2966	2967	2968	2969	2970	2971	2972	2973	2974	2975	2976	2977	2978	2979	2980	2981	2982	2983	2984	2985	2986	2987	2988	2989	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1993 年 12 月 20 日
 1994 年 1 月 1 日
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7  ps -f,25,250
8  ps -f,250,25 0 top of heap
9  ps -f,250,25 0 bottom of heap
10 ps -f,25,250 0 memory
11 ps -f,250,250
12 ps -f,25,250
13 ps -f,25,250
14
15 ps -f,25,250 0 some more memory
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APPENDIX B MCNP CALCULATION RESULTS

This appendix contains tables of all of the results of the MCNP runs used to determine assembly limitations for equipment and facilities used in the manufacture, shipping, and storage of nuclear fuel.

Table B-1. Results of MCNP4C2 calculations of $L(E_0)$ in a 300 cylinder completely filled with 3-R water reflector

$\ln(E_0/E_0^{\text{ref}})$	\ln_{ref}	σ
5	0.07007	0.00003
6	0.07007	0.00003
7	0.07000	0.00003
8	0.06907	0.00000
9	0.17006	0.00003
10	0.16000	0.00000
11	0.16000	0.00004
12	0.00000	0.00000
13	0.00000	0.00001
14	0.00007	0.00003
15	0.00000	0.00000
16	0.00000	0.00003
17	0.00000	0.00001
18	0.00000	0.00000
19, 20	0.00000	0.00000
21	0.00000	0.00000
22	0.00000	0.00001

Table B-2. Results of MCNP4C2 calculations of $L(E_0)$ in a 300 cylinder, filled to brim with 3-R, its moderator, lying on a concrete slab

$\ln(E_0/E_0^{\text{ref}})$	\ln_{ref}	σ
5	0.00000	0.00000
6	0.00000	0.00000
7	0.00000	0.00000
8	0.00000	0.00000
9	0.00000	0.00000
10	0.00000	0.00000
11	0.00000	0.00000
12	0.00000	0.00000
13	0.00000	0.00000
14	0.00000	0.00000
15	0.00000	0.00000
16	0.00000	0.00000
17	0.00000	0.00000
18	0.00000	0.00000
19	0.00000	0.00000
20	0.00000	0.00000

Table 6-3 Results of MCNP4C2 calculations of U_{eff} in a 300-cylinder, completely filled, no moderator, lying on a concrete slab

wt% ^{235}U	k_{eff}	σ_f
0	0.49764	0.00040
0	0.50264	0.00040
2	0.50423	0.00040
4	0.50789	0.00040
6	0.50883	0.00041
10	0.509719	0.00040
11	0.71002	0.00040
12	0.74094	0.00040
12	0.77024	0.00040
14	0.76802	0.00040
16	0.80077	0.00041
18	0.84847	0.00044
17	0.86180	0.00044
19	0.81002	0.00040
19	0.80949	0.00041
20	0.80002	0.00041

Table 6-4 Results of MCNP4C2 calculations of U_{eff} in a 300-cylinder, completely filled, moderated by water at 20 °C, lying on a concrete slab

wt% ^{235}U	k_{eff}	σ_f
0	0.67136	0.00041
0	0.67636	0.00041
2	0.68424	0.00041
4	0.69719	0.00041
6	0.70530	0.00041
10	0.70942	0.00041
11	0.76409	0.00041
12	0.77114	0.00041
13	0.78830	0.00041
14	0.80272	0.00042
16	0.80843	0.00042
18	0.82307	0.00045
17	0.82939	0.00044
19	0.80829	0.00044
19	0.80750	0.00044
20	0.80002	0.00042

Table B-1 Results of MCNP4c2 calculations of L/F_0 in a 300 cylinder, completely filled, moderated by 0.4 g/cm water vapor, lying on a concrete slab

wgt. g/cm^3	L_{eff}	L/F_0
0	0.17622	0.00043
0	0.17421	0.00043
2	0.15318	0.00043
6	0.14038	0.00043
9	0.12489	0.00043
10	0.12000	0.00043
15	0.10483	0.00043
17	0.10000	0.00043
19	0.10000	0.00043
20	0.10000	0.00043
25	0.10000	0.00043

Table B-2 Results of MCNP4c2 calculations of L/F_0 in a 300 cylinder, completely filled, moderated by 0.4 g/cm water vapor, lying on a concrete slab

wgt. g/cm^3	L_{eff}	L/F_0
0	0.16793	0.00043
0	0.17202	0.00043
2	0.16290	0.00043
6	0.15070	0.00043
9	0.13390	0.00043
10	0.13234	0.00043
11	0.12172	0.00043
12	0.11102	0.00043
13	0.10439	0.00043
14	0.10000	0.00043
15	0.10000	0.00043
16	0.10047	0.00043
17	0.10000	0.00043
18	0.10007	0.00043
19	0.10044	0.00043
20	0.10044	0.00043

Table B-7 Results of MCNP-6.2 calculations of U_{eff} in a 300 cylinder, completely filled, moderated by 0.5 g/cc water vapor, lying on a concrete slab

$w_{eff}, g/cm^3$	k_{eff}	σ^2
0	0.00002	0.00000
0	0.00021	0.00000
2	0.00005	0.00004
4	0.00040	0.00001
6	0.00106	0.00000
10	0.00070	0.00000
11	0.00063	0.00000
12	0.00060	0.00000
13	0.00060	0.00000
14	0.00059	0.00001
15	0.00058	0.00001
16	0.00058	0.00001
17	0.00058	0.00001
18	0.00057	0.00001
19	0.00049	0.00001
20	0.00050	0.00001

Table B-8 Results of MCNP-6.2 calculations of U_{eff} in a 300 cylinder, completely filled, moderated by 0.4 g/cc water vapor, lying on a concrete slab

$w_{eff}, g/cm^3$	k_{eff}	σ^2
0	0.00000	0.00000
0	0.00000	0.00001
2	0.00007	0.00007
4	0.00034	0.00001
6	0.00066	0.00000
10	0.00049	0.00004
11	0.00006	0.00000
12	0.00000	0.00000
13	0.00000	0.00000
14	0.00000	0.00000
15	0.00000	0.00000
16	0.00000	0.00000
17	0.00000	0.00000
18	0.00000	0.00000
19	0.00000	0.00000
20	0.00000	0.00000

Table B-9 Results of MCNP4c2 calculations of LE, at a 300 cylinder, completely filled, moderated by 0.3 g/cc water vapor lying on a concrete slab

$\mu_{eff}, g/cm^2$	k_{eff}	σ^2
0	0.00000	0.00000
0	0.00000	0.00000
2	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
14	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
17	0.00000	0.00000
17	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
20	0.00000	0.00000

Table B-10 Results of MCNP4c2 calculations of LE, at a 300 cylinder, completely filled, moderated by 0.2 g/cc water vapor, lying on a concrete slab

$\mu_{eff}, g/cm^2$	k_{eff}	σ^2
0	0.00000	0.00000
0	0.00000	0.00000
2	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
10	0.00000	0.00000
11	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
17	0.00000	0.00000
10	0.00000	0.00000
10	0.00000	0.00000
20	0.00000	0.00000

Table B-11: Results of MCNP4C calculations of LF₁ in a 300 cylinder, completely filled, moderated by 0.1 g/cc water vapor, lying on a square slab

width, μm	k_{eff}	σ_f
3	0.56037	0.00045
6	0.56039	0.00050
7	0.60003	0.00049
8	0.60008	0.00055
9	0.60010	0.00060
10	0.70007	0.00065
11	0.70070	0.00065
12	0.70018	0.00065
13	0.60271	0.00065
14	0.60004	0.00065
15	0.60154	0.00064
16	0.60008	0.00065
17	0.60007	0.00065
18	0.60002	0.00065
19	0.60007	0.00067
20	0.60006	0.00065

Table B-12: Results of MCNP4C calculations of LF₁ in a 300 cylinder, completely filled, moderated by 0.01 g/cc water vapor, lying on a square slab

width, μm	k_{eff}	σ_f
3	0.00133	0.00041
6	0.00095	0.00040
7	0.00175	0.00050
8	0.00145	0.00051
9	0.00154	0.00049
10	0.00121	0.00050
11	0.00171	0.00050
12	0.00166	0.00067
13	0.00037	0.00050
14	0.00071	0.00050
15	0.00040	0.00050
16	0.00038	0.00060
17	0.00104	0.00050
18	0.00000	0.00050
19	0.00000	0.00050
20	0.00000	0.00050

Table B-13 Results of MCHPAC calculations of U_T in 300 cylinders in a rectangular patch, completely filled, moderated by water at 20 °C, lying on a concrete slab

$\text{mCH}_2/\text{L}^{\text{PM}}$	λ_{PM}	U_T
5	0.88540	0.00081
6	0.75481	0.00082
7	0.71981	0.00084
8	0.68586	0.00084
9	0.65308	0.00083
10	0.62136	0.00082
11	0.59064	0.00080
12	0.56081	0.00078
13	0.53196	0.00076
14	0.50400	0.00074
15	1.47485	0.00072
16	1.42738	0.00071
17	1.38632	0.00069
18	1.35133	0.00068
19	1.32140	0.00066
20	1.29524	0.00065

Table B-14 Results of MCHPAC calculations of U_T in a 300 cylinders in a rectangular patch, completely filled, no moderation, lying on a concrete slab

$\text{mCH}_2/\text{L}^{\text{PM}}$	λ_{PM}	U_T
5	0.88538	0.00081
6	0.75479	0.00082
7	0.71979	0.00084
8	0.68583	0.00084
9	0.65305	0.00083
10	0.62133	0.00082
11	0.59061	0.00080
12	0.56078	0.00078
13	0.53193	0.00076
14	0.50400	0.00074
15	1.42771	0.00072
16	1.38420	0.00070
17	1.34051	0.00068
18	1.30409	0.00066
19	1.26794	0.00064
20	1.23490	0.00062
20	1.17792	0.00061

Table B-13 Results of MCHP4-2 calculations of U/P_2 in a 305-cylinder in a triangular pile, completely filled, surrounded by 9.1 g/cc water vapor, lying on a concrete slab

$\omega/P_2, L^{1/2}$	f_{eff}	α
6	0.70000	0.00040
8	0.70716	0.00043
10	0.71432	0.00045
12	0.72148	0.00048
14	0.72872	0.00049
16	0.73595	0.00050
18	0.74315	0.00051
20	0.75039	0.00054
22	0.75760	0.00054
24	0.76480	0.00054
26	0.77200	0.00055
28	0.77921	0.00055
30	0.78641	0.00056
32	0.79361	0.00056
34	0.80081	0.00056
36	0.80801	0.00056
38	0.81521	0.00056
40	0.82241	0.00056

Table B-14 Results of MCHP4-2 calculations of U/P_2 in a 305-cylinder in a triangular pile, completely filled, surrounded by 8.2 g/cc water vapor, lying on a concrete slab

$\omega/P_2, L^{1/2}$	f_{eff}	α
6	0.70467	0.00044
8	0.70838	0.00042
10	0.71207	0.00040
12	0.71574	0.00037
14	0.71940	0.00035
16	0.72307	0.00034
18	0.72672	0.00033
20	0.73037	0.00032
22	0.73402	0.00031
24	0.73767	0.00030
26	0.74132	0.00029
28	0.74497	0.00028
30	0.74862	0.00027
32	0.75227	0.00026
34	0.75592	0.00025
36	0.75957	0.00024
38	0.76322	0.00023
40	0.76687	0.00022

Table B-13 Results of MCNP6.2 calculations of \overline{U}_D on a 30S cylinder in a triangular pitch, completely filled, moderated by 0.3 g/cc water vapor, lying on a concrete slab.

$w\% \text{ } ^{235}\text{U}$	k_{eff}	β
5	0.77021	0.00046
6	0.78000	0.00046
7	0.80070	0.00046
8	0.81036	0.00045
9	0.82404	0.00044
10	0.84344	0.00043
11	0.85807	0.00043
12	1.00646	0.00044
13	1.01146	0.00047
14	1.01198	0.00050
15	1.01154	0.00054
16	1.10493	0.00060
17	1.13418	0.00068
18	1.14940	0.00060
19	1.16414	0.00061
20	1.18190	0.00069

Table B-14 Results of MCNP6.2 calculations of \overline{U}_D on a 30S cylinder in a triangular pitch, completely filled, moderated by 0.3 g/cc water vapor, lying on a concrete slab.

$w\% \text{ } ^{235}\text{U}$	k_{eff}	β
5	0.76187	0.00050
6	0.77087	0.00050
7	0.81780	0.00054
8	0.82887	0.00050
9	0.84071	0.00058
10	0.85836	0.00061
11	0.88118	0.00068
12	0.91600	0.00068
13	1.04207	0.00068
14	1.05866	0.00060
15	1.06140	0.00066
16	1.06088	0.00066
17	1.10426	0.00068
18	1.12506	0.00067
19	1.14850	0.00066
20	1.16422	0.00068

Table B-19. Results of MCHPAC calculations of U^* for a 300 cylinder in a triangular patch completely filled, extended by 3.8 g/hr water vapor, being at a constant rate.

width, $g^{1/2}$	t_{90}	U^*
6	0.00071	0.00040
8	0.00094	0.00052
7	0.00080	0.00050
8	0.00113	0.00057
9	0.00143	0.00063
10	0.00169	0.00068
11	0.00198	0.00073
12	0.00227	0.00077
13	0.00257	0.00081
14	1.00000	0.00085
15	1.00000	0.00089
16	1.00121	0.00093
17	1.00250	0.00097
18	1.00376	0.00101
19	1.00506	0.00105
20	1.00631	0.00109

Table B-20. Results of MCHPAC calculations for 3-width, U^{*20} water/CH₂ dury in a 6-inch 405T 20 pipe.

U^{*20} g/hr	t_{90}	U^*
1.054	0.00040	0.00047
1.050	0.00050	0.00048
1.050	0.00070	0.00049
1.050	0.00080	0.00050
1.400	0.00090	0.00050
1.380	0.00100	0.00050
1.300	0.00130	0.00050
1.074	0.00150	0.00050
0.980	0.0017	0.00050
0.900	0.00170	0.00050
0.781	0.00180	0.00050
0.601	0.00191	0.00050

Table B-21 Results of MCHP4-2 calculations for 3-wt% U^{235} water/ CO_2 slurry at a 18-inch 402T 5A pipe

U-density g/cc	k_{eff}	β'
3.034	0.00468	0.00041
1.820	0.00094	0.00001
1.748	0.00044	0.00000
1.585	0.00007	0.00049
1.489	0.00000	0.00000
1.290	0.00004	0.00047
1.205	0.00047	0.00031
1.054	0.00007	0.00047
0.990	0.00014	0.00044
0.808	0.00006	0.00040
0.707	0.00006	0.00040
0.507	0.00000	0.00040

Table B-22 Results of MCHP4-2 calculations for 3-wt% U^{235} water/ CO_2 slurry at a 18-inch 402T 5A pipe

U-density g/cc	k_{eff}	β'
3.058	0.00000	0.00040
1.840	0.00000	0.00000
1.700	0.00000	0.00000
1.600	0.00004	0.00000
1.400	0.00007	0.00000
1.380	0.00000	0.00047
1.300	0.00000	0.00040
1.054	0.00007	0.00047
0.900	0.00000	0.00044
0.800	0.00000	0.00040
0.704	0.00004	0.00044
0.500	0.00000	0.00040

Table B-23 Results of MCNP4c2 calculations for 3-wt% U^{235} water/CO₂ slurry in a 6-inch AOST SS pipe

Slowness g/cm ³	k_{eff}	σ^2
2.054	0.73761	0.00030
1.999	0.73639	0.00030
1.950	0.73417	0.00030
1.900	0.73291	0.00030
1.850	0.73274	0.00030
1.800	0.73094	0.00030
1.750	0.73100	0.00030
1.694	0.80013	0.00040
0.600	0.87763	0.00040
0.400	0.89020	0.00040
0.301	0.83707	0.00040
0.101	0.90400	0.00040

Table B-24 Results of MCNP4c2 calculations for 3-wt% U^{235} water/CO₂ slurry in an 8-inch AOST SS pipe

Slowness g/cm ³	k_{eff}	σ^2
2.054	0.88713	0.00060
1.999	0.88680	0.00060
1.950	0.88664	0.00060
1.900	0.88734	0.00060
1.850	0.87673	0.00060
1.800	0.87630	0.00060
1.750	0.87630	0.00060
1.700	0.88681	0.00060
1.644	0.88700	0.00060
0.600	0.89400	0.00060
0.400	0.87800	0.00060
0.301	0.79407	0.00060
0.101	0.79420	0.00060

Table B-25 Results of MCNP4C calculations for 7-wt% U^{235} water/DO slurry in a 4-inch 408T 80 pipe

U -density g/cc	k_{eff}	σ_f
2.004	1.00743	0.00004
1.999	1.01033	0.00000
1.993	1.00800	0.00004
1.988	1.00743	0.00000
1.980	1.00604	0.00003
1.969	0.99833	0.00000
1.960	0.99379	0.00000
1.954	0.97879	0.00000
0.999	0.99999	0.00000
0.999	0.99979	0.00000
0.999	0.99999	0.00000
0.999	0.99999	0.00000
0.999	0.99999	0.00000

Table B-26 Results of MCNP4C calculations for 18-wt% U^{235} water/DO slurry in a 4-inch 408T 80 pipe

U -density g/cc	k_{eff}	σ_f
2.004	0.76300	0.00000
1.999	0.76900	0.00004
1.993	0.76900	0.00000
1.988	0.76900	0.00000
1.980	0.76941	0.00000
1.969	0.76821	0.00000
1.960	0.76900	0.00000
1.954	0.76801	0.00000
0.999	0.74700	0.00000
0.999	0.70400	0.00000
0.999	0.71874	0.00000
0.999	0.99999	0.00000

Table B-37 Results of HAZOP-H2 calculations for 10-wt% U^{235} water/ H_2O_2 slurry in an 8-inch 405T SS pipe

U-density (g/cc)	η_{sp}	η'
3.054	0.0086	0.00054
1.880	0.00878	0.00054
1.700	0.0088	0.00057
1.600	0.00728	0.00054
1.400	0.00676	0.00054
1.360	0.00744	0.00054
1.300	0.00079	0.00054
1.014	0.00058	0.00054
0.999	0.01100	0.00054
0.908	0.00100	0.00054
0.761	0.00079	0.00054
0.601	0.00014	0.00054

Table B-38 Results of HAZOP-H2 calculations for 15-wt% U^{235} water/ H_2O_2 slurry in a 8-inch 405T SS pipe

U-density (g/cc)	η_{sp}	η'
3.054	0.0008	0.00054
1.880	0.00018	0.00054
1.700	0.00051	0.00054
1.600	0.00054	0.00054
1.400	0.00028	0.00054
1.360	0.00007	0.00054
1.300	0.00008	0.00054
1.014	0.00080	0.00054
0.999	0.01028	0.00054
0.908	0.00080	0.00054
0.761	0.00079	0.00054
0.601	0.00014	0.00054

Table B-29. Results of MCHW42 calculations for 35-wt% $\text{Li}^{200}\text{water}/\text{Li}_2\text{O}_2$ slurry in a 6-inch 405T SS pipe.

Li density g/cc	k_{eff}	β^*
1.034	0.16201	0.00066
1.040	0.16193	0.00066
1.100	0.16273	0.00066
1.300	0.16420	0.00064
1.400	0.16476	0.00064
1.500	0.16538	0.00064
1.600	0.16600	0.00061
1.814	0.16800	0.00061
2.000	0.16970	0.00060
2.400	0.17290	0.00060
2.701	0.18006	0.00063
2.801	0.18313	0.00063

Table B-30. Results of MCHW42 calculations for 35-wt% $\text{Li}^{200}\text{water}/\text{Li}_2\text{O}_2$ slurry in a 6-inch 405T SS pipe.

Li density g/cc	k_{eff}	β^*
1.034	0.16170	0.00066
1.040	0.16166	0.00066
1.100	0.16236	0.00064
1.300	0.16440	0.00064
1.400	0.16478	0.00064
1.500	0.16516	0.00064
1.600	0.16554	0.00061
1.814	0.16760	0.00060
2.000	0.16960	0.00060
2.400	0.17300	0.00060
2.701	0.18070	0.00063
2.801	0.18240	0.00063

Table B-31. Results of MCNP4c2 calculations for 28-wt% U^{235} water/CO₂ slurry in at # web 4052 58 page

Uniformity g/g	k_{eff}	σ
0.004	1.00450	0.00000
0.005	1.00000	0.00000
0.006	1.00000	0.00000
0.008	1.00000	0.00000
0.010	1.00000	0.00000
0.015	1.00000	0.00000
0.020	1.00000	0.00000
0.030	1.00000	0.00000
0.040	1.00000	0.00000
0.050	1.00000	0.00000
0.060	1.00000	0.00000
0.070	1.00000	0.00000
0.080	1.00000	0.00000
0.090	1.00000	0.00000
0.100	1.00000	0.00000

Table B-32. Results of MCNP4c2 calculations for dry compression reactor with no moderator

wt% U^{235}	k_{eff}	σ
0	0.00000	0.00000
1	0.00000	0.00000
2	0.00000	0.00000
3	0.00000	0.00000
4	0.00000	0.00000
5	0.00000	0.00000
6	0.00000	0.00000
7	0.00000	0.00000
8	0.00000	0.00000
9	0.00000	0.00000
10	0.00000	0.00000
11	0.00000	0.00000
12	0.00000	0.00000
13	0.00000	0.00000
14	0.00000	0.00000
15	0.00000	0.00000
16	0.00000	0.00000
17	0.00000	0.00000
18	0.00000	0.00000
19	0.00000	0.00000
20	0.00000	0.00000

Table B-13: Results of MCM4C2-calculations for dry conversion reactor moderated by water at 30 °C

$w(\text{H}_2\text{O})^{20}$	β_{tot}	β
5	0.00038	0.00079
6	0.00039	0.00086
7	0.00040	0.00090
8	0.00040	0.00091
9	0.00040	0.00091
10	0.00040	0.00090
11	0.00039	0.00089
12	0.00038	0.00088
13	0.00037	0.00086
14	0.00036	0.00084
15	0.00035	0.00082
16	0.00034	0.00080
17	0.00033	0.00078
18	0.00032	0.00076
19	0.00031	0.00074
20	0.00030	0.00073

Table B-14: Results of MCM4C2-calculations for dry conversion reactor moderated by 2.5 g/l water vapor

$w(\text{H}_2\text{O})^{20}$	β_{tot}	β
5	0.00043	0.00074
6	0.00043	0.00075
7	0.00043	0.00076
8	0.00043	0.00076
9	0.00043	0.00076
10	0.00043	0.00076
11	0.00043	0.00076
12	0.00043	0.00076
13	0.00043	0.00076
14	0.00043	0.00076
15	0.00043	0.00076
16	0.00043	0.00076
17	0.00043	0.00076
18	0.00043	0.00076
19	0.00043	0.00076
20	0.00043	0.00076

Table B-35. Results of MCPKC calculations for dry conversion master modulated by 0.2 g/sa water vapor.

$\text{wt}\%_{\text{H}_2\text{O}}^{\text{ref}}$	β_{ref}	β
5	0.00011	0.00010
6	0.00020	0.00019
7	0.00032	0.00030
8	0.00046	0.00043
9	0.00062	0.00059
10	0.00079	0.00076
11	0.00108	0.00107
12	0.00139	0.00140
13	0.00180	0.00184
14	1.00001	0.00241
15	1.00040	0.00300
16	1.00111	0.00364
17	1.00244	0.00444
18	1.00737	0.00563
19	1.04777	0.00800
20	1.04831	0.00803

Table B-36. Results of MCPKC calculations for an infinite array of 43 gallon drums containing LiCl powder modulated by water at 30 °C.

$\text{wt}\%_{\text{H}_2\text{O}}^{\text{ref}}$	β_{ref}	β
5	0.00004	0.00003
6	0.00004	0.00003
7	0.00004	0.00004
8	0.00000	0.00000
9	0.00000	0.00003
10	0.00000	0.00003
11	0.00000	0.00011
12	0.00000	0.00006
13	0.00000	0.00009
14	0.00000	0.00017
15	0.00001	0.00004
16	0.00001	0.00003
17	0.00000	0.00003
18	0.00000	0.00003
19	0.00000	0.00003
20	1.00013	0.00000

Table B-27 Results of MCNP4C2 calculations for an infinite array of 40-gallon drums containing UO_2 powder moderated by 0.1 g/cc water vapor

$\mu_{\text{eff}}, \text{g}^{-1}\text{cm}^2$	k_{eff}	β
5	0.14623	0.00000
6	0.14028	0.00000
7	0.13140	0.00000
8	0.12058	0.00000
9	0.10788	0.00000
10	0.10000	0.00000
11	0.09479	0.00000
12	0.09059	0.00000
13	0.08697	0.00000
14	0.08389	0.00000
15	0.08117	0.00000
16	0.07880	0.00000
17	0.07668	0.00000
18	0.07480	0.00000
19	0.07316	0.00000
20	0.07170	0.00000

Table B-28 Results of MCNP4C2 calculations for an infinite array of 40-gallon drums containing UO_2 powder moderated by 0.2 g/cc water vapor

$\mu_{\text{eff}}, \text{g}^{-1}\text{cm}^2$	k_{eff}	β
5	0.17008	0.00000
6	0.17060	0.00000
7	0.16077	0.00000
8	0.14788	0.00000
9	0.13086	0.00000
10	0.10880	0.00000
11	0.09048	0.00000
12	0.06668	0.00000
13	0.04777	0.00000
14	0.03178	0.00000
15	0.02000	0.00000
16	0.01080	0.00000
17	0.00600	0.00000
18	0.00300	0.00000
19	0.00150	0.00000
20	0.00075	0.00000

Table B-39. Results of MCNP4C2 calculations for an infinite array of 43-pulse drums containing ^{235}U powder moderated by 0.3 g/cc water vapor

$\mu_{\text{eff}}, \text{g}^{-1}\text{cm}^2$	k_{eff}	σ^2
6	0.75404	0.00071
8	0.80887	0.00046
7	0.80837	0.00073
9	0.85488	0.0007
9	0.88802	0.00086
10	0.90767	0.00077
10	0.88862	0.00072
12	0.90716	0.00066
10	0.91959	0.00073
10	0.90714	0.00073
10	1.00070	0.00071
10	1.00058	0.00073
11	1.0068	0.00074
10	1.00656	0.00076
10	1.0068	0.00067
20	1.00059	0.00074

Table B-40. Results of MCNP4C2 calculations for an infinite array of 43-pulse drums containing ^{235}U powder moderated by 0.4 g/cc water vapor

$\mu_{\text{eff}}, \text{g}^{-1}\text{cm}^2$	k_{eff}	σ^2
6	0.75046	0.00071
8	0.81334	0.00068
7	0.81356	0.00073
9	0.87663	0.00070
9	0.90007	0.00071
10	0.90088	0.00076
11	0.90862	0.00072
12	0.90733	0.00071
10	0.91678	0.00072
10	0.91658	0.00071
10	1.00063	0.00077
10	1.00067	0.00076
11	1.00070	0.00071
10	1.00070	0.00076
10	1.00070	0.00073
20	1.00066	0.00071

Table E-41 Results of MCHP4C2 calculations for an infinite array of 45-pulse beams containing LiCl^{a} powder irradiated by 0.5 g/sec water vapor

wt% LiCl^{a}	β_{eq}	β^*
5	0.17095	0.00071
6	0.08048	0.00073
7	0.04481	0.00074
8	0.03094	0.00076
9	0.02087	0.0007
10	0.01094	0.00079
11	0.00883	0.00071
12	0.00617	0.00079
13	0.00409	0.00087
14	0.00344	0.00088
15	0.00264	0.00074
16	1.00173	0.00079
17	1.001	0.00079
18	1.00071	0.00079
19	1.00037	0.00079
20	1.0003	0.0007

Table E-42 Results of MCHP4C2 calculations for an infinite array of 45-pulse beams containing LiCl^{a} powder irradiated by 1.5 g/sec water vapor

wt% LiCl^{a}	β_{eq}	β^*
5	0.17037	0.00071
6	0.10038	0.00076
7	0.07031	0.00088
8	0.03878	0.00073
9	0.03087	0.00088
10	0.01947	0.00071
11	0.00817	0.00071
12	0.01073	0.00079
13	0.00743	0.00085
14	0.00482	0.00085
15	0.00342	0.00076
16	0.00261	0.00071
17	0.10001	0.00085
18	0.00784	0.00082
19	1.00045	0.00081
20	1.00038	0.00071

Table B-43 Results of MCNP4C2 calculations for infinite array of polyethylene pellet beds containing a 2 to 1 ratio by volume of water to UO_2 moderated by 0.65 g/cm³ water vapor

$\mu_{\text{eff}}/\mu_{\text{tr}}^{\text{H}_2\text{O}}$	k_{eff}	β
5	0.76636	0.00080
6	0.66183	0.00078
7	0.70067	0.00076
8	0.77408	0.00075
9	0.73878	0.00064
10	0.70712	0.00064
11	0.74820	0.00063
12	0.78376	0.00060
13	0.78426	0.00064
14	0.78427	0.00065
15	0.77636	0.00063
16	0.75476	0.00060
17	0.75436	0.00063
18	0.75369	0.00074
19	0.75317	0.00063
20	0.80041	0.00063

Table B-44 Results of MCNP4C2 calculations for infinite array of polyethylene pellet beds containing a 2 to 1 ratio by volume of water to UO_2 moderated by 0.1 g/cm³ water vapor

$\mu_{\text{eff}}/\mu_{\text{tr}}^{\text{H}_2\text{O}}$	k_{eff}	β
5	0.50748	0.00078
6	0.40484	0.00073
7	0.47384	0.00078
8	0.49460	0.00077
9	0.49307	0.00074
10	0.49487	0.00078
11	0.50810	0.00076
12	0.54328	0.00076
13	0.54376	0.00074
14	0.54366	0.00076
15	0.53960	0.00077
16	0.54437	0.00077
17	0.54449	0.00076
18	0.54421	0.00083
19	1.00029	0.00077
20	1.00034	0.00079

Table B-47 Results of MCNP4C calculations for infinite array of singly-boreman perforated tubes containing a 2 to 1 ratio by volume of steam to LCP moderated by 8.3 g/cc water vapor

$\mu_{eff}, \text{g/cm}^2$	k_{eff}	σ_f
0	0.70080	0.00087
1	0.70086	0.00087
2	0.70074	0.00085
3	0.70076	0.00086
4	0.70087	0.00086
10	0.70086	0.00086
15	0.70088	0.00086
20	0.70088	0.00086
25	0.70073	0.00086
30	0.70068	0.00076
35	0.70066	0.00086
40	0.70102	0.00086
45	0.70080	0.00086
50	0.70078	0.00086
55	0.70078	0.00086
60	0.70078	0.00086
65	0.70078	0.00086
70	0.70078	0.00086

Table B-48 Results of MCNP3-csp calculations for single 15x15 assembly moderated by water at 20 °C

$\mu_{eff}, \text{g/cm}^2$	k_{eff}	σ_f
0	1.04409	0.00000
1	1.03775	0.00000
2	1.03230	0.00000
3	1.02640	0.00000
4	1.02040	0.00000
5	1.01440	0.00000
10	1.00800	0.00000
11	1.00700	0.00000
12	1.00640	0.00000
13	1.00580	0.00000
14	1.00520	0.00000
15	1.00460	0.00000
16	1.00400	0.00000
17	1.00340	0.00000
18	1.00280	0.00000
19	1.00220	0.00000
20	1.00160	0.00000
25	1.00000	0.00000

Table B-49. Results of MCNP5-eps calculations for single 15x15 assembly with steel rod wires moderated by water at 28 °C

$wth, \lambda^{(eps)}$	k_{eff}	β
0	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
10	0.00000	0.00000
11	0.00000	0.00000
12	0.00000	0.00000
13	0.00000	0.00000
14	0.00000	0.00000
15	0.00000	0.00000
16	0.00000	0.00000
17	0.00000	0.00000
18	0.00000	0.00000
19	0.00000	0.00000
20	0.00000	0.00000

Table B-50. Results of MCNP5-eps calculations for single 15x15 assembly with a BFAA moderated by water at 28 °C

$wth, \lambda^{(eps)}$	k_{eff}	β
0	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
0	0.00000	0.00000
10	0.00000	0.00000
11	0.00000	0.00000
12	0.00000	0.00000
13	0.00000	0.00000
14	0.00000	0.00000
15	0.00000	0.00000
16	0.00000	0.00000
17	0.00000	0.00000
18	0.00000	0.00000
19	0.00000	0.00000
20	0.00000	0.00000

Table B-31 Results of MCHPS rps calculations for infinite array of shipping containers containing two 12x15 assemblies moderated by water at 20 °C

$w\% \text{ } ^{235}\text{U}$	k_{eff}	β
1	0.92146	0.00007
2	0.94036	0.00011
3	0.95914	0.00019
4	0.97794	0.00031
5	0.99678	0.00047
10	1.00094	0.00069
11	1.00102	0.00069
12	1.00163	0.00064
13	1.00209	0.00058
14	1.00246	0.00051
15	1.00276	0.00046
16	1.00303	0.00041
17	1.00324	0.00037
18	1.00341	0.00033
19	1.00356	0.00030
20	1.00371	0.00027

Table B-32 Results of MCHPS rps calculations for infinite array of shipping containers containing two 12x15 assemblies moderated by 0.9 g/cc water vapor

$w\% \text{ } ^{235}\text{U}$	k_{eff}	β
6	0.98388	0.00007
8	0.99036	0.00011
9	0.99316	0.00016
10	0.99594	0.00024
11	0.99807	0.00038
12	0.99948	0.00052
13	0.99988	0.00067
14	0.99996	0.00073
15	1.00000	0.00073
16	1.00004	0.00069
17	1.00006	0.00064
18	1.00005	0.00058
19	1.00003	0.00051
20	1.00001	0.00046

Table B-33. Results of MCNP3-cpi calculations for infinite array of shipping containers containing one ^{235}U assembly moderated by 0.5 g/cc water vapor

$\mu_{\text{eff}}, \text{g}^{-1}\text{cm}^2$	k_{eff}	σ^2
6	0.97612	0.00002
8	0.98017	0.00003
7	0.97604	0.00004
8	0.97636	0.00002
8	0.98002	0.00007
10	0.97601	0.00004
10	0.98038	0.00003
10	0.97678	0.00003
10	0.98007	0.00003
14	0.97606	0.00004
14	0.98008	0.00003
16	0.98000	0.00003
17	0.97603	0.00004
18	0.98037	0.00001
19	0.98070	0.00001
20	0.98072	0.00001

Table B-34. Results of MCNP3-cpi calculations for infinite array of shipping containers containing one ^{235}U assembly moderated by 0.5 g/cc water vapor

$\mu_{\text{eff}}, \text{g}^{-1}\text{cm}^2$	k_{eff}	σ^2
4	0.94633	0.00000
4	0.94660	0.00000
7	0.94606	0.00001
8	0.94613	0.00000
8	0.94674	0.00000
10	0.94666	0.00000
10	0.94606	0.00000
10	0.94638	0.00000
10	0.94617	0.00000
14	0.94660	0.00000
14	0.94677	0.00000
16	0.94681	0.00000
17	0.94660	0.00000
18	0.94627	0.00000
19	0.94670	0.00000
20	0.94678	0.00000

Table B-37. Results of MCNP5-eps calculations for infinite array of shipping containers containing two 15d3 assemblies with no moderator

eps, g^{-1}cm^2	k_{eff}	σ^2
5	0.17534	0.00011
6	0.10007	0.00010
7	0.10400	0.00011
8	0.10870	0.00011
9	0.10400	0.00010
10	0.10006	0.00010
15	0.14014	0.00010
16	0.14004	0.00010
19	0.15000	0.00010
14	0.10007	0.00010
18	0.10007	0.00010
19	0.10194	0.00010
17	0.11000	0.00010
16	0.10000	0.00010
19	0.10017	0.00010
20	0.10000	0.00010

Table B-38. Results of MCNP5-eps calculations for infinite array of shipping containers containing two 15d3 assemblies with steel inserts moderated by water at 20 °C

eps, g^{-1}cm^2	k_{eff}	σ^2
5	0.87002	0.00000
6	0.80000	0.00000
7	0.80070	0.00000
8	0.80000	0.00070
9	0.80000	0.00000
10	0.80000	0.00000
11	0.80000	0.00000
12	0.80000	0.00000
13	1.00000	0.00000
14	1.00000	0.00000
15	1.00000	0.00000
16	1.00000	0.00000
17	1.00000	0.00000
18	1.00000	0.00000
19	1.00000	0.00000
20	1.00000	0.00000

Table B-59. Results of MCNP5 nps calculations for infinite array of shipping containers containing two 15x15 assemblies with BWRAs moderated by water at 20 °C.

$\text{effs, } \mu^{\text{eff}}$	k_{eff}	σ
6	0.79366	0.00001
8	0.80017	0.00001
7	0.80000	0.00001
9	0.80000	0.00001
6	0.79990	0.00001
10	0.80000	0.00001
11	0.80000	0.00001
12	0.80001	0.00001
13	0.80000	0.00001
14	0.80000	0.00001
15	0.80000	0.00001
16	0.80000	0.00001
17	0.80001	0.00001
18	0.80000	0.00001
19	0.80000	0.00001
20	0.80000	0.00001

Table B-60. Results of MCNP5 nps calculations a spent fuel pool containing no boron.

$\text{effs, } \mu^{\text{eff}}$	k_{eff}	σ
6	0.94000	0.00004
8	0.94000	0.00007
7	0.94001	0.00000
9	1.00000	0.00000
6	1.00000	0.00000
10	1.00000	0.00001
11	1.00000	0.00000
12	1.00000	0.00000
13	1.00000	0.00000
14	1.00000	0.00000
15	1.00000	0.00000
16	1.00000	0.00000
17	1.00000	0.00000
18	1.00000	0.00000
19	1.00000	0.00000
20	1.00000	0.00000

Table B-61 Results of MCNP3 exp calculations: spent fuel pool containing 500-ppm boron.

$\mu_{\text{eff}} \text{ M}^{-1}$	k_{eff}	σ^2
5	0.95075	0.00066
6	0.94930	0.00060
7	0.94962	0.00050
8	0.94938	0.00047
9	0.94990	0.00031
10	0.94927	0.00061
11	0.94911	0.00034
12	0.94985	0.00030
13	0.95011	0.00030
14	0.94990	0.00031
15	1.00028	0.00030
16	1.00761	0.00031
17	1.01236	0.00037
18	1.01664	0.00034
19	1.02443	0.00038
20	1.03107	0.00033

Table B-62 Results of MCNP3 exp calculations: spent fuel pool using BPLA's and containing no boron.

$\mu_{\text{eff}} \text{ M}^{-1}$	k_{eff}	σ^2
5	0.92866	0.00065
6	0.92858	0.00066
7	0.92956	0.00064
8	0.92960	0.00066
9	0.92890	0.00033
10	0.92823	0.00034
11	0.92848	0.00060
12	0.92750	0.00030
13	0.92840	0.00030
14	0.92823	0.00030
15	0.92821	0.00030
16	0.92765	0.00034
17	0.92761	0.00066
18	0.92820	0.00033
19	0.92823	0.00034
20	0.92881	0.00033

Table B-63 Results of MCNP-mp calculations: a spent fuel pool using DPLA's and containing 500 ppm boron.

MCNP^{ref}	k_{eff}	β
5	0.73833	0.00070
6	0.77128	0.00067
7	0.78763	0.00064
8	0.81808	0.00060
9	0.83475	0.00058
10	0.85094	0.00053
11	0.86546	0.00049
12	0.87879	0.00046
13	0.89010	0.00043
14	0.90138	0.00041
15	0.91267	0.00040
16	0.92396	0.00037
17	0.93527	0.00034
18	0.94649	0.00030
19	0.95761	0.00027
20	0.96873	0.00025

APPENDIX C CASHMIR INPUT FILES

This appendix contains the four case CASHMIR-1 input files used to determine discharge currents and cycle lengths for vehicles from 3-whe U^{250} to 10-whe U^{250} .

APPENDIX D CASMO-5 AND CASPER-5 CALCULATION RESULTS

This appendix contains the results from CASMO-5 and CASPER-5 calculations for discharge burnups and cycle lengths for treatments from 5-wdts 10^{22} to 10-wdts 10^{22} .

Table D-1. Results of CASH00.1 and CASH00-4 calculations of the number of bands for 12-day escape plots

Development Length, cm	12-month		24-month		36-month		48-month		60-month	
	Bands in Core	Bands in Core	Bands in Core	Bands in Core	Bands in Core	Bands in Core	Bands in Core	Bands in Core	Bands in Core	Bands in Core
4.8	4.11	2.52	1.73	1.15	0.79	0.54	0.38	0.26	0.18	0.13
5.8	5.25	3.28	2.22	1.44	0.94	0.64	0.44	0.30	0.20	0.15
6.8	6.44	4.03	2.68	1.76	1.14	0.76	0.52	0.35	0.23	0.17
8.0	8.00	5.00	3.33	2.22	1.48	1.00	0.67	0.44	0.29	0.22
9.0	9.78	6.02	4.02	2.68	1.76	1.15	0.76	0.51	0.33	0.25
10.0	11.78	7.19	4.76	3.20	2.14	1.40	0.94	0.62	0.40	0.30
11.0	14.03	8.50	5.50	3.67	2.40	1.60	1.07	0.70	0.46	0.34
12.0	16.56	9.90	6.30	4.10	2.69	1.80	1.19	0.78	0.51	0.38
13.0	19.38	11.40	7.20	4.60	3.00	2.00	1.33	0.88	0.57	0.43
14.0	22.50	13.00	8.10	5.10	3.33	2.22	1.50	1.00	0.66	0.50
15.0	25.94	14.70	9.10	5.70	3.70	2.40	1.67	1.11	0.74	0.56
16.0	29.71	16.60	10.30	6.40	4.10	2.69	1.88	1.25	0.83	0.63
17.0	33.83	18.60	11.70	7.20	4.60	3.00	2.14	1.40	0.94	0.70
18.0	38.31	20.80	13.20	8.10	5.10	3.33	2.40	1.60	1.07	0.78
19.0	43.16	23.20	14.80	9.10	5.70	3.70	2.69	1.80	1.19	0.88
20.0	48.39	25.80	16.50	10.30	6.30	4.10	3.00	2.00	1.33	0.99
21.0	54.01	28.60	18.30	11.70	7.20	4.60	3.33	2.22	1.50	1.11
22.0	60.04	31.60	20.30	13.20	8.10	5.10	3.70	2.40	1.67	1.25
23.0	66.50	34.90	22.40	14.80	9.10	5.70	4.10	2.69	1.88	1.40
24.0	73.40	38.40	24.60	16.50	10.30	6.30	4.60	3.00	2.14	1.56
25.0	80.76	42.10	26.90	18.30	11.70	7.20	5.10	3.33	2.40	1.73
26.0	88.60	46.00	29.30	20.30	13.20	8.10	5.70	3.70	2.69	1.91
27.0	96.94	50.10	31.80	22.40	14.80	9.10	6.30	4.10	3.00	2.11
28.0	105.79	54.40	34.40	24.60	16.50	10.30	7.00	4.60	3.33	2.32
29.0	115.16	58.90	37.10	26.90	18.30	11.70	7.70	5.10	3.70	2.54
30.0	125.07	63.60	39.90	29.30	20.30	13.20	8.50	5.70	4.10	2.77
31.0	135.54	68.50	42.80	31.80	22.40	14.80	9.40	6.30	4.60	3.02
32.0	146.60	73.60	45.80	34.40	24.60	16.50	10.40	7.00	5.10	3.28
33.0	158.27	78.90	48.90	37.10	26.90	18.30	11.50	7.70	5.70	3.56
34.0	170.58	84.40	51.90	39.90	29.30	20.30	12.70	8.50	6.30	3.85
35.0	183.55	90.10	55.00	42.80	31.80	22.40	14.00	9.40	7.00	4.16
36.0	197.21	96.00	58.10	45.80	34.40	24.60	15.40	10.40	7.70	4.48
37.0	211.58	102.10	61.30	48.90	37.10	26.90	16.90	11.50	8.50	4.82
38.0	226.69	108.40	64.60	51.90	39.90	29.30	18.50	12.70	9.40	5.18
39.0	242.57	114.90	68.00	55.00	42.80	31.80	20.20	14.00	10.40	5.56
40.0	259.25	121.60	71.50	58.10	45.80	34.40	22.10	15.40	11.50	5.96
41.0	276.76	128.50	75.10	61.30	48.90	37.10	24.10	16.90	12.70	6.38
42.0	295.04	135.60	78.80	64.60	51.90	39.90	26.30	18.50	14.00	6.82
43.0	314.12	142.90	82.60	68.00	55.00	42.80	28.70	20.20	15.40	7.28
44.0	334.04	150.40	86.50	71.50	58.10	45.80	31.30	22.10	16.90	7.76
45.0	354.84	158.10	90.50	75.10	61.30	48.90	34.10	24.10	18.50	8.26
46.0	376.56	166.00	94.60	78.80	64.60	51.90	37.10	26.30	20.20	8.78
47.0	399.24	174.10	98.80	82.60	68.00	55.00	40.30	28.70	22.10	9.32
48.0	422.91	182.40	103.10	86.50	71.50	58.10	43.70	31.30	24.10	9.88
49.0	447.61	190.90	107.50	90.50	75.10	61.30	47.30	34.10	26.30	10.46
50.0	473.37	199.60	112.00	94.60	78.80	64.60	51.10	37.10	28.70	11.06

Table D-2 Results of CC-BBDD-3 and CC-BBDD-4 evaluation of the number of basins for 30-day storage plants

Evaluation with 30- day	10 basins/30 months		20 basins/30 months		30 basins/30 months		40 basins/30 months	
	Basins in Days	Basins in Days	Basins in Days	Basins in Days	Basins in Days	Basins in Days	Basins in Days	Basins in Days
4.0	4.00	2.50	1.50	1.00	0.50	0.00	0.00	0.00
5.0	5.00	3.24	2.00	1.43	0.75	0.00	0.00	0.00
6.0	6.00	3.88	2.50	1.75	1.00	0.00	0.00	0.00
7.0	7.00	4.50	3.00	2.00	1.25	0.00	0.00	0.00
8.0	8.00	5.00	3.50	2.25	1.50	0.00	0.00	0.00
9.0	9.00	5.45	4.00	2.50	1.75	0.00	0.00	0.00
10.0	10.00	5.85	4.50	2.75	2.00	0.00	0.00	0.00
11.0	11.00	6.20	5.00	3.00	2.25	0.00	0.00	0.00
12.0	12.00	6.50	5.50	3.25	2.50	0.00	0.00	0.00
13.0	13.00	6.75	6.00	3.50	2.75	0.00	0.00	0.00
14.0	14.00	7.00	6.50	3.75	3.00	0.00	0.00	0.00
15.0	15.00	7.20	7.00	4.00	3.25	0.00	0.00	0.00
16.0	16.00	7.36	7.50	4.25	3.50	0.00	0.00	0.00
17.0	17.00	7.50	8.00	4.50	3.75	0.00	0.00	0.00
18.0	18.00	7.62	8.50	4.75	4.00	0.00	0.00	0.00
19.0	19.00	7.72	9.00	5.00	4.25	0.00	0.00	0.00
20.0	20.00	7.80	9.50	5.25	4.50	0.00	0.00	0.00
21.0	21.00	7.87	10.00	5.50	4.75	0.00	0.00	0.00
22.0	22.00	7.93	10.50	5.75	5.00	0.00	0.00	0.00
23.0	23.00	7.98	11.00	6.00	5.25	0.00	0.00	0.00
24.0	24.00	8.02	11.50	6.25	5.50	0.00	0.00	0.00
25.0	25.00	8.06	12.00	6.50	5.75	0.00	0.00	0.00
26.0	26.00	8.09	12.50	6.75	6.00	0.00	0.00	0.00
27.0	27.00	8.12	13.00	7.00	6.25	0.00	0.00	0.00
28.0	28.00	8.15	13.50	7.25	6.50	0.00	0.00	0.00
29.0	29.00	8.17	14.00	7.50	6.75	0.00	0.00	0.00
30.0	30.00	8.20	14.50	7.75	7.00	0.00	0.00	0.00
31.0	31.00	8.22	15.00	8.00	7.25	0.00	0.00	0.00
32.0	32.00	8.24	15.50	8.25	7.50	0.00	0.00	0.00
33.0	33.00	8.26	16.00	8.50	7.75	0.00	0.00	0.00
34.0	34.00	8.28	16.50	8.75	8.00	0.00	0.00	0.00
35.0	35.00	8.30	17.00	9.00	8.25	0.00	0.00	0.00
36.0	36.00	8.32	17.50	9.25	8.50	0.00	0.00	0.00
37.0	37.00	8.34	18.00	9.50	8.75	0.00	0.00	0.00
38.0	38.00	8.36	18.50	9.75	9.00	0.00	0.00	0.00
39.0	39.00	8.38	19.00	10.00	9.25	0.00	0.00	0.00
40.0	40.00	8.40	19.50	10.25	9.50	0.00	0.00	0.00
41.0	41.00	8.42	20.00	10.50	9.75	0.00	0.00	0.00
42.0	42.00	8.44	20.50	10.75	10.00	0.00	0.00	0.00
43.0	43.00	8.46	21.00	11.00	10.25	0.00	0.00	0.00
44.0	44.00	8.48	21.50	11.25	10.50	0.00	0.00	0.00
45.0	45.00	8.50	22.00	11.50	10.75	0.00	0.00	0.00
46.0	46.00	8.52	22.50	11.75	11.00	0.00	0.00	0.00
47.0	47.00	8.54	23.00	12.00	11.25	0.00	0.00	0.00
48.0	48.00	8.56	23.50	12.25	11.50	0.00	0.00	0.00
49.0	49.00	8.58	24.00	12.50	11.75	0.00	0.00	0.00
50.0	50.00	8.60	24.50	12.75	12.00	0.00	0.00	0.00

Table D-3 Results of CASTRO-2 and CASTRO-4 calculations of burnup in 15-day outage plans.

Enrichment with U ₂₃₅	Quench criticality	15-month burnup (GWd/tU)	24-month burnup (GWd/tU)	36-month burnup (GWd/tU)	39-month burnup (GWd/tU)	42-month burnup (GWd/tU)
4.0	48.58	15.71	44.93	21.92	49.8	44.6
4.0	49.09	42.40	52.94	48.13	49.8	45.6
4.0	77.47	39.17	53.58	33.97	49.27	45.6
4.0	48.28	17.52	45.32	21.37	50.57	45.6
4.0	49.09	48.42	77.37	39.47	50.58	45.6
7.0	170.25	32.28	84.54	37.38	59.48	53.56
7.0	169.98	157.10	83.18	65.24	77.20	61.80
8.0	134.77	168.28	100.47	52.88	64.95	58.44
8.0	135.15	798.37	59.39	100.48	64.62	57.75
8.0	134.58	103.79	74.48	107.63	100.08	64.39
8.0	138.16	57.16	123.25	113.58	107.32	60.53
8.0	145.77	129.88	108.34	132.87	111.32	60.88
8.0						157.53

Table B-4. Results of CYM4D-1 and CYM4D-4 calculations of forage in 30-day cutting plans

Residual dry wt lb/ha	6 months Dry wt/ha (lb/ha) (CYM4D-1)	9 months Dry wt/ha (lb/ha) (CYM4D-1)	14 months Dry wt/ha (lb/ha) (CYM4D-1)	18 months Dry wt/ha (lb/ha) (CYM4D-1)	24 months Dry wt/ha (lb/ha) (CYM4D-1)	30 months Dry wt/ha (lb/ha) (CYM4D-1)
4.8	47.35	52.31	47.81	52.56	48	48
8.0	48.48	53.58	53.88	48.38	47.5	47.5
11.2	71.85	59.52	51.82	53.38	44.58	47.5
14.4	14.05	77.38	53.88	52.57	54.35	47.5
17.6	34.15	88.88	78.82	75.42	52.54	54.38
20.8	52.81	52.88	82.82	78.88	75.55	52.58
24.0	109.11	125.71	82.84	85.81	72.88	52.58
27.2	173.42	155.45	125.88	125.54	82.81	72.88
30.4	124.83	149.55	155.84	125.71	82.78	82.82
33.6	152.26	124.48	115.48	155.88	125.75	82.78
36.8	188.81	121.88	122.81	148.54	125.78	125.78
40.0	167.43	148.35	122.48	122.48	125.52	125.52

APPENDIX E FUEL CYCLE-COST CALCULATIONS

This appendix contains tables of all of the fuel cycle cost calculations.

Table 3-5. Base feed cycle rates for 20-day storage plants for the first 3 years.

Estimated first year dry yield	10 months		15 months		20 months		25 months		30 months	
	millibush, cwt/acre	Feed Cycle Cost Per Cwt of Dry Matter	millibush, cwt/acre	Feed Cycle Cost Per Cwt of Dry Matter	millibush, cwt/acre	Feed Cycle Cost Per Cwt of Dry Matter	millibush, cwt/acre	Feed Cycle Cost Per Cwt of Dry Matter	millibush, cwt/acre	Feed Cycle Cost Per Cwt of Dry Matter
40	1.24	\$.34	1.36	\$.34	1.48	\$.34	1.60	\$.34	1.72	\$.34
50	1.37	\$.35	1.51	\$.35	1.64	\$.35	1.77	\$.35	1.90	\$.35
60	1.51	\$.36	1.66	\$.36	1.80	\$.36	1.93	\$.36	2.06	\$.36
70	1.66	\$.36	1.82	\$.36	1.97	\$.36	2.10	\$.36	2.23	\$.36
75	1.73	\$.36	1.90	\$.36	2.05	\$.36	2.18	\$.36	2.31	\$.36
79	1.78	\$.36	1.95	\$.36	2.10	\$.36	2.23	\$.36	2.36	\$.36
80	1.81	\$.36	1.98	\$.36	2.13	\$.36	2.26	\$.36	2.39	\$.36
85	1.94	\$.36	2.13	\$.36	2.28	\$.36	2.41	\$.36	2.54	\$.36
90	2.09	\$.36	2.28	\$.36	2.43	\$.36	2.56	\$.36	2.69	\$.36
95	2.15	\$.36	2.34	\$.36	2.49	\$.36	2.62	\$.36	2.75	\$.36
100	2.20	\$.36	2.39	\$.36	2.54	\$.36	2.67	\$.36	2.80	\$.36

Table B-3 Base full cycle costs for 15-day design periods after the first 5 years

Accelerated cycle time with 15-m	15 months		18 months		24 months		36 months		48 months	
	substation	Full Cycle Cost	substation	Full Cycle Cost	substation	Full Cycle Cost	substation	Full Cycle Cost	substation	Full Cycle Cost
8.4	\$143	7.38	7.38	8.37	8.37	9.36	9.36	10.35	10.35	11.34
8.6	\$144	7.37	7.37	8.36	8.36	9.35	9.35	10.34	10.34	11.33
8.8	\$145	7.35	7.35	8.34	8.34	9.33	9.33	10.32	10.32	11.31
9.0	\$146	7.34	7.34	8.33	8.33	9.32	9.32	10.31	10.31	11.30
9.2	\$147	7.32	7.32	8.31	8.31	9.30	9.30	10.29	10.29	11.28
9.4	\$148	7.31	7.31	8.30	8.30	9.29	9.29	10.28	10.28	11.27
9.6	\$149	7.29	7.29	8.28	8.28	9.27	9.27	10.26	10.26	11.25
9.8	\$150	7.28	7.28	8.27	8.27	9.26	9.26	10.25	10.25	11.24
10.0	\$151	7.26	7.26	8.25	8.25	9.24	9.24	10.23	10.23	11.22
10.2	\$152	7.25	7.25	8.24	8.24	9.23	9.23	10.22	10.22	11.21
10.4	\$153	7.23	7.23	8.22	8.22	9.21	9.21	10.20	10.20	11.19
10.6	\$154	7.22	7.22	8.21	8.21	9.20	9.20	10.19	10.19	11.18

Table E-4. Fuel cycle costs for plants with 12-day outages for the five 8-year sets (13 participating reactors)

Conventional cycle cost with 12m	12-month		24-month		36-month		48-month	
	relativity,	relativity,	relativity,	relativity,	relativity,	relativity,	relativity,	relativity,
4.0	1.40	1.38	1.34	1.31	1.27	1.24	1.21	1.18
4.5	1.44	1.42	1.37	1.33	1.28	1.25	1.22	1.19
5.0	1.48	1.46	1.40	1.36	1.31	1.27	1.24	1.21
5.5	1.54	1.51	1.45	1.41	1.36	1.32	1.28	1.25
6.0	1.61	1.57	1.50	1.46	1.41	1.37	1.33	1.30
7.0	1.75	1.69	1.63	1.58	1.53	1.48	1.44	1.40
7.5	1.85	1.77	1.70	1.65	1.60	1.55	1.51	1.47
8.0	1.93	1.83	1.75	1.70	1.65	1.60	1.55	1.51
8.5	2.00	1.90	1.81	1.75	1.70	1.65	1.60	1.55
9.0	2.08	1.97	1.88	1.82	1.76	1.71	1.66	1.61
9.5	2.15	2.03	1.94	1.88	1.82	1.77	1.72	1.67
10.0	2.21	2.09	2.00	1.94	1.88	1.83	1.78	1.73

Table E-3. Post-cycle tests for plants with 15-day coverage for the first 4 years with 20 participating nurseries.

Post-cycle test with 4 yr	15 months		24 months		30 months		4 years
	Post Cycle Coverage m ² /m ² (m ² /m ²)	15 months m ² /m ² (m ² /m ²)	24 months m ² /m ² (m ² /m ²)	30 months m ² /m ² (m ² /m ²)	Post Cycle Coverage m ² /m ² (m ² /m ²)	4 years m ² /m ² (m ² /m ²)	
4.1	0.40	1.10	0.41	0.41	0.41	0.41	0.41
5.0	0.44	1.11	0.77	0.21	0.77	0.77	0.77
5.5	0.48	1.21	0.78	0.41	0.41	0.41	0.41
6.0	0.54	1.26	1.00	1.41	0.50	0.50	0.50
6.5	0.61	1.30	1.50	1.00	0.50	0.43	0.43
7.0	0.72	1.31	1.60	1.70	1.60	0.43	0.43
7.5	0.80	1.52	1.60	1.60	1.60	0.39	0.39
8.0	0.90	0.50	1.71	1.60	1.60	0.37	0.37
8.5	0.94	0.52	2.20	0.71	1.60	0.37	0.37
9.0	0.95	0.55	1.60	1.60	1.60	0.35	0.35
9.5	0.97	0.55	1.60	1.60	1.60	0.35	0.35
10.0	0.91	0.45	0.41	1.40	1.40	0.33	0.33

Table E-4 Real cycle costs for plants with 30-day outage for the first 3 years with 30 participating reactors.

Outage start year	10 years		14 years		20 years		30 years		40 years	
	reliability, %	Cost of Cycle Completion reliability, \$/cycle	reliability, %	Cost of Cycle Completion reliability, \$/cycle	reliability, %	Cost of Cycle Completion reliability, \$/cycle	reliability, %	Cost of Cycle Completion reliability, \$/cycle	reliability, %	Cost of Cycle Completion reliability, \$/cycle
1975	9.24	1.34	9.24	1.34	9.24	1.34	9.24	1.34	9.24	1.34
80	9.07	0.23	9.07	0.23	9.07	0.23	9.07	0.23	9.07	0.23
90	9.01	0.26	9.01	0.26	9.01	0.26	9.01	0.26	9.01	0.26
95	9.08	0.28	9.08	0.28	9.08	0.28	9.08	0.28	9.08	0.28
98	9.49	0.24	9.49	0.24	9.49	0.24	9.49	0.24	9.49	0.24
70	9.08	0.41	9.08	0.41	9.08	0.41	9.08	0.41	9.08	0.41
75	9.08	0.40	9.08	0.40	9.08	0.40	9.08	0.40	9.08	0.40
85	9.08	0.23	9.08	0.23	9.08	0.23	9.08	0.23	9.08	0.23
92	9.01	0.26	9.01	0.26	9.01	0.26	9.01	0.26	9.01	0.26
94	9.08	0.28	9.08	0.28	9.08	0.28	9.08	0.28	9.08	0.28
96	9.17	0.26	9.17	0.26	9.17	0.26	9.17	0.26	9.17	0.26
99	9.08	0.24	9.08	0.24	9.08	0.24	9.08	0.24	9.08	0.24

Table E-4 Fuel cycle cost for plants with 15-day outage for the first 3 years with 20 participating members

Load with 15% outage	12 months		14 months		20 months		24 months		36 months		48 months	
	mid-range	sub-range	mid-range	sub-range	mid-range	sub-range	mid-range	sub-range	mid-range	sub-range	mid-range	sub-range
4.0	0.40	1.00	0.41	0.91	0.41	0.91	0.41	0.91	0.41	0.91	0.41	0.91
6.0	0.46	1.10	0.46	1.10	0.47	1.10	0.47	1.10	0.47	1.10	0.47	1.10
8.0	0.48	1.18	0.48	1.18	0.49	1.18	0.49	1.18	0.49	1.18	0.49	1.18
10.0	0.54	1.25	0.54	1.25	0.55	1.25	0.55	1.25	0.55	1.25	0.55	1.25
12.0	0.61	1.33	0.61	1.33	0.62	1.33	0.62	1.33	0.62	1.33	0.62	1.33
14.0	0.72	1.47	0.72	1.47	0.73	1.47	0.73	1.47	0.73	1.47	0.73	1.47
16.0	0.80	1.60	0.80	1.60	0.81	1.60	0.81	1.60	0.81	1.60	0.81	1.60
18.0	0.90	1.75	0.90	1.75	0.91	1.75	0.91	1.75	0.91	1.75	0.91	1.75
20.0	0.96	1.87	0.96	1.87	0.97	1.87	0.97	1.87	0.97	1.87	0.97	1.87
22.0	1.10	2.02	1.10	2.02	1.11	2.02	1.11	2.02	1.11	2.02	1.11	2.02
24.0	1.20	2.16	1.20	2.16	1.21	2.16	1.21	2.16	1.21	2.16	1.21	2.16
26.0	1.30	2.30	1.30	2.30	1.31	2.30	1.31	2.30	1.31	2.30	1.31	2.30
28.0	1.40	2.44	1.40	2.44	1.41	2.44	1.41	2.44	1.41	2.44	1.41	2.44
30.0	1.50	2.58	1.50	2.58	1.51	2.58	1.51	2.58	1.51	2.58	1.51	2.58
32.0	1.60	2.72	1.60	2.72	1.61	2.72	1.61	2.72	1.61	2.72	1.61	2.72
34.0	1.70	2.86	1.70	2.86	1.71	2.86	1.71	2.86	1.71	2.86	1.71	2.86
36.0	1.80	3.00	1.80	3.00	1.81	3.00	1.81	3.00	1.81	3.00	1.81	3.00
38.0	1.90	3.14	1.90	3.14	1.91	3.14	1.91	3.14	1.91	3.14	1.91	3.14
40.0	2.00	3.28	2.00	3.28	2.01	3.28	2.01	3.28	2.01	3.28	2.01	3.28
42.0	2.10	3.42	2.10	3.42	2.11	3.42	2.11	3.42	2.11	3.42	2.11	3.42
44.0	2.20	3.56	2.20	3.56	2.21	3.56	2.21	3.56	2.21	3.56	2.21	3.56
46.0	2.30	3.70	2.30	3.70	2.31	3.70	2.31	3.70	2.31	3.70	2.31	3.70
48.0	2.40	3.84	2.40	3.84	2.41	3.84	2.41	3.84	2.41	3.84	2.41	3.84
50.0	2.50	3.98	2.50	3.98	2.51	3.98	2.51	3.98	2.51	3.98	2.51	3.98
52.0	2.60	4.12	2.60	4.12	2.61	4.12	2.61	4.12	2.61	4.12	2.61	4.12
54.0	2.70	4.26	2.70	4.26	2.71	4.26	2.71	4.26	2.71	4.26	2.71	4.26
56.0	2.80	4.40	2.80	4.40	2.81	4.40	2.81	4.40	2.81	4.40	2.81	4.40
58.0	2.90	4.54	2.90	4.54	2.91	4.54	2.91	4.54	2.91	4.54	2.91	4.54
60.0	3.00	4.68	3.00	4.68	3.01	4.68	3.01	4.68	3.01	4.68	3.01	4.68
62.0	3.10	4.82	3.10	4.82	3.11	4.82	3.11	4.82	3.11	4.82	3.11	4.82
64.0	3.20	4.96	3.20	4.96	3.21	4.96	3.21	4.96	3.21	4.96	3.21	4.96
66.0	3.30	5.10	3.30	5.10	3.31	5.10	3.31	5.10	3.31	5.10	3.31	5.10
68.0	3.40	5.24	3.40	5.24	3.41	5.24	3.41	5.24	3.41	5.24	3.41	5.24
70.0	3.50	5.38	3.50	5.38	3.51	5.38	3.51	5.38	3.51	5.38	3.51	5.38
72.0	3.60	5.52	3.60	5.52	3.61	5.52	3.61	5.52	3.61	5.52	3.61	5.52
74.0	3.70	5.66	3.70	5.66	3.71	5.66	3.71	5.66	3.71	5.66	3.71	5.66
76.0	3.80	5.80	3.80	5.80	3.81	5.80	3.81	5.80	3.81	5.80	3.81	5.80
78.0	3.90	5.94	3.90	5.94	3.91	5.94	3.91	5.94	3.91	5.94	3.91	5.94
80.0	4.00	6.08	4.00	6.08	4.01	6.08	4.01	6.08	4.01	6.08	4.01	6.08
82.0	4.10	6.22	4.10	6.22	4.11	6.22	4.11	6.22	4.11	6.22	4.11	6.22
84.0	4.20	6.36	4.20	6.36	4.21	6.36	4.21	6.36	4.21	6.36	4.21	6.36
86.0	4.30	6.50	4.30	6.50	4.31	6.50	4.31	6.50	4.31	6.50	4.31	6.50
88.0	4.40	6.64	4.40	6.64	4.41	6.64	4.41	6.64	4.41	6.64	4.41	6.64
90.0	4.50	6.78	4.50	6.78	4.51	6.78	4.51	6.78	4.51	6.78	4.51	6.78
92.0	4.60	6.92	4.60	6.92	4.61	6.92	4.61	6.92	4.61	6.92	4.61	6.92
94.0	4.70	7.06	4.70	7.06	4.71	7.06	4.71	7.06	4.71	7.06	4.71	7.06
96.0	4.80	7.20	4.80	7.20	4.81	7.20	4.81	7.20	4.81	7.20	4.81	7.20
98.0	4.90	7.34	4.90	7.34	4.91	7.34	4.91	7.34	4.91	7.34	4.91	7.34
100.0	5.00	7.48	5.00	7.48	5.01	7.48	5.01	7.48	5.01	7.48	5.01	7.48

Table 8-13 Post cycle units for plants with 11-day average for the last 5 years with 5 participating processors

Combined with year	15 months Combined Cycle Coal plants		18 months Combined Cycle Coal plants		24 months Combined Cycle Coal plants		30 months Combined Cycle Coal plants		36 months Combined Cycle Coal plants	
	units	millions	units	millions	units	millions	units	millions	units	millions
4.0	8.40	1.88	8.50	1.91	8.50	1.91	8.50	1.91	8.50	1.91
4.5	8.44	1.91	8.54	1.94	8.54	1.94	8.54	1.94	8.54	1.94
4.6	8.46	1.92	8.56	1.95	8.56	1.95	8.56	1.95	8.56	1.95
4.8	8.50	1.96	8.60	1.98	8.60	1.98	8.60	1.98	8.60	1.98
4.9	8.52	1.97	8.62	1.99	8.62	1.99	8.62	1.99	8.62	1.99
5.0	8.56	2.00	8.66	2.02	8.66	2.02	8.66	2.02	8.66	2.02
5.1	8.58	2.01	8.68	2.03	8.68	2.03	8.68	2.03	8.68	2.03
5.2	8.64	2.04	8.74	2.06	8.74	2.06	8.74	2.06	8.74	2.06
5.3	8.66	2.05	8.76	2.07	8.76	2.07	8.76	2.07	8.76	2.07
5.4	8.68	2.06	8.78	2.08	8.78	2.08	8.78	2.08	8.78	2.08
5.5	8.70	2.07	8.80	2.09	8.80	2.09	8.80	2.09	8.80	2.09
5.6	8.72	2.08	8.82	2.10	8.82	2.10	8.82	2.10	8.82	2.10
5.7	8.74	2.09	8.84	2.11	8.84	2.11	8.84	2.11	8.84	2.11
5.8	8.76	2.10	8.86	2.12	8.86	2.12	8.86	2.12	8.86	2.12
5.9	8.78	2.11	8.88	2.13	8.88	2.13	8.88	2.13	8.88	2.13
6.0	8.80	2.12	8.90	2.14	8.90	2.14	8.90	2.14	8.90	2.14
6.1	8.82	2.13	8.92	2.15	8.92	2.15	8.92	2.15	8.92	2.15
6.2	8.84	2.14	8.94	2.16	8.94	2.16	8.94	2.16	8.94	2.16
6.3	8.86	2.15	8.96	2.17	8.96	2.17	8.96	2.17	8.96	2.17
6.4	8.88	2.16	8.98	2.18	8.98	2.18	8.98	2.18	8.98	2.18
6.5	8.90	2.17	9.00	2.19	9.00	2.19	9.00	2.19	9.00	2.19
6.6	8.92	2.18	9.02	2.20	9.02	2.20	9.02	2.20	9.02	2.20
6.7	8.94	2.19	9.04	2.21	9.04	2.21	9.04	2.21	9.04	2.21
6.8	8.96	2.20	9.06	2.22	9.06	2.22	9.06	2.22	9.06	2.22
6.9	8.98	2.21	9.08	2.23	9.08	2.23	9.08	2.23	9.08	2.23
7.0	9.00	2.22	9.10	2.24	9.10	2.24	9.10	2.24	9.10	2.24

Thurs 6-12 | Fall 2024 course for students for the first | every week | participating students

Study (ref)	12 months		18 months		24 months		30 months		36 months		48 months	
	relapse-free survival (%)	relapse-free survival (95% CI)	relapse-free survival (%)	relapse-free survival (95% CI)	relapse-free survival (%)	relapse-free survival (95% CI)	relapse-free survival (%)	relapse-free survival (95% CI)	relapse-free survival (%)	relapse-free survival (95% CI)	relapse-free survival (%)	relapse-free survival (95% CI)
1	85	(83-87)	78	(76-80)	72	(70-74)	68	(66-70)	65	(63-67)	62	(60-64)
2	82	(80-84)	75	(73-77)	70	(68-72)	66	(64-68)	63	(61-65)	60	(58-62)
3	80	(78-82)	73	(71-75)	68	(66-70)	64	(62-66)	61	(59-63)	58	(56-60)
4	78	(76-80)	71	(69-73)	66	(64-68)	62	(60-64)	59	(57-61)	56	(54-58)
5	75	(73-77)	68	(66-70)	63	(61-65)	59	(57-61)	56	(54-58)	53	(51-55)
6	72	(70-74)	65	(63-67)	60	(58-62)	56	(54-58)	53	(51-55)	50	(48-52)
7	70	(68-72)	63	(61-65)	58	(56-60)	54	(52-56)	51	(49-53)	48	(46-50)
8	68	(66-70)	61	(59-63)	56	(54-58)	52	(50-54)	49	(47-51)	46	(44-48)
9	65	(63-67)	58	(56-60)	53	(51-55)	49	(47-51)	46	(44-48)	43	(41-45)
10	62	(60-64)	55	(53-57)	50	(48-52)	46	(44-48)	43	(41-45)	40	(38-42)
11	60	(58-62)	53	(51-55)	48	(46-50)	44	(42-46)	41	(39-43)	38	(36-40)
12	58	(56-60)	51	(49-53)	46	(44-48)	42	(40-44)	39	(37-41)	36	(34-38)
13	55	(53-57)	48	(46-50)	43	(41-45)	39	(37-41)	36	(34-38)	33	(31-35)
14	52	(50-54)	45	(43-47)	40	(38-42)	36	(34-38)	33	(31-35)	30	(28-32)
15	50	(48-52)	43	(41-45)	38	(36-40)	34	(32-36)	31	(29-33)	28	(26-30)
16	48	(46-50)	41	(39-43)	36	(34-38)	32	(30-34)	29	(27-31)	26	(24-28)
17	45	(43-47)	38	(36-40)	33	(31-35)	29	(27-31)	26	(24-28)	23	(21-25)
18	42	(40-44)	35	(33-37)	30	(28-32)	26	(24-28)	23	(21-25)	20	(18-22)
19	40	(38-42)	33	(31-35)	28	(26-30)	24	(22-26)	21	(19-23)	18	(16-20)
20	38	(36-40)	31	(29-33)	26	(24-28)	22	(20-24)	19	(17-21)	16	(14-18)
21	35	(33-37)	28	(26-30)	23	(21-25)	19	(17-21)	16	(14-18)	13	(11-15)
22	32	(30-34)	25	(23-27)	20	(18-22)	16	(14-18)	13	(11-15)	10	(8-12)
23	30	(28-32)	23	(21-25)	18	(16-20)	14	(12-16)	11	(9-13)	8	(6-10)
24	28	(26-30)	21	(19-23)	16	(14-18)	12	(10-14)	9	(7-11)	6	(4-8)
25	25	(23-27)	18	(16-20)	13	(11-15)	9	(7-11)	6	(4-8)	3	(1-5)
26	22	(20-24)	15	(13-17)	10	(8-12)	7	(5-9)	4	(2-6)	1	(0-3)
27	20	(18-22)	13	(11-15)	8	(6-10)	5	(3-7)	2	(0-4)	0	(0-2)
28	18	(16-20)	11	(9-13)	6	(4-8)	3	(1-5)	1	(0-3)	0	(0-2)
29	15	(13-17)	8	(6-10)	4	(2-6)	2	(0-4)	0	(0-2)	0	(0-2)
30	12	(10-14)	5	(3-7)	2	(0-4)	1	(0-3)	0	(0-2)	0	(0-2)

Table 10-10: Read cycle counts for plots with 30-day counts for the first 5 years with 1 participating master

Read Cycle Count	15 months		18 months		24 months		30 months		40 months	
	frequency	relative frequency	frequency	relative frequency	frequency	relative frequency	frequency	relative frequency	frequency	relative frequency
40	0.14	0.14	0.16	0.14	0.14	0.14	0.16	0.14	0.16	0.14
80	0.27	0.24	0.24	0.21	0.21	0.21	0.24	0.21	0.24	0.21
120	0.40	0.40	0.40	0.37	0.41	0.41	0.40	0.40	0.40	0.39
160	0.53	0.53	0.48	0.46	0.37	0.37	0.36	0.36	0.36	0.36
200	0.60	0.60	0.55	0.51	0.34	0.34	0.34	0.34	0.35	0.35
240	0.77	0.77	0.62	0.59	0.34	0.33	0.33	0.33	0.37	0.37
280	0.83	0.83	0.63	0.63	0.23	0.23	0.23	0.23	0.30	0.30
320	0.86	0.86	0.71	0.71	0.21	0.21	0.21	0.21	0.28	0.28
360	0.95	0.95	0.84	0.84	0.08	0.08	0.08	0.08	0.08	0.08
400	0.98	0.98	0.97	0.97	0.02	0.02	0.02	0.02	0.02	0.02
440	1.00	1.00	1.00	1.00	0.00	0.00	0.00	0.00	0.00	0.00

Table E-17. Fuel cycle costs for plants with 15-day swings for the first 3 years with one swing increased to 30d a subsequent

Swing length with 15d	72 months		78 months		84 months		90 months		96 months		102 months		108 months		114 months		120 months	
	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh	fuel cycle cost mill/kWh
4.5	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26
6.0	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04
6.5	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07	0.07
6.8	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08
6.9	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10
7.0	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08	0.08
7.5	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05
8.0	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02
8.5	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05
9.0	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06
10.0	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.11

Table 6-18 Fuel cycle costs for plants with 30-day ratings for the first 3 years with fuel costs increased to \$100 a kilogram

Enriched fuel cost \$/kg U ²³⁵	12-month		14-month		16-month		18-month		20-month		22-month		24-month	
	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵	\$/kg U ²³⁵
4.0	0.74	0.80	0.86	0.90	0.95	1.00	1.05	1.10	1.15	1.20	1.25	1.30	1.35	1.40
5.0	0.77	0.83	0.89	0.93	0.98	1.03	1.08	1.13	1.18	1.23	1.28	1.33	1.38	1.43
6.0	0.81	0.87	0.93	0.97	1.02	1.07	1.12	1.17	1.22	1.27	1.32	1.37	1.42	1.47
7.0	0.85	0.91	0.97	1.01	1.06	1.11	1.16	1.21	1.26	1.31	1.36	1.41	1.46	1.51
8.0	0.89	0.95	1.01	1.05	1.10	1.15	1.20	1.25	1.30	1.35	1.40	1.45	1.50	1.55
9.0	0.93	0.99	1.05	1.09	1.14	1.19	1.24	1.29	1.34	1.39	1.44	1.49	1.54	1.59
10.0	0.97	1.03	1.09	1.13	1.18	1.23	1.28	1.33	1.38	1.43	1.48	1.53	1.58	1.63
11.0	1.01	1.07	1.13	1.17	1.22	1.27	1.32	1.37	1.42	1.47	1.52	1.57	1.62	1.67
12.0	1.05	1.11	1.17	1.21	1.26	1.31	1.36	1.41	1.46	1.51	1.56	1.61	1.66	1.71
13.0	1.09	1.15	1.21	1.25	1.30	1.35	1.40	1.45	1.50	1.55	1.60	1.65	1.70	1.75
14.0	1.13	1.19	1.25	1.29	1.34	1.39	1.44	1.49	1.54	1.59	1.64	1.69	1.74	1.79
15.0	1.17	1.23	1.29	1.33	1.38	1.43	1.48	1.53	1.58	1.63	1.68	1.73	1.78	1.83
16.0	1.21	1.27	1.33	1.37	1.42	1.47	1.52	1.57	1.62	1.67	1.72	1.77	1.82	1.87
17.0	1.25	1.31	1.37	1.41	1.46	1.51	1.56	1.61	1.66	1.71	1.76	1.81	1.86	1.91
18.0	1.29	1.35	1.41	1.45	1.50	1.55	1.60	1.65	1.70	1.75	1.80	1.85	1.90	1.95
19.0	1.33	1.39	1.45	1.49	1.54	1.59	1.64	1.69	1.74	1.79	1.84	1.89	1.94	1.99
20.0	1.37	1.43	1.49	1.53	1.58	1.63	1.68	1.73	1.78	1.83	1.88	1.93	1.98	2.03

Table 1.20 Fuel cycle times for plants with 10-day outages for the first 3 years with the outage occurred in 2003 • All figures are

	3 years	4 years	5 years	6 years	7 years	8 years
Recessed from Core Cycle w/o 1 st refueling	refueling, days	refueling, days	refueling, days	refueling, days	refueling, days	refueling, days
40	10.00	10.00	10.00	10.00	10.00	10.00
50	10.00	10.00	10.00	10.00	10.00	10.00
60	10.00	10.00	10.00	10.00	10.00	10.00
70	10.00	10.00	10.00	10.00	10.00	10.00
80	10.00	10.00	10.00	10.00	10.00	10.00
90	10.00	10.00	10.00	10.00	10.00	10.00
100	10.00	10.00	10.00	10.00	10.00	10.00
110	10.00	10.00	10.00	10.00	10.00	10.00
120	10.00	10.00	10.00	10.00	10.00	10.00
130	10.00	10.00	10.00	10.00	10.00	10.00
140	10.00	10.00	10.00	10.00	10.00	10.00
150	10.00	10.00	10.00	10.00	10.00	10.00
160	10.00	10.00	10.00	10.00	10.00	10.00
170	10.00	10.00	10.00	10.00	10.00	10.00
180	10.00	10.00	10.00	10.00	10.00	10.00
190	10.00	10.00	10.00	10.00	10.00	10.00
200	10.00	10.00	10.00	10.00	10.00	10.00

Table 2-21 Fuel cycle costs for plants with 12-day outage for the 1-year cycle cost basis increased to \$25 a day per MW

MW	12-month		12-month		12-month		12-month		12-month	
	absolute	relative	absolute	relative	absolute	relative	absolute	relative	absolute	relative
Investment for Base Coal-Fuel Cycle Cost and Base Coal-Fuel Cycle Cost										
100	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
200	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
300	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
400	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
500	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
600	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
700	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
800	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
900	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
1000	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
1200	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
1400	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
1600	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
1800	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
2000	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
2200	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
2400	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
2600	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
2800	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00
3000	1.18	1.00	1.13	1.00	1.12	1.00	1.11	1.00	1.10	1.00

Table 6-12 Post cycle costs for plants with 30-day average for the first 3 years with rate code decreased to 220 a kilowatt-hour

with 30 day average	11 months		24 months		35 months		48 months		60 months	
	revenues, millions	expenses, millions	revenues, millions	expenses, millions	revenues, millions	expenses, millions	revenues, millions	expenses, millions	revenues, millions	expenses, millions
4.0	1.14	1.14	1.14	1.14	1.14	1.14	1.14	1.14	1.14	1.14
5.0	1.11	2.03	1.44	1.44	1.77	1.77	1.88	1.88	1.99	1.99
6.0	1.46	1.75	1.44	1.44	1.88	1.88	1.88	1.88	2.01	2.01
8.0	1.46	2.03	1.36	1.36	1.78	1.78	1.73	1.73	1.99	1.99
9.0	1.46	1.46	1.44	1.44	1.76	1.76	1.74	1.74	1.99	1.99
10.0	1.05	1.88	1.44	1.44	1.88	1.88	1.43	1.43	1.78	1.78
15.0	1.08	2.52	1.44	1.44	1.76	1.76	1.73	1.73	1.84	1.84
20.0	1.07	1.88	1.44	1.44	1.76	1.76	1.74	1.74	1.85	1.85
25.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
30.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
35.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
40.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
45.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
50.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
55.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
60.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
65.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
70.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
75.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
80.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
85.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
90.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
95.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88
100.0	1.46	1.46	1.44	1.44	1.88	1.88	1.73	1.73	1.88	1.88

Table 8.26 Fuel cycle costs for plants with 30-day outage for the first 3 years with component costs assumed to \$1.3 a kilogram

Enrichment \$0.1/g ²³⁵	18 months Fuel Cycle Component Costs \$1000/0.1% ²³⁵	12 months Fuel Cycle Component Costs \$1000/0.1% ²³⁵	30 months Fuel Cycle Component Costs \$1000/0.1% ²³⁵	24 months Fuel Cycle Component Costs \$1000/0.1% ²³⁵	48 months Fuel Cycle Component Costs \$1000/0.1% ²³⁵
4.8	1.41 0.40	0.37 0.36	0.18 0.78	0.01 0.01	0.01 0.01
8.5	0.40 0.40	0.37 0.37	0.64 0.64	0.11 0.11	0.01 0.01
9.9	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
8.8	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
7.6	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
7.8	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
9.0	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
8.6	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
8.5	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
8.8	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01
8.6	0.40 0.40	0.37 0.37	0.64 0.64	0.10 0.10	0.01 0.01

Table B.28 Pool cycle costs for plants with 12-day outage for the first 3 years with variable costs decreased to \$50/s (2004)

Pool cycle cost with 12-day outage	12-month availability	12-month cycle cost	12-month availability	12-month cycle cost	12-month availability	12-month cycle cost	12-month availability	12-month cycle cost
\$/MWh	\$/MWh	\$/MWh	\$/MWh	\$/MWh	\$/MWh	\$/MWh	\$/MWh	\$/MWh
0.1	0.20	0.40	0.30	0.60	0.40	0.80	0.50	1.00
0.2	0.20	0.80	0.30	1.20	0.40	1.60	0.50	2.00
0.3	0.30	1.20	0.40	1.60	0.50	2.00	0.60	2.40
0.4	0.40	1.60	0.50	2.00	0.60	2.40	0.70	2.80
0.5	0.50	2.00	0.60	2.40	0.70	2.80	0.80	3.20
0.6	0.60	2.40	0.70	2.80	0.80	3.20	0.90	3.60
0.7	0.70	2.80	0.80	3.20	0.90	3.60	1.00	4.00
0.8	0.80	3.20	0.90	3.60	1.00	4.00	1.10	4.40
0.9	0.90	3.60	1.00	4.00	1.10	4.40	1.20	4.80
1.0	1.00	4.00	1.10	4.40	1.20	4.80	1.30	5.20

Table 8-31. Fuel cycle costs for plants with 12-day outages for the first 3 years with enrichment costs decreased to 1¢/kg (1993)

Enrichment fuel cycle cost/yr	12-month enrichment cost/kgU	18-month enrichment cost/kgU	24-month enrichment cost/kgU	30-month enrichment cost/kgU	36-month enrichment cost/kgU	42-month enrichment cost/kgU
4.0	2.86	2.24	2.11	2.11	2.14	2.1
8.0	2.86	2.18	2.11	2.11	2.46	2.4
12.0	2.87	2.12	2.11	2.11	2.79	2.6
16.0	2.86	2.12	2.11	2.11	3.11	2.6
20.0	2.86	2.12	2.11	2.11	3.29	2.6
24.0	2.87	2.11	2.11	2.11	3.55	2.6
28.0	2.87	2.11	2.11	2.11	3.87	2.6
32.0	2.87	2.11	2.11	2.11	4.19	2.6
36.0	2.87	2.11	2.11	2.11	4.51	2.6
40.0	2.87	2.11	2.11	2.11	4.83	2.6
44.0	2.87	2.11	2.11	2.11	5.15	2.6
48.0	2.87	2.11	2.11	2.11	5.47	2.6
52.0	2.87	2.11	2.11	2.11	5.79	2.6
56.0	2.87	2.11	2.11	2.11	6.11	2.6
60.0	2.87	2.11	2.11	2.11	6.43	2.6

Table B-34 Fuel cycle costs for plants with 30-day outage for the first 3 years with maintenance costs increased to \$110 a MWd

Estimated SWU, ^a %	12 months		24 months		30 months		36 months		48 months	
	fuel cycle costs, \$/MWh	combined costs, \$/MWh	fuel cycle costs, \$/MWh	combined costs, \$/MWh	fuel cycle costs, \$/MWh	combined costs, \$/MWh	fuel cycle costs, \$/MWh	combined costs, \$/MWh	fuel cycle costs, \$/MWh	combined costs, \$/MWh
4.0	8.08	8.34	8.02	8.28	8.01	8.27	7.99	8.25	7.97	8.23
4.5	8.59	8.85	8.51	8.77	8.50	8.76	8.49	8.75	8.47	8.73
5.0	9.08	9.36	9.02	9.28	9.01	9.27	8.99	9.25	8.97	9.23
5.5	9.57	9.85	9.51	9.77	9.50	9.76	9.49	9.75	9.47	9.73
6.0	10.06	10.36	10.02	10.28	10.01	10.27	9.99	10.25	9.97	10.23
7.0	11.08	11.38	11.02	11.28	11.01	11.27	10.99	11.25	10.97	11.23
8.0	12.10	12.40	12.02	12.28	12.01	12.27	11.99	12.25	11.97	12.23
9.0	13.12	13.42	13.02	13.28	13.01	13.27	12.99	13.25	12.97	13.23
10.0	14.14	14.44	14.02	14.28	14.01	14.27	13.99	14.25	13.97	14.23
11.0	15.16	15.46	15.02	15.28	15.01	15.27	14.99	15.25	14.97	15.23
12.0	16.18	16.48	16.02	16.28	16.01	16.27	15.99	16.25	15.97	16.23
13.0	17.20	17.50	17.02	17.28	17.01	17.27	16.99	17.25	16.97	17.23
14.0	18.22	18.52	18.02	18.28	18.01	18.27	17.99	18.25	17.97	18.23
15.0	19.24	19.54	19.02	19.28	19.01	19.27	18.99	19.25	18.97	19.23
16.0	20.26	20.56	20.02	20.28	20.01	20.27	19.99	20.25	19.97	20.23
17.0	21.28	21.58	21.02	21.28	21.01	21.27	20.99	21.25	20.97	21.23

Table B-10 Fuel cycle costs for plants with 12-day outages for the first 3 years with stochastic costs increased to \$150 a \$/Btu

Investment cost \$/kW _e	12 months		14 months		16 months		18 months		20 months	
	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu	in \$/Btu/hp, in \$/Btu
4.0	0.11	0.07	0.08	0.10	0.10	0.12	0.09	0.11	0.11	0.13
4.5	0.10	0.06	0.07	0.09	0.08	0.10	0.08	0.09	0.09	0.11
5.0	0.09	0.05	0.06	0.08	0.07	0.09	0.07	0.08	0.08	0.10
5.5	0.08	0.05	0.05	0.07	0.06	0.08	0.06	0.07	0.07	0.09
6.0	0.08	0.04	0.05	0.06	0.05	0.07	0.05	0.06	0.06	0.08
7.0	0.08	0.04	0.05	0.06	0.05	0.07	0.05	0.06	0.06	0.08
7.5	0.07	0.03	0.04	0.05	0.04	0.06	0.04	0.05	0.05	0.07
8.0	0.07	0.03	0.04	0.05	0.04	0.06	0.04	0.05	0.05	0.07
8.5	0.07	0.03	0.04	0.05	0.04	0.06	0.04	0.05	0.05	0.07
9.0	0.06	0.03	0.04	0.05	0.04	0.06	0.04	0.05	0.05	0.07
9.5	0.06	0.03	0.04	0.05	0.04	0.06	0.04	0.05	0.05	0.07
10.0	0.06	0.03	0.04	0.05	0.04	0.06	0.04	0.05	0.05	0.07

Table B.10 Fuel cycle costs for plants with 18-day outages for the first 3 years with distribution costs assumed by DOE

Reprocessed fuel, kgU_{235}	24 months Fuel Cycle Cost/Fuel Cycle, \$/kgU ₂₃₅	36 months Fuel Cycle Cost/Fuel Cycle, \$/kgU ₂₃₅	48 months Fuel Cycle Cost/Fuel Cycle, \$/kgU ₂₃₅	60 months Fuel Cycle Cost/Fuel Cycle, \$/kgU ₂₃₅	72 months Fuel Cycle Cost/Fuel Cycle, \$/kgU ₂₃₅
4.8	0.24	0.30	0.33	0.35	0.36
9.6	0.28	0.36	0.40	0.43	0.45
14.4	0.29	0.38	0.42	0.46	0.48
19.2	0.40	0.50	0.55	0.61	0.64
24.0	0.44	0.56	0.62	0.69	0.73
28.8	0.46	0.59	0.65	0.73	0.77
33.6	0.48	0.62	0.68	0.76	0.81
38.4	0.50	0.64	0.71	0.79	0.84
43.2	0.51	0.65	0.73	0.81	0.86
48.0	0.52	0.66	0.74	0.83	0.88
52.8	0.53	0.67	0.75	0.84	0.89
57.6	0.54	0.68	0.76	0.85	0.90
62.4	0.55	0.69	0.77	0.86	0.91
67.2	0.56	0.70	0.78	0.87	0.92
72.0	0.56	0.71	0.79	0.88	0.93
76.8	0.57	0.72	0.80	0.89	0.94
81.6	0.58	0.73	0.81	0.90	0.95
86.4	0.58	0.74	0.82	0.91	0.96
91.2	0.59	0.75	0.83	0.92	0.97
96.0	0.59	0.75	0.84	0.93	0.97
100.8	0.60	0.76	0.84	0.94	0.98
105.6	0.60	0.76	0.85	0.94	0.98
110.4	0.61	0.77	0.85	0.95	0.99
115.2	0.61	0.77	0.86	0.95	0.99
120.0	0.62	0.78	0.86	0.96	1.00
124.8	0.62	0.78	0.87	0.96	1.00
129.6	0.63	0.79	0.87	0.97	1.00
134.4	0.63	0.79	0.88	0.97	1.01
139.2	0.64	0.80	0.88	0.98	1.01
144.0	0.64	0.80	0.89	0.98	1.01
148.8	0.64	0.81	0.89	0.99	1.02
153.6	0.65	0.81	0.90	0.99	1.02
158.4	0.65	0.82	0.90	1.00	1.02
163.2	0.66	0.82	0.91	1.00	1.03
168.0	0.66	0.83	0.91	1.01	1.03
172.8	0.66	0.83	0.92	1.01	1.03
177.6	0.67	0.84	0.92	1.02	1.04
182.4	0.67	0.84	0.93	1.02	1.04
187.2	0.68	0.85	0.93	1.03	1.04
192.0	0.68	0.85	0.94	1.03	1.05
196.8	0.68	0.86	0.94	1.04	1.05
201.6	0.69	0.86	0.95	1.04	1.05
206.4	0.69	0.87	0.95	1.05	1.06
211.2	0.69	0.87	0.96	1.05	1.06
216.0	0.70	0.88	0.96	1.06	1.06
220.8	0.70	0.88	0.97	1.06	1.07
225.6	0.70	0.89	0.97	1.07	1.07
230.4	0.71	0.89	0.98	1.07	1.07
235.2	0.71	0.90	0.98	1.08	1.08
240.0	0.71	0.90	0.99	1.08	1.08
244.8	0.72	0.91	0.99	1.09	1.08
249.6	0.72	0.91	1.00	1.09	1.09
254.4	0.72	0.92	1.00	1.10	1.09
259.2	0.73	0.92	1.01	1.10	1.10
264.0	0.73	0.93	1.01	1.11	1.10
268.8	0.73	0.93	1.02	1.11	1.10
273.6	0.74	0.94	1.02	1.12	1.11
278.4	0.74	0.94	1.03	1.12	1.11
283.2	0.74	0.95	1.03	1.13	1.12
288.0	0.75	0.95	1.04	1.13	1.12
292.8	0.75	0.96	1.04	1.14	1.12
297.6	0.75	0.96	1.05	1.14	1.13
302.4	0.76	0.97	1.05	1.15	1.13
307.2	0.76	0.97	1.06	1.15	1.13
312.0	0.76	0.98	1.06	1.16	1.14
316.8	0.77	0.98	1.07	1.16	1.14
321.6	0.77	0.99	1.07	1.17	1.14
326.4	0.77	0.99	1.08	1.17	1.15
331.2	0.78	1.00	1.08	1.18	1.15
336.0	0.78	1.00	1.09	1.18	1.15
340.8	0.78	1.01	1.09	1.19	1.16
345.6	0.79	1.01	1.10	1.19	1.16
350.4	0.79	1.02	1.10	1.20	1.16
355.2	0.79	1.02	1.11	1.20	1.17
360.0	0.80	1.03	1.11	1.21	1.17
364.8	0.80	1.03	1.12	1.21	1.17
369.6	0.80	1.04	1.12	1.22	1.18
374.4	0.81	1.04	1.13	1.22	1.18
379.2	0.81	1.05	1.13	1.23	1.18
384.0	0.81	1.05	1.14	1.23	1.19
388.8	0.82	1.06	1.14	1.24	1.19
393.6	0.82	1.06	1.15	1.24	1.19
398.4	0.82	1.07	1.15	1.25	1.20
403.2	0.83	1.07	1.16	1.25	1.20
408.0	0.83	1.08	1.16	1.26	1.20
412.8	0.83	1.08	1.17	1.26	1.21
417.6	0.84	1.09	1.17	1.27	1.21
422.4	0.84	1.09	1.18	1.27	1.21
427.2	0.84	1.10	1.18	1.28	1.22
432.0	0.85	1.10	1.19	1.28	1.22
436.8	0.85	1.11	1.19	1.29	1.22
441.6	0.85	1.11	1.20	1.29	1.23
446.4	0.86	1.12	1.20	1.30	1.23
451.2	0.86	1.12	1.21	1.30	1.23
456.0	0.86	1.13	1.21	1.31	1.24
460.8	0.87	1.13	1.22	1.31	1.24
465.6	0.87	1.14	1.22	1.32	1.24
470.4	0.87	1.14	1.23	1.32	1.25
475.2	0.88	1.15	1.23	1.33	1.25
480.0	0.88	1.15	1.24	1.33	1.25
484.8	0.88	1.16	1.24	1.34	1.26
489.6	0.89	1.16	1.25	1.34	1.26
494.4	0.89	1.17	1.25	1.35	1.26
499.2	0.89	1.17	1.26	1.35	1.27
504.0	0.90	1.18	1.26	1.36	1.27
508.8	0.90	1.18	1.27	1.36	1.27
513.6	0.90	1.19	1.27	1.37	1.28
518.4	0.91	1.19	1.28	1.37	1.28
523.2	0.91	1.20	1.28	1.38	1.28
528.0	0.91	1.20	1.29	1.38	1.29
532.8	0.92	1.21	1.29	1.39	1.29
537.6	0.92	1.21	1.30	1.39	1.30
542.4	0.92	1.22	1.30	1.40	1.30
547.2	0.93	1.22	1.31	1.40	1.31
552.0	0.93	1.23	1.31	1.41	1.31
556.8	0.93	1.23	1.32	1.41	1.32
561.6	0.94	1.24	1.32	1.42	1.32
566.4	0.94	1.24	1.33	1.42	1.33
571.2	0.94	1.25	1.33	1.43	1.33
576.0	0.95	1.25	1.34	1.43	1.34
580.8	0.95	1.26	1.34	1.44	1.34
585.6	0.95	1.26	1.35	1.44	1.35
590.4	0.96	1.27	1.35	1.45	1.35
595.2	0.96	1.27	1.36	1.45	1.36
600.0	0.96	1.28	1.36	1.46	1.36
604.8	0.97	1.28	1.37	1.46	1.37
609.6	0.97	1.29	1.37	1.47	1.37
614.4	0.97	1.29	1.38	1.47	1.38
619.2	0.98	1.30	1.38	1.48	1.38
624.0	0.98	1.30	1.39	1.48	1.39
628.8	0.98	1.31	1.39	1.49	1.39
633.6	0.99	1.31	1.40	1.49	1.40
638.4	0.99	1.32	1.40	1.50	1.40
643.2	0.99	1.32	1.41	1.50	1.41
648.0	1.00	1.33	1.41	1.51	1.41
652.8	1.00	1.33	1.42	1.51	1.42
657.6	1.00	1.34	1.42	1.52	1.42
662.4	1.01	1.34	1.43	1.52	1.43
667.2	1.01	1.35	1.43	1.53	1.43
672.0	1.01	1.35	1.44	1.53	1.44
676.8	1.02	1.36	1.44	1.54	1.44
681.6	1.02	1.36	1.45	1.54	1.45
686.4	1.02	1.37	1.45	1.55	1.45
691.2	1.03	1.37	1.46	1.55	1.46
696.0	1.03	1.38	1.46	1.56	1.46
700.8	1.03	1.38	1.47	1.56	1.47
705.6	1.04	1.39	1.47	1.57	1.47
710.4	1.04	1.39	1.48	1.57	1.48
715.2	1.04	1.40	1.48	1.58	1.48
720.0	1.05	1.40	1.49	1.58	1.49
724.8	1.05	1.41	1.49	1.59	1.49
729.6	1.05	1.41	1.50	1.59	1.50
734.4	1.06	1.42	1.50	1.60	1.50
739.2	1.06	1.42	1.51	1.60	1.51
744.0	1.06	1.43	1.51	1.61	1.51
748.8	1.07	1.43	1.52	1.61	1.52
753.6	1.07	1.44	1.52	1.62	1.52
758.4	1.07	1.44	1.53	1.62	1.53
763.2	1.08	1.45	1.53	1.63	1.53
768.0	1.08	1.45	1.54	1.63	1.54
772.8	1.08	1.46	1.54	1.64	1.54
777.6	1.09	1.46	1.55	1.64	1.55
782.4	1.09	1.47	1.55	1.65	1.55
787.2	1.09	1.47	1.56	1.65	1.56
792.0	1.10	1.48	1.56	1.66	1.56
796.8	1.10	1.48	1.57	1.66	1.57
801.6	1.10	1.49	1.57	1.67	1.57
806.4	1.11	1.49	1.58	1.67	1.58
811.2	1.11	1.50	1.58	1.68	1.58
816.0	1.11	1.50	1.59	1.68	1.59
820.8	1.12	1.51	1.59	1.69	1.59
825.6	1.12	1.51	1.60	1.69	1.60
830.4	1.12	1.52	1.60	1.70	1.60
835.2	1.13	1.52	1.61	1.70	1.61
840.0	1.13	1.53	1.61	1.71	1.61
844.8	1.13	1.53	1.62	1.71	1.62
849.6	1.14	1.54	1.62	1.72	1.62
854.4	1.14	1.54	1.63	1.72	1.63
859.2	1.14	1.55	1.63	1.73	1.63
864.0	1.15	1.55	1.64	1.73	1.64
868.8	1.15	1.56	1.64	1.74	1.64
873.6	1.15	1.56	1.65	1.74	1.65
878.4	1.16	1.57	1.65	1.75	1.65
883.2	1.16	1.57	1.66	1.75	1.66
888.0	1.16	1.58	1.66	1.76	1.66
892.8	1.17	1.58	1.67	1.76	1.67
897.6	1.17	1.59	1.67	1.77	1.67
902.4	1.17	1.59	1.68	1.77	1.68
907.2	1.18	1.60	1.68	1.78	1.68
912.0	1.18	1.60	1.69	1.78	1.69
916.8	1.18	1.61	1.69	1.79	1.69
921.6	1.19	1.61	1.70	1.79	1.70
926.4	1.19	1.62	1.70	1.80	1.70
931.2	1.19	1.62	1.71	1.80	1.71
936.0	1.20	1.63	1.71	1.81	1.71
940.8	1.20	1.63	1.72	1.81	1.72
945.6	1.20	1.64	1.72	1.82	1.72
950.4	1.21	1.64	1.73	1.82	1.73
955.2	1.21				

Table B-11 Fuel cycle costs for plants with 30-day swings for the first 3 years with breakeven costs normalized to 2004

Breakeven cost, \$/MWh	10-month fuel cycle		18-month fuel cycle		24-month fuel cycle		30-month fuel cycle		40-month fuel cycle	
	fuel costs	variable costs	fuel costs	variable costs	fuel costs	variable costs	fuel costs	variable costs	fuel costs	variable costs
1.0	0.36	0.44	0.36	0.44	0.37	0.45	0.38	0.46	0.39	0.47
2.0	0.37	0.41	0.38	0.41	0.39	0.41	0.40	0.40	0.40	0.40
3.0	0.40	0.40	0.39	0.39	0.40	0.39	0.40	0.39	0.40	0.39
4.0	0.42	0.38	0.40	0.38	0.41	0.38	0.41	0.38	0.41	0.38
5.0	0.43	0.34	0.41	0.34	0.42	0.34	0.42	0.34	0.42	0.34
6.0	0.44	0.30	0.42	0.30	0.43	0.30	0.43	0.30	0.43	0.30
7.0	0.45	0.26	0.43	0.26	0.44	0.26	0.44	0.26	0.44	0.26
8.0	0.47	0.22	0.44	0.22	0.45	0.22	0.45	0.22	0.45	0.22
9.0	0.48	0.18	0.45	0.18	0.46	0.18	0.46	0.18	0.46	0.18
10.0	0.49	0.14	0.46	0.14	0.47	0.14	0.47	0.14	0.47	0.14
11.0	0.50	0.10	0.47	0.10	0.48	0.10	0.48	0.10	0.48	0.10
12.0	0.51	0.06	0.48	0.06	0.49	0.06	0.49	0.06	0.49	0.06

Table 3-40: Fuel cycle costs for plants with 1-day outages for the first 3 years with alternative costs discussed by LBN

Reactor with LBN	14 months outage/yr, \$/MWh _{th}	14 months outage/yr, Cost Fuel Cycle Cost \$MWh _{th}	14 months outage/yr, \$/MWh _{th}	14 months outage/yr, Cost Fuel Cycle Cost \$MWh _{th}	14 months outage/yr, \$/MWh _{th}
4B	8.37	7.75	7.83	8.01	8.01
6B	8.38	7.75	7.75	8.04	8.04
5B	8.40	7.75	7.84	8.10	8.10
8A	8.56	7.75	7.75	8.23	8.23
8B	8.47	7.75	7.84	8.23	8.24
7A	8.59	7.80	7.83	7.95	8.25
7B	8.77	7.80	7.84	7.75	8.15
6A	8.49	7.84	7.85	7.75	8.23
8C	8.54	8.08	7.87	7.91	7.91
8D	8.73	8.08	7.85	7.83	7.83
9A	8.37	8.21	7.85	7.83	8.21
9B	8.45	8.50	8.00	7.75	8.50

Table B-41 Fuel cycle costs for plants with 18-day average for the first 3 years with licensing costs decreased by 50%

Electricity cost, \$/MWh	18-month fuel cycle cost with 18-day average, \$/MWh	18-month fuel cycle cost with 18-day average, \$/MWh	18-month fuel cycle cost with 18-day average, \$/MWh	20-month fuel cycle cost with 18-day average, \$/MWh	40-month fuel cycle cost with 18-day average, \$/MWh
4.8	8.28	8.28	8.28	8.13	8.08
5.0	8.33	8.33	8.33	8.43	8.43
5.4	8.75	8.75	8.75	8.25	8.25
6.0	9.35	9.35	9.35	8.71	8.71
6.6	9.83	9.83	9.83	9.34	9.34
7.0	10.35	10.35	10.35	9.88	9.88
7.6	10.95	10.95	10.95	1.04	1.04
8.0	11.75	11.75	11.75	1.08	1.08
8.6	12.67	12.67	12.67	1.37	1.37
9.0	13.68	13.68	13.68	1.57	1.57
9.6	14.78	14.78	14.78	1.77	1.77
10.0	15.88	15.88	15.88	1.98	1.98

Table E-40 Fuel-cycle costs for glass with 10-day outage for the first 3 years with fabrication costs decreased by 20%.

Normalized costs \$/MWh	4 months		8 months		16 months		24 months		40 months	
	initial \$/MWh	reduction %	initial \$/MWh	reduction %	initial \$/MWh	reduction %	initial \$/MWh	reduction %	initial \$/MWh	reduction %
4.0	8.73	0.43	8.73	0.18	8.73	0.14	8.73	0.04	8.73	0.01
5.0	8.78	0.79	8.78	0.34	8.78	0.30	8.78	0.08	8.78	0.04
6.0	8.81	0.81	8.81	0.44	8.81	0.33	8.81	0.14	8.81	0.06
8.0	8.89	0.89	8.89	0.54	8.89	0.43	8.89	0.24	8.89	0.10
9.0	8.96	0.96	8.96	0.60	8.96	0.49	8.96	0.30	8.96	0.13
10.0	9.00	0.99	9.00	0.63	9.00	0.52	9.00	0.33	9.00	0.15
12.0	9.07	0.97	9.07	0.66	9.07	0.55	9.07	0.36	9.07	0.17
15.0	9.11	0.99	9.11	0.69	9.11	0.58	9.11	0.39	9.11	0.19
20.0	9.14	0.99	9.14	0.71	9.14	0.60	9.14	0.41	9.14	0.21
25.0	9.17	0.99	9.17	0.72	9.17	0.61	9.17	0.42	9.17	0.22
30.0	9.19	0.99	9.19	0.73	9.19	0.62	9.19	0.43	9.19	0.23
40.0	9.23	0.99	9.23	0.74	9.23	0.63	9.23	0.44	9.23	0.24
50.0	9.25	0.99	9.25	0.75	9.25	0.64	9.25	0.45	9.25	0.25
60.0	9.27	0.99	9.27	0.75	9.27	0.64	9.27	0.45	9.27	0.25
70.0	9.28	0.99	9.28	0.75	9.28	0.64	9.28	0.45	9.28	0.25
80.0	9.29	0.99	9.29	0.75	9.29	0.64	9.29	0.45	9.29	0.25
100.0	9.30	0.99	9.30	0.75	9.30	0.64	9.30	0.45	9.30	0.25

Table E-46 Fuel cycle costs for plants with 18-day outages for the first 3 years with actual licensing costs incurred by 2004

Estimated net cycle construction cost, \$/kW _e	12 months		18 months		24 months		30 months		36 months	
	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e	initially, \$/kW _e
44	8.46	7.63	8.62	8.62	8.68	8.68	8.68	8.68	8.68	8.68
50	8.41	7.54	7.72	7.72	8.28	8.28	8.28	8.28	8.28	8.28
53	8.46	7.54	7.68	7.68	8.00	8.00	8.00	8.00	8.00	8.00
55	8.51	7.71	7.81	7.81	7.71	7.71	7.71	7.71	7.71	7.71
56	8.51	7.77	7.82	7.82	7.88	7.88	7.88	7.88	7.88	7.88
56	8.58	7.84	7.81	7.81	7.88	7.88	7.88	7.88	7.88	7.88
56	8.79	7.96	7.96	7.96	7.99	7.99	7.99	7.99	7.99	7.99
58	8.88	8.02	7.72	7.72	7.88	7.88	7.88	7.88	7.88	7.88
58	8.88	8.05	7.77	7.77	7.88	7.88	7.88	7.88	7.88	7.88
58	8.75	8.05	7.82	7.82	7.88	7.88	7.88	7.88	7.88	7.88
58	8.75	8.03	7.82	7.82	7.88	7.88	7.88	7.88	7.88	7.88
70.5	8.58	8.47	8.58	8.58	7.84	7.84	7.84	7.84	7.84	7.84

Table B-47 Fruit apple scores for plants with 30-day ratings for the first 5 years with above bearing units determined by 2006

Stratification mL/gm	10 years		20 years		30 years		40 years	
	mean	std dev	mean	std dev	mean	std dev	mean	std dev
4.0	0.36	0.23	0.33	0.33	0.40	0.30	0.45	0.25
5.0	0.33	0.23	0.27	0.30	0.40	0.28	0.45	0.28
6.0	0.27	0.20	0.26	0.25	0.23	0.23	0.28	0.24
8.0	0.24	0.21	0.21	0.20	0.20	0.20	0.28	0.28
8.5	0.40	0.28	0.28	0.26	0.25	0.25	0.27	0.27
9.0	0.50	0.28	0.28	0.21	0.30	0.25	0.28	0.25
9.5	0.60	0.44	0.44	0.32	0.47	0.30	0.48	0.28
10.0	0.74	0.50	0.50	0.38	0.50	0.35	0.50	0.25
10.5	0.69	0.38	0.58	0.28	0.58	0.25	0.55	0.25
11.0	0.67	0.27	0.57	0.25	0.55	0.25	0.55	0.25
11.5	0.93	0.38	0.88	0.30	0.85	0.25	0.75	0.25
12.0	0.27	0.04	0.04	0.00	0.00	0.00	0.00	0.00

Table 8.48 Fuel-cycle costs for plants with 18-day outages for the first 3 years with interest-bearing costs decreased by 50%.

Interest-bearing cost of fuel-cycle credit	10 years	14 years	18 years	22 years	26 years	30 years
with 18-day outages	relative	relative	relative	relative	relative	relative
1.0	0.34	2.81	7.48	1.00	0.00	0.00
0.5	0.31	2.53	6.74	0.94	0.00	0.00
0.0	0.41	3.11	7.99	1.00	0.00	0.00
0.5	0.46	3.31	8.33	1.03	0.00	0.00
0.0	0.53	3.79	9.38	1.00	0.00	0.00
2.0	0.60	4.02	9.82	1.07	0.00	0.00
2.5	0.70	4.67	11.31	1.00	0.00	0.00
0.0	0.64	3.88	9.49	1.00	0.00	0.00
0.0	0.69	4.06	9.79	1.00	0.00	0.00
0.0	0.56	3.17	7.46	0.77	0.00	0.00
0.0	0.61	3.33	7.88	0.80	0.00	0.00
0.0	0.66	3.51	8.31	0.86	0.00	0.00
0.0	0.68	3.58	8.43	0.87	0.00	0.00

Table 8.58 Total cycle times for plants with 12-day intervals for the first 3 years with initial inventory, units received by 2004

Inventory at 1 Jan	12 months		24 months		36 months		48 months	
	initial inv.	initial inv.	initial inv.	initial inv.	initial inv.	initial inv.	initial inv.	initial inv.
40	8.47	7.44	8.50	8.43	8.46	8.46	8.46	8.46
80	8.48	7.74	7.74	8.39	8.39	8.39	8.39	8.39
120	8.50	7.75	7.75	8.39	8.39	8.39	8.39	8.39
160	8.50	7.74	7.68	7.83	8.30	8.30	8.30	8.30
200	8.50	7.81	7.61	7.71	8.20	8.20	8.20	8.20
240	8.50	7.84	7.68	7.70	7.97	7.97	7.97	7.97
280	8.50	7.85	7.70	7.71	7.98	7.98	7.98	7.98
320	8.50	8.05	7.85	7.73	7.73	7.73	7.73	7.73
360	8.50	8.20	7.85	7.82	7.82	7.82	7.82	7.82
400	8.50	8.26	8.01	7.86	7.86	7.86	7.86	7.86
440	8.50	8.44	8.28	7.88	7.88	7.88	7.88	7.88

Table 8-53. Final cycle costs for plants with 30-day ramps for the first 3 years with related licensing costs increased by 20%.

Investment \$/kW _{peak}	10 months		20 months		30 months		40 months		50 months	
	initial costs	interest	initial costs	interest	initial costs	interest	initial costs	interest	initial costs	interest
\$0	\$ 0	\$ 0	\$ 0	\$ 0	\$ 0	\$ 0	\$ 0	\$ 0	\$ 0	\$ 0
\$1	\$ 1	\$ 0.21	\$ 1	\$ 0.20	\$ 1	\$ 0.19	\$ 1	\$ 0.18	\$ 1	\$ 0.16
\$2	\$ 2	\$ 0.40	\$ 2	\$ 0.39	\$ 2	\$ 0.38	\$ 2	\$ 0.37	\$ 2	\$ 0.34
\$3	\$ 3	\$ 0.59	\$ 3	\$ 0.58	\$ 3	\$ 0.57	\$ 3	\$ 0.56	\$ 3	\$ 0.52
\$4	\$ 4	\$ 0.78	\$ 4	\$ 0.77	\$ 4	\$ 0.76	\$ 4	\$ 0.75	\$ 4	\$ 0.71
\$5	\$ 5	\$ 0.96	\$ 5	\$ 0.95	\$ 5	\$ 0.94	\$ 5	\$ 0.93	\$ 5	\$ 0.88
\$6	\$ 6	\$ 1.15	\$ 6	\$ 1.14	\$ 6	\$ 1.13	\$ 6	\$ 1.12	\$ 6	\$ 1.07
\$7	\$ 7	\$ 1.33	\$ 7	\$ 1.32	\$ 7	\$ 1.31	\$ 7	\$ 1.30	\$ 7	\$ 1.25
\$8	\$ 8	\$ 1.52	\$ 8	\$ 1.51	\$ 8	\$ 1.50	\$ 8	\$ 1.49	\$ 8	\$ 1.43
\$9	\$ 9	\$ 1.70	\$ 9	\$ 1.69	\$ 9	\$ 1.68	\$ 9	\$ 1.67	\$ 9	\$ 1.61
\$10	\$ 10	\$ 1.89	\$ 10	\$ 1.88	\$ 10	\$ 1.87	\$ 10	\$ 1.86	\$ 10	\$ 1.79
\$11	\$ 11	\$ 2.07	\$ 11	\$ 2.06	\$ 11	\$ 2.05	\$ 11	\$ 2.04	\$ 11	\$ 1.97
\$12	\$ 12	\$ 2.26	\$ 12	\$ 2.25	\$ 12	\$ 2.24	\$ 12	\$ 2.23	\$ 12	\$ 2.15
\$13	\$ 13	\$ 2.44	\$ 13	\$ 2.43	\$ 13	\$ 2.42	\$ 13	\$ 2.41	\$ 13	\$ 2.33
\$14	\$ 14	\$ 2.63	\$ 14	\$ 2.62	\$ 14	\$ 2.61	\$ 14	\$ 2.60	\$ 14	\$ 2.51
\$15	\$ 15	\$ 2.81	\$ 15	\$ 2.80	\$ 15	\$ 2.79	\$ 15	\$ 2.78	\$ 15	\$ 2.69
\$16	\$ 16	\$ 3.00	\$ 16	\$ 2.99	\$ 16	\$ 2.98	\$ 16	\$ 2.97	\$ 16	\$ 2.87
\$17	\$ 17	\$ 3.18	\$ 17	\$ 3.17	\$ 17	\$ 3.16	\$ 17	\$ 3.15	\$ 17	\$ 3.05
\$18	\$ 18	\$ 3.37	\$ 18	\$ 3.36	\$ 18	\$ 3.35	\$ 18	\$ 3.34	\$ 18	\$ 3.23
\$19	\$ 19	\$ 3.55	\$ 19	\$ 3.54	\$ 19	\$ 3.53	\$ 19	\$ 3.52	\$ 19	\$ 3.41
\$20	\$ 20	\$ 3.74	\$ 20	\$ 3.73	\$ 20	\$ 3.72	\$ 20	\$ 3.71	\$ 20	\$ 3.59
\$21	\$ 21	\$ 3.92	\$ 21	\$ 3.91	\$ 21	\$ 3.90	\$ 21	\$ 3.89	\$ 21	\$ 3.77
\$22	\$ 22	\$ 4.11	\$ 22	\$ 4.10	\$ 22	\$ 4.09	\$ 22	\$ 4.08	\$ 22	\$ 3.95
\$23	\$ 23	\$ 4.29	\$ 23	\$ 4.28	\$ 23	\$ 4.27	\$ 23	\$ 4.26	\$ 23	\$ 4.13
\$24	\$ 24	\$ 4.48	\$ 24	\$ 4.47	\$ 24	\$ 4.46	\$ 24	\$ 4.45	\$ 24	\$ 4.31
\$25	\$ 25	\$ 4.66	\$ 25	\$ 4.65	\$ 25	\$ 4.64	\$ 25	\$ 4.63	\$ 25	\$ 4.49
\$26	\$ 26	\$ 4.85	\$ 26	\$ 4.84	\$ 26	\$ 4.83	\$ 26	\$ 4.82	\$ 26	\$ 4.67
\$27	\$ 27	\$ 5.03	\$ 27	\$ 5.02	\$ 27	\$ 5.01	\$ 27	\$ 5.00	\$ 27	\$ 4.85
\$28	\$ 28	\$ 5.22	\$ 28	\$ 5.21	\$ 28	\$ 5.20	\$ 28	\$ 5.19	\$ 28	\$ 5.03
\$29	\$ 29	\$ 5.40	\$ 29	\$ 5.39	\$ 29	\$ 5.38	\$ 29	\$ 5.37	\$ 29	\$ 5.21
\$30	\$ 30	\$ 5.59	\$ 30	\$ 5.58	\$ 30	\$ 5.57	\$ 30	\$ 5.56	\$ 30	\$ 5.39
\$31	\$ 31	\$ 5.77	\$ 31	\$ 5.76	\$ 31	\$ 5.75	\$ 31	\$ 5.74	\$ 31	\$ 5.57
\$32	\$ 32	\$ 5.96	\$ 32	\$ 5.95	\$ 32	\$ 5.94	\$ 32	\$ 5.93	\$ 32	\$ 5.75
\$33	\$ 33	\$ 6.14	\$ 33	\$ 6.13	\$ 33	\$ 6.12	\$ 33	\$ 6.11	\$ 33	\$ 5.93
\$34	\$ 34	\$ 6.33	\$ 34	\$ 6.32	\$ 34	\$ 6.31	\$ 34	\$ 6.30	\$ 34	\$ 6.11
\$35	\$ 35	\$ 6.51	\$ 35	\$ 6.50	\$ 35	\$ 6.49	\$ 35	\$ 6.48	\$ 35	\$ 6.29
\$36	\$ 36	\$ 6.70	\$ 36	\$ 6.69	\$ 36	\$ 6.68	\$ 36	\$ 6.67	\$ 36	\$ 6.47
\$37	\$ 37	\$ 6.88	\$ 37	\$ 6.87	\$ 37	\$ 6.86	\$ 37	\$ 6.85	\$ 37	\$ 6.65
\$38	\$ 38	\$ 7.07	\$ 38	\$ 7.06	\$ 38	\$ 7.05	\$ 38	\$ 7.04	\$ 38	\$ 6.83
\$39	\$ 39	\$ 7.25	\$ 39	\$ 7.24	\$ 39	\$ 7.23	\$ 39	\$ 7.22	\$ 39	\$ 7.01
\$40	\$ 40	\$ 7.44	\$ 40	\$ 7.43	\$ 40	\$ 7.42	\$ 40	\$ 7.41	\$ 40	\$ 7.19
\$41	\$ 41	\$ 7.62	\$ 41	\$ 7.61	\$ 41	\$ 7.60	\$ 41	\$ 7.59	\$ 41	\$ 7.37
\$42	\$ 42	\$ 7.81	\$ 42	\$ 7.80	\$ 42	\$ 7.79	\$ 42	\$ 7.78	\$ 42	\$ 7.55
\$43	\$ 43	\$ 8.00	\$ 43	\$ 7.99	\$ 43	\$ 7.98	\$ 43	\$ 7.97	\$ 43	\$ 7.73
\$44	\$ 44	\$ 8.18	\$ 44	\$ 8.17	\$ 44	\$ 8.16	\$ 44	\$ 8.15	\$ 44	\$ 7.91
\$45	\$ 45	\$ 8.37	\$ 45	\$ 8.36	\$ 45	\$ 8.35	\$ 45	\$ 8.34	\$ 45	\$ 8.09
\$46	\$ 46	\$ 8.55	\$ 46	\$ 8.54	\$ 46	\$ 8.53	\$ 46	\$ 8.52	\$ 46	\$ 8.27
\$47	\$ 47	\$ 8.74	\$ 47	\$ 8.73	\$ 47	\$ 8.72	\$ 47	\$ 8.71	\$ 47	\$ 8.45
\$48	\$ 48	\$ 8.92	\$ 48	\$ 8.91	\$ 48	\$ 8.90	\$ 48	\$ 8.89	\$ 48	\$ 8.63
\$49	\$ 49	\$ 9.11	\$ 49	\$ 9.10	\$ 49	\$ 9.09	\$ 49	\$ 9.08	\$ 49	\$ 8.81
\$50	\$ 50	\$ 9.29	\$ 50	\$ 9.28	\$ 50	\$ 9.27	\$ 50	\$ 9.26	\$ 50	\$ 8.99
\$51	\$ 51	\$ 9.48	\$ 51	\$ 9.47	\$ 51	\$ 9.46	\$ 51	\$ 9.45	\$ 51	\$ 9.17
\$52	\$ 52	\$ 9.66	\$ 52	\$ 9.65	\$ 52	\$ 9.64	\$ 52	\$ 9.63	\$ 52	\$ 9.35
\$53	\$ 53	\$ 9.85	\$ 53	\$ 9.84	\$ 53	\$ 9.83	\$ 53	\$ 9.82	\$ 53	\$ 9.53
\$54	\$ 54	\$ 10.03	\$ 54	\$ 10.02	\$ 54	\$ 10.01	\$ 54	\$ 10.00	\$ 54	\$ 9.71
\$55	\$ 55	\$ 10.22	\$ 55	\$ 10.21	\$ 55	\$ 10.20	\$ 55	\$ 10.19	\$ 55	\$ 9.89
\$56	\$ 56	\$ 10.40	\$ 56	\$ 10.39	\$ 56	\$ 10.38	\$ 56	\$ 10.37	\$ 56	\$ 10.07
\$57	\$ 57	\$ 10.59	\$ 57	\$ 10.58	\$ 57	\$ 10.57	\$ 57	\$ 10.56	\$ 57	\$ 10.25
\$58	\$ 58	\$ 10.77	\$ 58	\$ 10.76	\$ 58	\$ 10.75	\$ 58	\$ 10.74	\$ 58	\$ 10.43
\$59	\$ 59	\$ 10.96	\$ 59	\$ 10.95	\$ 59	\$ 10.94	\$ 59	\$ 10.93	\$ 59	\$ 10.61
\$60	\$ 60	\$ 11.14	\$ 60	\$ 11.13	\$ 60	\$ 11.12	\$ 60	\$ 11.11	\$ 60	\$ 10.79
\$61	\$ 61	\$ 11.33	\$ 61	\$ 11.32	\$ 61	\$ 11.31	\$ 61	\$ 11.30	\$ 61	\$ 10.97
\$62	\$ 62	\$ 11.51	\$ 62	\$ 11.50	\$ 62	\$ 11.49	\$ 62	\$ 11.48	\$ 62	\$ 11.15
\$63	\$ 63	\$ 11.70	\$ 63	\$ 11.69	\$ 63	\$ 11.68	\$ 63	\$ 11.67	\$ 63	\$ 11.33
\$64	\$ 64	\$ 11.88	\$ 64	\$ 11.87	\$ 64	\$ 11.86	\$ 64	\$ 11.85	\$ 64	\$ 11.51
\$65	\$ 65	\$ 12.07	\$ 65	\$ 12.06	\$ 65	\$ 12.05	\$ 65	\$ 12.04	\$ 65	\$ 11.69
\$66	\$ 66	\$ 12.25	\$ 66	\$ 12.24	\$ 66	\$ 12.23	\$ 66	\$ 12.22	\$ 66	\$ 11.87
\$67	\$ 67	\$ 12.44	\$ 67	\$ 12.43	\$ 67	\$ 12.42	\$ 67	\$ 12.41	\$ 67	\$ 12.05
\$68	\$ 68	\$ 12.62	\$ 68	\$ 12.61	\$ 68	\$ 12.60	\$ 68	\$ 12.59	\$ 68	\$ 12.23
\$69	\$ 69	\$ 12.81	\$ 69	\$ 12.80	\$ 69	\$ 12.79	\$ 69	\$ 12.78	\$ 69	\$ 12.41
\$70	\$ 70	\$ 13.00	\$ 70	\$ 12.99	\$ 70	\$ 12.98	\$ 70	\$ 12.97	\$ 70	\$ 12.59
\$71	\$ 71	\$ 13.18	\$ 71	\$ 13.17	\$ 71	\$ 13.16	\$ 71	\$ 13.15	\$ 71	\$ 12.77
\$72	\$ 72	\$ 13.37	\$ 72	\$ 13.36	\$ 72	\$ 13.35	\$ 72	\$ 13.34	\$ 72	\$ 12.95
\$73	\$ 73	\$ 13.55	\$ 73	\$ 13.54	\$ 73	\$ 13.53	\$ 73	\$ 13.52	\$ 73	\$ 13.13
\$74	\$ 74	\$ 13.74	\$ 74	\$ 13.73	\$ 74	\$ 13.72	\$ 74	\$ 13.71	\$ 74	\$ 13.31
\$75	\$ 75	\$ 13.92	\$ 75	\$ 13.91	\$ 75	\$ 13.90	\$ 75	\$ 13.89	\$ 75	\$ 13.49
\$76	\$ 76	\$ 14.11	\$ 76	\$ 14.10	\$ 76	\$ 14.09	\$ 76	\$ 14.08	\$ 76	\$ 13.67
\$77	\$ 77	\$ 14.29	\$ 77	\$ 14.28	\$ 77	\$ 14.27	\$ 77	\$ 14.26	\$ 77	\$ 13.85
\$78	\$ 78	\$ 14.48	\$ 78	\$ 14.47	\$ 78	\$ 14.46	\$ 78	\$ 14.45	\$ 78	\$ 14.03
\$79	\$ 79	\$ 14.66	\$ 79	\$ 14.65	\$ 79	\$ 14.64	\$ 79	\$ 14.63	\$ 79	\$ 14.21
\$80	\$ 80	\$ 14.85	\$ 80	\$ 14.84	\$ 80	\$ 14.83	\$ 80	\$ 14.82	\$ 80	\$ 14.39
\$81	\$ 81	\$ 15.03	\$ 81	\$ 15.02	\$ 81	\$ 15.01	\$ 81	\$ 15.00	\$ 81	\$ 14.57
\$82	\$ 82	\$ 15.22	\$ 82	\$ 15.21	\$ 82	\$ 15.20	\$ 82	\$ 15.19	\$ 82	\$ 14.75
\$83	\$ 83	\$ 15.40	\$ 83	\$ 15.39	\$ 83	\$ 15.38	\$ 83	\$ 15.37	\$ 83	\$ 14.93
\$84	\$ 84	\$ 15.59	\$ 84	\$ 15.58	\$ 84	\$ 15.57	\$ 84	\$ 15.56	\$ 84	\$ 15.11
\$85	\$ 85	\$ 15.77	\$ 85	\$ 15.76	\$ 85	\$ 15.75	\$ 85	\$ 15.74	\$ 85	\$ 15.29
\$86	\$ 86	\$ 15.96	\$ 86	\$ 15.95	\$ 86	\$ 15.94	\$ 86	\$ 15.93	\$ 86	\$ 15.47
\$87	\$ 87	\$ 16.14	\$ 87	\$ 16.13	\$ 87	\$ 16.12	\$ 87	\$ 16.11	\$ 87	\$ 15.65
\$88	\$ 88	\$ 16.33	\$ 88	\$ 16.32	\$ 88	\$ 16.31	\$ 88	\$ 16.30	\$ 88	\$ 15.83
\$89	\$ 89	\$ 16.51	\$ 89	\$ 16.50	\$ 89	\$ 16.49	\$ 89	\$ 16.48	\$ 89	\$ 16.01
\$90	\$ 90	\$ 16.70	\$ 90	\$ 16.69	\$ 90	\$ 16.68	\$ 90	\$ 16.67	\$ 90	\$ 16.19
\$91	\$ 91	\$ 16.88	\$ 91	\$ 16.87	\$ 91	\$ 16.86	\$ 91	\$ 16.85	\$ 91	\$ 16.37
\$92	\$ 92	\$ 17.07	\$ 92	\$ 17.06	\$ 92	\$ 17.05	\$ 92	\$ 17.04	\$ 92	\$ 16.55
\$93	\$ 93	\$ 17.25	\$ 93	\$ 17.24	\$ 93	\$ 17.23	\$ 93	\$ 17.22	\$ 93	\$ 16.73
\$94	\$ 94	\$ 17.44	\$ 94	\$ 17.43	\$ 94	\$ 17.42	\$ 94	\$ 17.41	\$ 94	\$ 16.91
\$95	\$ 95	\$ 17.62	\$ 95	\$ 17.61	\$ 95	\$ 17.60	\$ 95	\$ 17.59	\$ 95	\$ 17.09
\$96	\$ 96	\$ 17.81	\$ 96	\$ 17.80	\$ 96	\$ 17.79	\$ 96	\$ 17.78	\$ 96	\$ 17.27
\$97	\$ 97	\$ 18.00	\$ 97	\$ 17.99	\$ 97	\$ 17.98	\$ 97	\$ 17.97	\$ 97	\$ 17.45
\$98	\$ 98	\$ 18.18	\$ 98	\$ 18.17	\$ 98	\$ 18.16	\$ 98	\$ 18.15	\$ 98	\$ 17.63
\$99	\$ 99	\$ 18.37	\$ 99	\$ 18.36	\$ 99	\$ 18.35	\$ 99	\$ 18.34	\$ 99	\$ 17.81
\$100	\$ 100	\$ 18.55	\$ 100	\$ 18.54	\$ 100	\$ 18.53	\$ 100	\$ 18.52	\$ 100	\$ 17.99

Table B-10: Fuel cycle costs for plants with 12-day outages for the first 8 years with closed breeding, costs increased by 50%.

Breeding fuel cycle cost \$/GJ _{th}	12-month		18-month		24-month		30-month		36-month		42-month	
	initially	replenish	initially	replenish	initially	replenish	initially	replenish	initially	replenish	initially	replenish
4.0	0.11	1.00	0.09	0.78	0.07	0.72	0.05	0.68	0.04	0.64	0.03	0.60
6.0	0.40	2.50	0.31	2.41	0.21	2.30	0.16	2.18	0.10	2.06	0.07	1.95
8.0	0.88	5.00	0.65	4.92	0.43	4.74	0.30	4.56	0.19	4.38	0.12	4.20
10.0	1.36	7.50	0.92	7.41	0.60	7.23	0.43	7.05	0.28	6.87	0.18	6.69
12.0	1.84	10.00	1.19	9.92	0.78	9.74	0.56	9.56	0.36	9.38	0.24	9.20
14.0	2.32	12.50	1.46	12.41	0.96	12.23	0.74	12.05	0.48	11.87	0.32	11.69
16.0	2.80	15.00	1.73	14.92	1.14	14.74	0.92	14.56	0.66	14.38	0.44	14.20
18.0	3.28	17.50	2.00	17.41	1.32	17.23	1.10	17.05	0.84	16.87	0.56	16.69
20.0	3.76	20.00	2.27	19.92	1.50	19.74	1.28	19.56	0.96	19.38	0.68	19.20
22.0	4.24	22.50	2.54	22.41	1.68	22.23	1.46	22.05	1.12	21.87	0.80	21.69
24.0	4.72	25.00	2.81	24.92	1.86	24.74	1.64	24.56	1.30	24.38	0.92	24.20
26.0	5.20	27.50	3.09	27.41	2.04	27.23	1.82	27.05	1.48	26.87	1.04	26.69
28.0	5.68	30.00	3.36	29.92	2.22	29.74	2.00	29.56	1.66	29.38	1.16	29.20
30.0	6.16	32.50	3.64	31.92	2.40	31.74	2.18	31.56	1.84	31.38	1.28	31.20
32.0	6.64	35.00	3.91	34.92	2.58	34.74	2.36	34.56	2.02	34.38	1.40	34.20
34.0	7.12	37.50	4.19	36.92	2.76	36.74	2.54	36.56	2.20	36.38	1.52	36.20
36.0	7.60	40.00	4.46	38.92	2.94	38.74	2.72	38.56	2.38	38.38	1.64	38.20
38.0	8.08	42.50	4.74	40.92	3.12	40.74	2.90	40.56	2.56	40.38	1.76	40.20
40.0	8.56	45.00	5.01	42.92	3.30	42.74	3.08	42.56	2.74	42.38	1.88	42.20
42.0	9.04	47.50	5.29	44.92	3.48	44.74	3.26	44.56	2.92	44.38	2.00	44.20
44.0	9.52	50.00	5.56	46.92	3.66	46.74	3.44	46.56	3.10	46.38	2.12	46.20
46.0	10.00	52.50	5.84	48.92	3.84	48.74	3.62	48.56	3.28	48.38	2.24	48.20
48.0	10.48	55.00	6.11	50.92	4.02	50.74	3.80	50.56	3.46	50.38	2.36	50.20
50.0	10.96	57.50	6.39	52.92	4.20	52.74	3.98	52.56	3.64	52.38	2.48	52.20
52.0	11.44	60.00	6.66	54.92	4.38	54.74	4.16	54.56	3.82	54.38	2.60	54.20
54.0	11.92	62.50	6.94	56.92	4.56	56.74	4.34	56.56	4.00	56.38	2.72	56.20
56.0	12.40	65.00	7.21	58.92	4.74	58.74	4.52	58.56	4.18	58.38	2.84	58.20
58.0	12.88	67.50	7.49	60.92	4.92	60.74	4.70	60.56	4.36	60.38	2.96	60.20
60.0	13.36	70.00	7.76	62.92	5.10	62.74	4.88	62.56	4.54	62.38	3.08	62.20
62.0	13.84	72.50	8.04	64.92	5.28	64.74	5.06	64.56	4.72	64.38	3.20	64.20
64.0	14.32	75.00	8.31	66.92	5.46	66.74	5.24	66.56	4.90	66.38	3.32	66.20
66.0	14.80	77.50	8.59	68.92	5.64	68.74	5.42	68.56	5.08	68.38	3.44	68.20
68.0	15.28	80.00	8.86	70.92	5.82	70.74	5.60	70.56	5.26	70.38	3.56	70.20
70.0	15.76	82.50	9.14	72.92	6.00	72.74	5.78	72.56	5.44	72.38	3.68	72.20
72.0	16.24	85.00	9.41	74.92	6.18	74.74	5.96	74.56	5.62	74.38	3.80	74.20
74.0	16.72	87.50	9.69	76.92	6.36	76.74	6.14	76.56	5.80	76.38	3.92	76.20
76.0	17.20	90.00	9.96	78.92	6.54	78.74	6.32	78.56	5.98	78.38	4.04	78.20
78.0	17.68	92.50	10.24	80.92	6.72	80.74	6.50	80.56	6.16	80.38	4.16	80.20
80.0	18.16	95.00	10.51	82.92	6.90	82.74	6.68	82.56	6.34	82.38	4.28	82.20
82.0	18.64	97.50	10.79	84.92	7.08	84.74	6.86	84.56	6.52	84.38	4.40	84.20
84.0	19.12	100.00	11.06	86.92	7.26	86.74	7.04	86.56	6.70	86.38	4.52	86.20
86.0	19.60		11.34		7.44		7.22		6.88		4.64	
88.0	20.08		11.61		7.62		7.40		7.06		4.76	
90.0	20.56		11.89		7.80		7.58		7.24		4.88	
92.0	21.04		12.16		7.98		7.76		7.42		5.00	
94.0	21.52		12.44		8.16		7.94		7.60		5.12	
96.0	22.00		12.71		8.34		8.12		7.78		5.24	
98.0	22.48		12.99		8.52		8.30		7.96		5.36	
100.0	22.96		13.26		8.70		8.48		8.14		5.48	

Table B-43 Final cycle costs for plants with 30-day outage for the first 3 years with initial loading costs normalized by 2004

Electricity unit cost with 1% inflation	18-month cycle cost indicator		18-month cycle cost indicator		18-month cycle cost indicator		18-month cycle cost indicator		18-month cycle cost indicator	
	indicator	indicator	indicator	indicator	indicator	indicator	indicator	indicator	indicator	indicator
4.0	0.32	0.42	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
4.5	0.29	0.34	0.35	0.35	0.35	0.35	0.35	0.35	0.35	0.35
5.0	0.30	0.34	0.35	0.35	0.35	0.35	0.35	0.35	0.35	0.35
5.5	0.30	0.34	0.35	0.35	0.35	0.35	0.35	0.35	0.35	0.35
6.0	0.32	0.40	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
7.0	0.35	0.47	0.37	0.37	0.35	0.35	0.35	0.35	0.35	0.35
7.5	0.37	0.50	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
8.0	0.38	0.54	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
8.5	0.39	0.57	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
9.0	0.40	0.59	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
9.5	0.41	0.61	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35
10.0	0.42	0.63	0.38	0.38	0.35	0.35	0.35	0.35	0.35	0.35

Table B-10 Feed cycle costs for plants with 12-day outage for the first 3 years with replacement power costs increased to

$$30 \frac{\text{cents}}{\text{kWh}} \times \frac{1.05}{1.05 - 0.75}$$

	12 months	18 months	24 months	36 months	48 months	60 months	72 months	84 months
End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)	End-of-year fuel cost per cycle (\$/MWh)
1.0	8.32	7.88	8.32	8.76	9.20	9.64	10.08	10.52
1.5	9.33	7.87	7.87	8.31	8.75	9.19	9.63	10.07
2.0	9.34	7.88	7.88	8.32	8.76	9.20	9.64	10.08
2.5	9.35	7.89	7.89	8.33	8.77	9.21	9.65	10.09
3.0	9.36	7.90	7.90	8.34	8.78	9.22	9.66	10.10
3.5	9.37	7.91	7.91	8.35	8.79	9.23	9.67	10.11
4.0	9.38	7.92	7.92	8.36	8.80	9.24	9.68	10.12
4.5	9.39	7.93	7.93	8.37	8.81	9.25	9.69	10.13
5.0	9.40	7.94	7.94	8.38	8.82	9.26	9.70	10.14
5.5	9.41	7.95	7.95	8.39	8.83	9.27	9.71	10.15
6.0	9.42	7.96	7.96	8.40	8.84	9.28	9.72	10.16
6.5	9.43	7.97	7.97	8.41	8.85	9.29	9.73	10.17
7.0	9.44	7.98	7.98	8.42	8.86	9.30	9.74	10.18
7.5	9.45	7.99	7.99	8.43	8.87	9.31	9.75	10.19
8.0	9.46	8.00	8.00	8.44	8.88	9.32	9.76	10.20
8.5	9.47	8.01	8.01	8.45	8.89	9.33	9.77	10.21
9.0	9.48	8.02	8.02	8.46	8.90	9.34	9.78	10.22
9.5	9.49	8.03	8.03	8.47	8.91	9.35	9.79	10.23
10.0	9.50	8.04	8.04	8.48	8.92	9.36	9.80	10.24
10.5	9.51	8.05	8.05	8.49	8.93	9.37	9.81	10.25
11.0	9.52	8.06	8.06	8.50	8.94	9.38	9.82	10.26
11.5	9.53	8.07	8.07	8.51	8.95	9.39	9.83	10.27
12.0	9.54	8.08	8.08	8.52	8.96	9.40	9.84	10.28
12.5	9.55	8.09	8.09	8.53	8.97	9.41	9.85	10.29
13.0	9.56	8.10	8.10	8.54	8.98	9.42	9.86	10.30
13.5	9.57	8.11	8.11	8.55	8.99	9.43	9.87	10.31
14.0	9.58	8.12	8.12	8.56	9.00	9.44	9.88	10.32
14.5	9.59	8.13	8.13	8.57	9.01	9.45	9.89	10.33
15.0	9.60	8.14	8.14	8.58	9.02	9.46	9.90	10.34
15.5	9.61	8.15	8.15	8.59	9.03	9.47	9.91	10.35
16.0	9.62	8.16	8.16	8.60	9.04	9.48	9.92	10.36
16.5	9.63	8.17	8.17	8.61	9.05	9.49	9.93	10.37
17.0	9.64	8.18	8.18	8.62	9.06	9.50	9.94	10.38
17.5	9.65	8.19	8.19	8.63	9.07	9.51	9.95	10.39
18.0	9.66	8.20	8.20	8.64	9.08	9.52	9.96	10.40
18.5	9.67	8.21	8.21	8.65	9.09	9.53	9.97	10.41
19.0	9.68	8.22	8.22	8.66	9.10	9.54	9.98	10.42
19.5	9.69	8.23	8.23	8.67	9.11	9.55	9.99	10.43
20.0	9.70	8.24	8.24	8.68	9.12	9.56	10.00	10.44
20.5	9.71	8.25	8.25	8.69	9.13	9.57	10.01	10.45
21.0	9.72	8.26	8.26	8.70	9.14	9.58	10.02	10.46
21.5	9.73	8.27	8.27	8.71	9.15	9.59	10.03	10.47
22.0	9.74	8.28	8.28	8.72	9.16	9.60	10.04	10.48
22.5	9.75	8.29	8.29	8.73	9.17	9.61	10.05	10.49
23.0	9.76	8.30	8.30	8.74	9.18	9.62	10.06	10.50
23.5	9.77	8.31	8.31	8.75	9.19	9.63	10.07	10.51
24.0	9.78	8.32	8.32	8.76	9.20	9.64	10.08	10.52
24.5	9.79	8.33	8.33	8.77	9.21	9.65	10.09	10.53
25.0	9.80	8.34	8.34	8.78	9.22	9.66	10.10	10.54
25.5	9.81	8.35	8.35	8.79	9.23	9.67	10.11	10.55
26.0	9.82	8.36	8.36	8.80	9.24	9.68	10.12	10.56
26.5	9.83	8.37	8.37	8.81	9.25	9.69	10.13	10.57
27.0	9.84	8.38	8.38	8.82	9.26	9.70	10.14	10.58
27.5	9.85	8.39	8.39	8.83	9.27	9.71	10.15	10.59
28.0	9.86	8.40	8.40	8.84	9.28	9.72	10.16	10.60
28.5	9.87	8.41	8.41	8.85	9.29	9.73	10.17	10.61
29.0	9.88	8.42	8.42	8.86	9.30	9.74	10.18	10.62
29.5	9.89	8.43	8.43	8.87	9.31	9.75	10.19	10.63
30.0	9.90	8.44	8.44	8.88	9.32	9.76	10.20	10.64
30.5	9.91	8.45	8.45	8.89	9.33	9.77	10.21	10.65
31.0	9.92	8.46	8.46	8.90	9.34	9.78	10.22	10.66
31.5	9.93	8.47	8.47	8.91	9.35	9.79	10.23	10.67
32.0	9.94	8.48	8.48	8.92	9.36	9.80	10.24	10.68
32.5	9.95	8.49	8.49	8.93	9.37	9.81	10.25	10.69
33.0	9.96	8.50	8.50	8.94	9.38	9.82	10.26	10.70
33.5	9.97	8.51	8.51	8.95	9.39	9.83	10.27	10.71
34.0	9.98	8.52	8.52	8.96	9.40	9.84	10.28	10.72
34.5	9.99	8.53	8.53	8.97	9.41	9.85	10.29	10.73
35.0	10.00	8.54	8.54	8.98	9.42	9.86	10.30	10.74
35.5	10.01	8.55	8.55	8.99	9.43	9.87	10.31	10.75
36.0	10.02	8.56	8.56	9.00	9.44	9.88	10.32	10.76
36.5	10.03	8.57	8.57	9.01	9.45	9.89	10.33	10.77
37.0	10.04	8.58	8.58	9.02	9.46	9.90	10.34	10.78
37.5	10.05	8.59	8.59	9.03	9.47	9.91	10.35	10.79
38.0	10.06	8.60	8.60	9.04	9.48	9.92	10.36	10.80
38.5	10.07	8.61	8.61	9.05	9.49	9.93	10.37	10.81
39.0	10.08	8.62	8.62	9.06	9.50	9.94	10.38	10.82
39.5	10.09	8.63	8.63	9.07	9.51	9.95	10.39	10.83
40.0	10.10	8.64	8.64	9.08	9.52	9.96	10.40	10.84
40.5	10.11	8.65	8.65	9.09	9.53	9.97	10.41	10.85
41.0	10.12	8.66	8.66	9.10	9.54	9.98	10.42	10.86
41.5	10.13	8.67	8.67	9.11	9.55	9.99	10.43	10.87
42.0	10.14	8.68	8.68	9.12	9.56	10.00	10.44	10.88
42.5	10.15	8.69	8.69	9.13	9.57	10.01	10.45	10.89
43.0	10.16	8.70	8.70	9.14	9.58	10.02	10.46	10.90
43.5	10.17	8.71	8.71	9.15	9.59	10.03	10.47	10.91
44.0	10.18	8.72	8.72	9.16	9.60	10.04	10.48	10.92
44.5	10.19	8.73	8.73	9.17	9.61	10.05	10.49	10.93
45.0	10.20	8.74	8.74	9.18	9.62	10.06	10.50	10.94
45.5	10.21	8.75	8.75	9.19	9.63	10.07	10.51	10.95
46.0	10.22	8.76	8.76	9.20	9.64	10.08	10.52	10.96
46.5	10.23	8.77	8.77	9.21	9.65	10.09	10.53	10.97
47.0	10.24	8.78	8.78	9.22	9.66	10.10	10.54	10.98
47.5	10.25	8.79	8.79	9.23	9.67	10.11	10.55	10.99
48.0	10.26	8.80	8.80	9.24	9.68	10.12	10.56	11.00
48.5	10.27	8.81	8.81	9.25	9.69	10.13	10.57	11.01
49.0	10.28	8.82	8.82	9.26	9.70	10.14	10.58	11.02
49.5	10.29	8.83	8.83	9.27	9.71	10.15	10.59	11.03
50.0	10.30	8.84	8.84	9.28	9.72	10.16	10.60	11.04
50.5	10.31	8.85	8.85	9.29	9.73	10.17	10.61	11.05
51.0	10.32	8.86	8.86	9.30	9.74	10.18	10.62	11.06
51.5	10.33	8.87	8.87	9.31	9.75	10.19	10.63	11.07
52.0	10.34	8.88	8.88	9.32	9.76	10.20	10.64	11.08
52.5	10.35	8.89	8.89	9.33	9.77	10.21	10.65	11.09
53.0	10.36	8.90	8.90	9.34	9.78	10.22	10.66	11.10
53.5	10.37	8.91	8.91	9.35	9.79	10.23	10.67	11.11
54.0	10.38	8.92	8.92	9.36	9.80	10.24	10.68	11.12
54.5	10.39	8.93	8.93	9.37	9.81	10.25	10.69	11.13
55.0	10.40	8.94	8.94	9.38	9.82	10.26	10.70	11.14
55.5	10.41	8.95	8.95	9.39	9.83	10.27	10.71	11.15
56.0	10.42	8.96	8.96	9.40	9.84	10.28	10.72	11.16
56.5	10.43	8.97	8.97	9.41	9.85	10.29	10.73	11.17
57.0	10.44	8.98	8.98	9.42	9.86	10.30	10.74	11.18
57.5	10.45	8.99	8.99	9.43	9.87	10.31	10.75	11.19
58.0	10.46	9.00	9.00	9.44	9.88	10.32	10.76	11.20
58.5	10.47	9.01	9.01	9.45	9.89	10.33	10.77	11.21
59.0	10.48	9.02	9.02	9.46	9.90	10.34	10.78	11.22
59.5	10.49	9.03	9.03	9.47	9.91	10.35	10.79	11.23
60.0	10.50	9.04	9.04	9.48	9.92	10.36	10.80	11.24
60.5	10.51	9.05	9.05	9.49	9.93	10.37	10.81	11.25
61.0	10.52	9.06	9.06	9.50	9.94	10.38	10.82	11.26
61.5	10.53	9.07	9.07	9.51	9.95	10.39	10.83	11.27
62.0	10.54	9.08	9.08	9.52	9.96	10.40	10.84	11.28
62.5	10.55	9.09	9.09	9.53	9.97	10.41	10.85	11.29
63.0	10.56	9.10	9.10	9.54	9.98	10.42	10.86	11.30
63.5	10.57	9.11	9.11	9.55	9.99	10.43	10.87	11.31
64.0	10.58	9.12	9.12	9.56	10.00	10.44	10.88	11.32
64.5	10.59	9.13	9.13	9.57	10.01	10.45	10.89	11.33
65.0	10.60	9.14	9.14	9.58	10.02	10.46	10.90	11.34
65.5	10.61	9.15	9.15	9.59	10.03	10.47	10.91	11.35
66.0	10.62	9.16	9.16	9.60	10.04	10.48	10.92	11.36
66.5	10.63	9.17	9.17	9.61	10.05	10.49	10.93	11.37
67.0	10.64	9.18	9.18	9.62	10.06	10.50	10.94	11.38
67.5	10.65	9.19	9.19	9.63	10.07</			

Table E-36: End cycle costs for plants with 12-day cooling for the first 3 years with replacement, prices converted to

$$20 \frac{\text{cents}}{\text{kWh}} \cdot \frac{100}{100 - \text{eff}_c}$$

End cycle cost per kWh	12-month efficiency	18-month efficiency	24-month efficiency	30-month efficiency	36-month efficiency	48-month efficiency
4.0	0.40	0.34	0.30	0.26	0.24	0.22
5.0	0.47	0.40	0.35	0.30	0.28	0.26
6.0	0.51	0.43	0.37	0.32	0.30	0.28
8.0	0.57	0.48	0.41	0.35	0.33	0.31
10.0	0.64	0.53	0.45	0.39	0.37	0.35
12.0	0.70	0.57	0.49	0.42	0.40	0.38
14.0	0.76	0.62	0.53	0.45	0.43	0.41
16.0	0.80	0.67	0.57	0.49	0.47	0.45
18.0	0.85	0.72	0.61	0.52	0.50	0.48
20.0	0.89	0.77	0.65	0.55	0.53	0.51
22.0	0.93	0.81	0.69	0.58	0.56	0.54
24.0	0.97	0.85	0.73	0.61	0.59	0.57
26.0	0.99	0.89	0.77	0.64	0.62	0.60
28.0	1.00	0.90	0.79	0.66	0.64	0.62
30.0	1.00	0.91	0.80	0.67	0.65	0.63
32.0	1.00	0.91	0.81	0.68	0.66	0.64
34.0	1.00	0.92	0.82	0.69	0.67	0.65
36.0	1.00	0.92	0.83	0.70	0.68	0.66
38.0	1.00	0.93	0.84	0.71	0.69	0.67
40.0	1.00	0.93	0.85	0.72	0.70	0.68
42.0	1.00	0.94	0.86	0.73	0.71	0.69
44.0	1.00	0.94	0.87	0.74	0.72	0.70
46.0	1.00	0.95	0.88	0.75	0.73	0.71
48.0	1.00	0.95	0.89	0.76	0.74	0.72
50.0	1.00	0.96	0.90	0.77	0.75	0.73
52.0	1.00	0.96	0.91	0.78	0.76	0.74
54.0	1.00	0.97	0.92	0.79	0.77	0.75
56.0	1.00	0.97	0.93	0.80	0.78	0.76
58.0	1.00	0.98	0.94	0.81	0.79	0.77
60.0	1.00	0.98	0.95	0.82	0.80	0.78
62.0	1.00	0.99	0.96	0.83	0.81	0.79
64.0	1.00	0.99	0.97	0.84	0.82	0.80
66.0	1.00	0.99	0.98	0.85	0.83	0.81
68.0	1.00	1.00	0.99	0.86	0.84	0.82
70.0	1.00	1.00	1.00	0.87	0.85	0.83

Table 8.18 Fuel cycle costs for plants with 18-day outage for the first 5 years with replacement power costs decreased to $20 \frac{\text{cents}}{\text{kWh}}$ 10^7 kg

	9 months	18 months	24 months	30 months	36 months	42 months
fuel cycle cost	fuel cycle cost	fuel cycle cost	fuel cycle cost	fuel cycle cost	fuel cycle cost	fuel cycle cost
4.8	8.27	7.18	7.18	8.24	8.24	8.24
5.0	8.50	7.40	7.40	8.11	8.11	8.11
5.5	8.97	7.46	7.46	7.95	7.95	7.95
6.0	9.56	7.46	7.46	7.86	7.86	7.86
6.6	9.93	7.46	7.46	7.80	7.80	7.80
7.0	10.21	7.50	7.50	7.84	7.84	7.84
7.5	10.43	7.60	7.47	7.95	7.95	7.95
8.0	10.66	7.70	7.52	7.99	7.99	7.99
8.6	10.94	7.85	7.66	7.96	7.79	7.66
9.0	11.16	7.99	7.66	7.96	7.79	7.66
9.6	11.38	8.26	7.78	7.92	7.78	7.66
10.0	11.56	8.16	7.87	7.92	7.85	7.66

Table B-28 Fuel cycle costs for plants with 30-day outages for the first 3 years with replacement, power costs determined in

$$20 \frac{\text{cents}}{\text{MWh}} \frac{100}{100 - A_r}$$

Replacement costs, \$/yr	12-month fuel cycle cost/ MWh-yr	18-month fuel cycle cost/ MWh-yr	24-month fuel cycle cost/ MWh-yr	30-month fuel cycle cost/ MWh-yr	36-month fuel cycle cost/ MWh-yr	42-month fuel cycle cost/ MWh-yr
0.0	0.00	0.00	0.00	0.00	0.00	0.00
0.1	0.00	0.00	0.00	0.00	0.00	0.00
0.2	0.00	0.00	0.00	0.00	0.00	0.00
0.3	0.00	0.00	0.00	0.00	0.00	0.00
0.4	0.00	0.00	0.00	0.00	0.00	0.00
0.5	0.00	0.00	0.00	0.00	0.00	0.00
0.6	0.00	0.00	0.00	0.00	0.00	0.00
0.7	0.00	0.00	0.00	0.00	0.00	0.00
0.8	0.00	0.00	0.00	0.00	0.00	0.00
0.9	0.00	0.00	0.00	0.00	0.00	0.00
1.0	0.00	0.00	0.00	0.00	0.00	0.00
1.1	0.00	0.00	0.00	0.00	0.00	0.00
1.2	0.00	0.00	0.00	0.00	0.00	0.00
1.3	0.00	0.00	0.00	0.00	0.00	0.00
1.4	0.00	0.00	0.00	0.00	0.00	0.00
1.5	0.00	0.00	0.00	0.00	0.00	0.00
1.6	0.00	0.00	0.00	0.00	0.00	0.00
1.7	0.00	0.00	0.00	0.00	0.00	0.00
1.8	0.00	0.00	0.00	0.00	0.00	0.00
1.9	0.00	0.00	0.00	0.00	0.00	0.00
2.0	0.00	0.00	0.00	0.00	0.00	0.00

Table E-60 Fuel cycle costs for plants with 18-day except for the first 3 years with replacement prices also decreased in

$$1.1 \frac{\text{cents}}{\text{MWh}} \frac{1975-1980}{1980-1985}$$

Fuel Cycle Cost 1975 \$/MWh	18-month 1975 \$/MWh	18-month 1980 \$/MWh	18-month 1985 \$/MWh	18-month 1990 \$/MWh	18-month 1995 \$/MWh	18-month 2000 \$/MWh
4.0	8.00	7.88	7.81	8.03	8.16	8.28
5.0	8.80	7.48	7.37	8.11	8.24	8.36
6.0	9.60	7.30	7.19	7.95	8.08	8.20
7.0	10.40	7.12	7.01	7.80	7.93	8.05
8.0	11.20	6.94	6.83	7.64	7.77	7.89
9.0	12.00	6.76	6.65	7.49	7.62	7.74
10.0	12.80	6.58	6.47	7.33	7.46	7.58
11.0	13.60	6.40	6.29	7.18	7.31	7.43
12.0	14.40	6.22	6.11	7.03	7.16	7.28
13.0	15.20	6.04	5.93	6.87	7.01	7.13
14.0	16.00	5.86	5.75	6.72	6.86	6.98
15.0	16.80	5.68	5.57	6.56	6.71	6.83
16.0	17.60	5.50	5.39	6.41	6.56	6.68
17.0	18.40	5.32	5.21	6.25	6.41	6.53
18.0	19.20	5.14	5.03	6.10	6.26	6.38
19.0	20.00	4.96	4.85	5.94	6.11	6.23
20.0	20.80	4.78	4.67	5.79	5.96	6.08
21.0	21.60	4.60	4.49	5.63	5.81	5.93
22.0	22.40	4.42	4.31	5.48	5.66	5.78
23.0	23.20	4.24	4.13	5.32	5.51	5.63
24.0	24.00	4.06	3.95	5.17	5.36	5.48
25.0	24.80	3.88	3.77	5.01	5.21	5.33
26.0	25.60	3.70	3.59	4.86	5.06	5.18
27.0	26.40	3.52	3.41	4.70	4.91	5.03
28.0	27.20	3.34	3.23	4.55	4.76	4.88
29.0	28.00	3.16	3.05	4.39	4.61	4.73
30.0	28.80	2.98	2.87	4.24	4.46	4.58
31.0	29.60	2.80	2.69	4.08	4.31	4.43
32.0	30.40	2.62	2.51	3.93	4.16	4.28
33.0	31.20	2.44	2.33	3.77	4.01	4.13
34.0	32.00	2.26	2.15	3.62	3.86	3.98
35.0	32.80	2.08	1.97	3.46	3.71	3.83
36.0	33.60	1.90	1.79	3.31	3.56	3.68
37.0	34.40	1.72	1.61	3.15	3.41	3.53
38.0	35.20	1.54	1.43	3.00	3.26	3.38
39.0	36.00	1.36	1.25	2.84	3.11	3.23
40.0	36.80	1.18	1.07	2.69	2.96	3.08
41.0	37.60	1.00	0.89	2.53	2.81	2.93
42.0	38.40	0.82	0.71	2.38	2.66	2.78
43.0	39.20	0.64	0.53	2.22	2.51	2.63
44.0	40.00	0.46	0.35	2.07	2.36	2.48
45.0	40.80	0.28	0.17	1.91	2.21	2.33
46.0	41.60	0.10	-0.01	1.76	2.06	2.18
47.0	42.40	-0.08	-0.19	1.60	1.91	2.03
48.0	43.20	-0.26	-0.37	1.45	1.76	1.88
49.0	44.00	-0.44	-0.55	1.29	1.61	1.73
50.0	44.80	-0.62	-0.73	1.14	1.46	1.58
51.0	45.60	-0.80	-0.91	0.98	1.31	1.43
52.0	46.40	-0.98	-1.09	0.83	1.16	1.28
53.0	47.20	-1.16	-1.27	0.67	1.01	1.13
54.0	48.00	-1.34	-1.45	0.52	0.86	0.98
55.0	48.80	-1.52	-1.63	0.36	0.71	0.83
56.0	49.60	-1.70	-1.81	0.20	0.56	0.68
57.0	50.40	-1.88	-1.99	0.05	0.41	0.53
58.0	51.20	-2.06	-2.17	-0.11	0.26	0.38
59.0	52.00	-2.24	-2.35	-0.26	0.11	0.23
60.0	52.80	-2.42	-2.53	-0.41	-0.04	0.08
61.0	53.60	-2.60	-2.71	-0.57	-0.19	-0.07
62.0	54.40	-2.78	-2.89	-0.72	-0.34	-0.22
63.0	55.20	-2.96	-3.07	-0.88	-0.49	-0.37
64.0	56.00	-3.14	-3.25	-1.03	-0.64	-0.52
65.0	56.80	-3.32	-3.43	-1.19	-0.79	-0.67
66.0	57.60	-3.50	-3.61	-1.34	-0.94	-0.82
67.0	58.40	-3.68	-3.79	-1.50	-1.09	-0.97
68.0	59.20	-3.86	-3.97	-1.65	-1.24	-1.12
69.0	60.00	-4.04	-4.15	-1.81	-1.39	-1.27
70.0	60.80	-4.22	-4.33	-1.96	-1.54	-1.42
71.0	61.60	-4.40	-4.51	-2.12	-1.69	-1.57
72.0	62.40	-4.58	-4.69	-2.27	-1.84	-1.72
73.0	63.20	-4.76	-4.87	-2.43	-1.99	-1.87
74.0	64.00	-4.94	-5.05	-2.58	-2.14	-2.02
75.0	64.80	-5.12	-5.23	-2.74	-2.29	-2.17
76.0	65.60	-5.30	-5.41	-2.89	-2.44	-2.32
77.0	66.40	-5.48	-5.59	-3.05	-2.59	-2.47
78.0	67.20	-5.66	-5.77	-3.20	-2.74	-2.62
79.0	68.00	-5.84	-5.95	-3.36	-2.89	-2.77
80.0	68.80	-6.02	-6.13	-3.51	-3.04	-2.92
81.0	69.60	-6.20	-6.31	-3.67	-3.19	-3.07
82.0	70.40	-6.38	-6.49	-3.82	-3.34	-3.22
83.0	71.20	-6.56	-6.67	-3.98	-3.49	-3.37
84.0	72.00	-6.74	-6.85	-4.13	-3.64	-3.52
85.0	72.80	-6.92	-7.03	-4.29	-3.79	-3.67
86.0	73.60	-7.10	-7.21	-4.44	-3.94	-3.82
87.0	74.40	-7.28	-7.39	-4.60	-4.09	-3.97
88.0	75.20	-7.46	-7.57	-4.75	-4.24	-4.12
89.0	76.00	-7.64	-7.75	-4.91	-4.39	-4.27
90.0	76.80	-7.82	-7.93	-5.06	-4.54	-4.42
91.0	77.60	-8.00	-8.11	-5.22	-4.69	-4.57
92.0	78.40	-8.18	-8.29	-5.37	-4.84	-4.72
93.0	79.20	-8.36	-8.47	-5.53	-4.99	-4.87
94.0	80.00	-8.54	-8.65	-5.68	-5.14	-5.02
95.0	80.80	-8.72	-8.83	-5.84	-5.29	-5.17
96.0	81.60	-8.90	-9.01	-5.99	-5.44	-5.32
97.0	82.40	-9.08	-9.19	-6.15	-5.59	-5.47
98.0	83.20	-9.26	-9.37	-6.30	-5.74	-5.62
99.0	84.00	-9.44	-9.55	-6.46	-5.89	-5.77
100.0	84.80	-9.62	-9.73	-6.61	-6.04	-5.92

Table E-4) Fuel cycle costs for plants with 30-day outages for the first 3 years with replacement prices estimated as

$$15 \frac{\text{cents}}{\text{MWh}} \ln \frac{t}{t_0}$$

Investment cost \$/kW _{el}	12-month outage cost \$/MWh	18-month outage cost \$/MWh	24-month outage cost \$/MWh	30-month outage cost \$/MWh	36-month outage cost \$/MWh	42-month outage cost \$/MWh
4.0	0.62	1.60	1.73	1.86	1.98	2.08
6.0	0.49	1.19	1.29	1.38	1.46	1.52
8.0	0.40	1.04	1.10	1.16	1.22	1.26
10.0	0.36	0.96	1.00	1.05	1.09	1.12
12.0	0.33	0.89	0.93	0.97	1.01	1.04
15.0	0.27	0.73	0.76	0.80	0.83	0.86
18.0	0.23	0.64	0.67	0.70	0.73	0.75
20.0	0.21	0.60	0.62	0.65	0.67	0.69
25.0	0.16	0.45	0.47	0.49	0.51	0.53
30.0	0.13	0.37	0.38	0.40	0.41	0.42
40.0	0.09	0.25	0.26	0.27	0.28	0.29
50.0	0.07	0.19	0.20	0.21	0.22	0.23

Table B-66 Fuel-cycle costs for plants with 21-day outages for the first 3 years with dry-cask storage ends increased by 20%.

	10 months	16 months	24 months	36 months	48 months	60 months
Normalized Fuel Cycle Cost/Fuel Cycle Cost	Normalized Fuel Cycle Cost/Fuel Cycle Cost	Normalized Fuel Cycle Cost/Fuel Cycle Cost	Normalized Fuel Cycle Cost/Fuel Cycle Cost	Normalized Fuel Cycle Cost/Fuel Cycle Cost	Normalized Fuel Cycle Cost/Fuel Cycle Cost	Normalized Fuel Cycle Cost/Fuel Cycle Cost
100%	1.00	1.00	1.00	1.00	1.00	1.00
110%	1.01	1.01	1.01	1.01	1.01	1.01
120%	1.02	1.02	1.02	1.02	1.02	1.02
130%	1.03	1.03	1.03	1.03	1.03	1.03
140%	1.04	1.04	1.04	1.04	1.04	1.04
150%	1.05	1.05	1.05	1.05	1.05	1.05
160%	1.06	1.06	1.06	1.06	1.06	1.06
170%	1.07	1.07	1.07	1.07	1.07	1.07
180%	1.08	1.08	1.08	1.08	1.08	1.08
190%	1.09	1.09	1.09	1.09	1.09	1.09
200%	1.10	1.10	1.10	1.10	1.10	1.10
210%	1.11	1.11	1.11	1.11	1.11	1.11
220%	1.12	1.12	1.12	1.12	1.12	1.12
230%	1.13	1.13	1.13	1.13	1.13	1.13
240%	1.14	1.14	1.14	1.14	1.14	1.14
250%	1.15	1.15	1.15	1.15	1.15	1.15
260%	1.16	1.16	1.16	1.16	1.16	1.16
270%	1.17	1.17	1.17	1.17	1.17	1.17
280%	1.18	1.18	1.18	1.18	1.18	1.18
290%	1.19	1.19	1.19	1.19	1.19	1.19
300%	1.20	1.20	1.20	1.20	1.20	1.20
310%	1.21	1.21	1.21	1.21	1.21	1.21
320%	1.22	1.22	1.22	1.22	1.22	1.22
330%	1.23	1.23	1.23	1.23	1.23	1.23
340%	1.24	1.24	1.24	1.24	1.24	1.24
350%	1.25	1.25	1.25	1.25	1.25	1.25

Table B-63 Fuel cycle costs for plants with 30-day average for the first 3 years with dry-vent storage costs increased by 50%.

Estimated mGJ/L ¹	10 months Fuel Cycle Composite Subsidies	18 months Fuel Cycle Composite Subsidies	24 months Fuel Cycle Composite Subsidies	30 months Fuel Cycle Composite Subsidies	36 months Fuel Cycle Composite Subsidies	42 months Fuel Cycle Composite Subsidies
4.0	0.24	0.18	0.12	0.08	0.03	0.00
5.0	0.39	0.28	0.20	0.14	0.05	0.00
6.0	0.54	0.38	0.26	0.20	0.08	0.00
8.0	0.80	0.57	0.39	0.27	0.08	0.00
10.0	1.05	0.77	0.54	0.38	0.10	0.00
15.0	1.65	1.09	0.79	0.56	0.16	0.00
20.0	2.25	1.50	1.04	0.78	0.22	0.00
30.0	3.45	2.25	1.56	1.08	0.33	0.00
40.0	4.65	3.00	2.08	1.44	0.44	0.00
50.0	5.85	3.75	2.60	1.80	0.55	0.00
60.0	7.05	4.50	3.12	2.16	0.66	0.00
70.0	8.25	5.25	3.64	2.52	0.77	0.00
80.0	9.45	6.00	4.16	2.88	0.88	0.00
90.0	10.65	6.75	4.68	3.24	0.99	0.00
100.0	11.85	7.50	5.20	3.60	1.10	0.00
150.0	17.78	11.25	7.80	5.40	1.65	0.00

Table B-48. Paid cycle costs for plans with 13-day out-of-pocket for the first 3 years with day cash savings costs decreased by 10%.

	13 months annualized costs	18 months annualized costs	24 months annualized costs	36 months annualized costs	48 months annualized costs
40	\$ 41	1 00	1 00	\$ 04	\$ 04
50	\$ 40	1 16	1 16	\$ 04	\$ 04
55	\$ 40	1 16	1 16	1 00	\$ 00
60	\$ 40	1 16	1 00	1 00	\$ 00
65	\$ 40	1 16	1 00	1 00	\$ 00
70	\$ 41	1 00	1 00	1 00	\$ 00
75	\$ 40	1 00	1 00	1 00	\$ 00
80	\$ 40	\$ 00	1 11	1 00	\$ 00
85	\$ 40	\$ 00	1 00	1 00	\$ 00
90	\$ 40	\$ 00	1 00	1 00	\$ 00
95	\$ 40	\$ 00	\$ 00	1 00	\$ 00
100	\$ 40	\$ 00	\$ 00	1 00	\$ 00

Table B-46 Fuel cycle costs for plants with 10-day average for the first 5 years with dry unit storage costs decreased by 10%.

SW,¢/kWh	10 months Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost	18 months Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost	24 months Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost	30 months Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost	36 months Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost
4.4	0.12	0.13	0.11	0.09	0.08
5.0	0.10	0.11	0.09	0.06	0.05
5.6	0.10	0.11	0.09	0.06	0.05
6.0	0.10	0.10	0.08	0.06	0.05
6.6	0.10	0.10	0.08	0.06	0.05
7.0	0.10	0.10	0.08	0.06	0.05
7.6	0.10	0.10	0.08	0.06	0.05
8.0	0.10	0.10	0.08	0.06	0.05
8.6	0.10	0.10	0.08	0.06	0.05
9.0	0.10	0.10	0.08	0.06	0.05
9.6	0.10	0.10	0.08	0.06	0.05
10.0	0.10	0.10	0.08	0.06	0.05
10.6	0.10	0.10	0.08	0.06	0.05

Table E-7.1 Fuel cycle costs for plants with 20-day outages for the first 2 years with dry cask storage costs increased by 20%.

Enrichment Cycle Cost Fuel Cycle Cost Fuel Cycle Cost Fuel Cycle Cost Fuel Cycle Cost	14 months		16 months		18 months		20 months		24 months	
	initially,	midcycle,	initially,	midcycle,	initially,	midcycle,	initially,	midcycle,	initially,	midcycle,
4.0	0.00	0.25	0.28	0.53	0.55	0.80	0.81	1.06	1.31	1.56
4.5	0.00	0.26	0.29	0.49	0.49	0.74	0.74	0.99	1.24	1.49
5.0	0.00	0.28	0.30	0.50	0.50	0.75	0.75	1.00	1.25	1.50
5.5	0.00	0.29	0.31	0.51	0.51	0.76	0.76	1.01	1.26	1.51
6.0	0.00	0.30	0.32	0.52	0.52	0.77	0.77	1.02	1.27	1.52
7.0	0.00	0.36	0.38	0.58	0.58	0.83	0.83	1.08	1.33	1.58
7.5	0.00	0.40	0.42	0.62	0.62	0.87	0.87	1.12	1.37	1.62
8.0	0.00	0.43	0.45	0.65	0.65	0.90	0.90	1.15	1.40	1.65
8.5	0.00	0.46	0.48	0.68	0.68	0.93	0.93	1.18	1.43	1.68
9.0	0.00	0.49	0.51	0.71	0.71	0.96	0.96	1.21	1.46	1.71
9.5	0.00	0.52	0.54	0.74	0.74	0.99	0.99	1.24	1.49	1.74
10.0	0.00	0.55	0.57	0.77	0.77	1.02	1.02	1.27	1.52	1.77
10.5	0.00	0.58	0.60	0.80	0.80	1.05	1.05	1.30	1.55	1.80
11.0	0.00	0.61	0.63	0.83	0.83	1.08	1.08	1.33	1.58	1.83
11.5	0.00	0.64	0.66	0.86	0.86	1.11	1.11	1.36	1.61	1.86
12.0	0.00	0.67	0.69	0.89	0.89	1.14	1.14	1.39	1.64	1.89
12.5	0.00	0.70	0.72	0.92	0.92	1.17	1.17	1.42	1.67	1.92
13.0	0.00	0.73	0.75	0.95	0.95	1.20	1.20	1.45	1.70	1.95

Table E-77: Fuel cycle costs for plants with 30-day outages for the first 3 years with revised design for assessment

Investment cost with LWR	24-month fuel cycle availability	36-month fuel cycle availability	48-month fuel cycle availability	60-month fuel cycle availability	72-month fuel cycle availability	84-month fuel cycle availability
\$/Btu	\$/Btu	\$/Btu	\$/Btu	\$/Btu	\$/Btu	\$/Btu
0.0	0.20	0.18	0.15	0.13	0.11	0.09
0.0	0.20	0.14	0.09	0.05	0.03	0.02
0.0	0.20	0.11	0.06	0.03	0.01	0.00
0.0	0.20	0.03	0.01	0.00	0.00	0.00
0.0	0.20	0.00	0.00	0.00	0.00	0.00
0.0	0.15	0.11	0.06	0.03	0.01	0.00
0.0	0.14	0.03	0.01	0.00	0.00	0.00
0.0	0.20	0.08	0.03	0.01	0.00	0.00
0.0	0.20	0.03	0.01	0.00	0.00	0.00
0.0	0.20	0.01	0.00	0.00	0.00	0.00
0.0	0.15	0.03	0.01	0.00	0.00	0.00
0.0	0.11	0.00	0.00	0.00	0.00	0.00

Table 6-13: Road cycle times for plans with 30-day overlap for the first 3 years with revised Approval for construction.

with 1 st yr	12 months		24 months		36 months		48 months		60 months	
	months	percentage	months	percentage	months	percentage	months	percentage	months	percentage
48	0.00	0.41	0.01	0.03	0.03	0.03	0.04	0.04	0.05	0.05
60	0.04	0.36	0.06	0.40	0.40	0.40	0.04	0.04	0.05	0.05
96	0.05	0.11	0.25	0.03	0.03	0.03	0.03	0.03	0.05	0.05
48	0.04	0.24	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
60	0.05	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
96	0.04	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
72	0.04	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
48	0.04	0.04	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
60	0.05	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
96	0.04	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
48	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05
10.0	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.05	0.05

Table B-74. Fuel cycle costs for plants with 18-day savings for the first 8 years with fuel purchase interest rates decreased to 0%

Electricity generation capacity, MW	12-month fuel cycle cost with 18-day savings		18-month fuel cycle cost with 18-day savings		24-month fuel cycle cost with 18-day savings		36-month fuel cycle cost with 18-day savings		48-month fuel cycle cost with 18-day savings	
	mill/kWh	¢/kWh	mill/kWh	¢/kWh	mill/kWh	¢/kWh	mill/kWh	¢/kWh	mill/kWh	¢/kWh
4.0	8.28	2.52	7.88	2.41	7.48	2.31	7.08	2.21	6.68	2.11
8.0	8.27	2.46	7.87	2.40	7.47	2.30	7.07	2.20	6.67	2.10
16.0	8.26	2.39	7.86	2.37	7.46	2.28	7.06	2.18	6.66	2.09
32.0	8.24	2.36	7.84	2.35	7.44	2.26	7.04	2.16	6.64	2.08
64.0	8.23	2.33	7.83	2.32	7.43	2.24	7.03	2.14	6.63	2.07
128.0	8.20	2.30	7.80	2.29	7.40	2.21	7.00	2.11	6.60	2.04
256.0	8.18	2.27	7.78	2.26	7.38	2.19	6.98	2.09	6.58	2.02
512.0	8.16	2.24	7.76	2.23	7.36	2.17	6.96	2.07	6.56	2.00
1,024.0	8.14	2.21	7.74	2.20	7.34	2.14	6.94	2.04	6.54	1.97
2,048.0	8.12	2.18	7.72	2.17	7.32	2.12	6.92	2.02	6.52	1.95
4,096.0	8.10	2.15	7.70	2.14	7.30	2.10	6.90	2.00	6.50	1.93

Table 6.26 Fuel cycle costs for plants with 11-day outage for the first 2 years with fuel purchase contract rates decreased to 17%

with 11- day outage	10 months recovery	18 months recovery	24 months recovery	30 months recovery	36 months recovery	42 months recovery
4.0	8.14	7.81	7.48	7.15	6.82	6.50
4.5	8.11	7.78	7.45	7.12	6.79	6.47
5.0	8.07	7.74	7.41	7.08	6.75	6.43
5.5	8.04	7.71	7.38	7.05	6.72	6.40
6.0	8.01	7.68	7.35	7.02	6.69	6.37
6.5	7.97	7.64	7.31	6.98	6.65	6.33
7.0	7.94	7.61	7.28	6.95	6.62	6.30
7.5	7.91	7.58	7.25	6.92	6.59	6.27
8.0	7.87	7.54	7.21	6.88	6.55	6.23
8.5	7.84	7.51	7.18	6.85	6.52	6.20
9.0	7.81	7.48	7.15	6.82	6.49	6.17
9.5	7.77	7.44	7.11	6.78	6.45	6.13
10.0	7.74	7.41	7.08	6.75	6.42	6.10

Table E.19 Fuel cycle costs for plants with 10-day cooling for the first 3 years with fuel purchase values: rates increased in 20%

End-use plant type, Cool Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost/Fuel Cycle Cost	10-month		10-month		10-month		10-month		10-month	
	in dollars	in dollars	in dollars	in dollars	in dollars	in dollars	in dollars	in dollars	in dollars	in dollars
4.0	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
6.0	0.00	0.07	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
8.0	0.01	0.40	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00
10.0	0.01	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
12.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
14.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
16.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
18.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
20.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
22.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
24.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
26.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
28.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
30.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
32.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
34.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
36.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
38.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
40.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
42.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
44.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
46.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
48.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
50.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
52.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
54.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
56.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
58.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
60.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
62.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
64.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
66.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
68.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
70.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
72.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
74.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
76.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
78.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
80.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
82.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
84.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
86.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
88.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
90.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
92.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
94.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
96.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
98.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
100.0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00

Table 8-60 Fuel cycle costs for plants with 12-day outage for the first 5 years with fuel purchase interest rates increasing 5%.

Average Fuel Cycle Cost Fuel Cycle Cost Fuel Cycle Cost Fuel Cycle Cost Fuel Cycle Cost with 1% with 2% with 3% with 4% with 5%	12 months	24 months	36 months	48 months	60 months
	mill/kWh	mill/kWh	mill/kWh	mill/kWh	mill/kWh
6.0	0.10	0.20	0.30	0.40	0.50
6.5	0.10	0.21	0.31	0.41	0.51
7.0	0.10	0.21	0.32	0.42	0.52
7.5	0.10	0.21	0.32	0.43	0.53
8.0	0.10	0.21	0.33	0.43	0.54
8.5	0.10	0.22	0.33	0.44	0.54
9.0	0.10	0.22	0.34	0.44	0.55
9.5	0.10	0.22	0.34	0.45	0.55
10.0	0.10	0.23	0.35	0.45	0.56
10.5	0.10	0.23	0.35	0.46	0.56
11.0	0.10	0.23	0.36	0.46	0.57
11.5	0.10	0.24	0.36	0.47	0.57
12.0	0.10	0.24	0.37	0.47	0.58
12.5	0.10	0.24	0.37	0.48	0.58
13.0	0.10	0.25	0.38	0.48	0.59
13.5	0.10	0.25	0.38	0.49	0.59
14.0	0.10	0.25	0.39	0.49	0.60
14.5	0.10	0.26	0.39	0.50	0.60
15.0	0.10	0.26	0.40	0.50	0.61
15.5	0.10	0.26	0.40	0.51	0.61
16.0	0.10	0.27	0.41	0.51	0.62
16.5	0.10	0.27	0.41	0.52	0.62
17.0	0.10	0.27	0.42	0.52	0.63
17.5	0.10	0.28	0.42	0.53	0.63
18.0	0.10	0.28	0.43	0.53	0.64
18.5	0.10	0.28	0.43	0.54	0.64
19.0	0.10	0.29	0.44	0.54	0.65
19.5	0.10	0.29	0.44	0.55	0.65
20.0	0.10	0.29	0.45	0.55	0.66
20.5	0.10	0.30	0.45	0.56	0.66
21.0	0.10	0.30	0.46	0.56	0.67
21.5	0.10	0.30	0.46	0.57	0.67
22.0	0.10	0.31	0.47	0.57	0.68
22.5	0.10	0.31	0.47	0.58	0.68
23.0	0.10	0.31	0.48	0.58	0.69
23.5	0.10	0.32	0.48	0.59	0.69
24.0	0.10	0.32	0.49	0.59	0.70
24.5	0.10	0.32	0.49	0.60	0.70
25.0	0.10	0.33	0.50	0.60	0.71
25.5	0.10	0.33	0.50	0.61	0.71
26.0	0.10	0.33	0.51	0.61	0.72
26.5	0.10	0.34	0.51	0.62	0.72
27.0	0.10	0.34	0.52	0.62	0.73
27.5	0.10	0.34	0.52	0.63	0.73
28.0	0.10	0.35	0.53	0.63	0.74
28.5	0.10	0.35	0.53	0.64	0.74
29.0	0.10	0.35	0.54	0.64	0.75
29.5	0.10	0.36	0.54	0.65	0.75
30.0	0.10	0.36	0.55	0.65	0.76
30.5	0.10	0.36	0.55	0.66	0.76
31.0	0.10	0.37	0.56	0.66	0.77
31.5	0.10	0.37	0.56	0.67	0.77
32.0	0.10	0.37	0.57	0.67	0.78
32.5	0.10	0.38	0.57	0.68	0.78
33.0	0.10	0.38	0.58	0.68	0.79
33.5	0.10	0.38	0.58	0.69	0.79
34.0	0.10	0.39	0.59	0.69	0.80
34.5	0.10	0.39	0.59	0.70	0.80
35.0	0.10	0.39	0.60	0.70	0.81
35.5	0.10	0.40	0.60	0.71	0.81
36.0	0.10	0.40	0.61	0.71	0.82
36.5	0.10	0.40	0.61	0.72	0.82
37.0	0.10	0.41	0.62	0.72	0.83
37.5	0.10	0.41	0.62	0.73	0.83
38.0	0.10	0.41	0.63	0.73	0.84
38.5	0.10	0.42	0.63	0.74	0.84
39.0	0.10	0.42	0.64	0.74	0.85
39.5	0.10	0.42	0.64	0.75	0.85
40.0	0.10	0.43	0.65	0.75	0.86
40.5	0.10	0.43	0.65	0.76	0.86
41.0	0.10	0.43	0.66	0.76	0.87
41.5	0.10	0.44	0.66	0.77	0.87
42.0	0.10	0.44	0.67	0.77	0.88
42.5	0.10	0.44	0.67	0.78	0.88
43.0	0.10	0.45	0.68	0.78	0.89
43.5	0.10	0.45	0.68	0.79	0.89
44.0	0.10	0.45	0.69	0.79	0.90
44.5	0.10	0.46	0.69	0.80	0.90
45.0	0.10	0.46	0.70	0.80	0.91
45.5	0.10	0.46	0.70	0.81	0.91
46.0	0.10	0.47	0.71	0.81	0.92
46.5	0.10	0.47	0.71	0.82	0.92
47.0	0.10	0.47	0.72	0.82	0.93
47.5	0.10	0.48	0.72	0.83	0.93
48.0	0.10	0.48	0.73	0.83	0.94
48.5	0.10	0.48	0.73	0.84	0.94
49.0	0.10	0.49	0.74	0.84	0.95
49.5	0.10	0.49	0.74	0.85	0.95
50.0	0.10	0.49	0.75	0.85	0.96
50.5	0.10	0.50	0.75	0.86	0.96
51.0	0.10	0.50	0.76	0.86	0.97
51.5	0.10	0.50	0.76	0.87	0.97
52.0	0.10	0.51	0.77	0.87	0.98
52.5	0.10	0.51	0.77	0.88	0.98
53.0	0.10	0.51	0.78	0.88	0.99
53.5	0.10	0.52	0.78	0.89	0.99
54.0	0.10	0.52	0.79	0.89	1.00
54.5	0.10	0.52	0.79	0.90	1.00
55.0	0.10	0.53	0.80	0.90	1.01
55.5	0.10	0.53	0.80	0.91	1.01
56.0	0.10	0.53	0.81	0.91	1.02
56.5	0.10	0.54	0.81	0.92	1.02
57.0	0.10	0.54	0.82	0.92	1.03
57.5	0.10	0.54	0.82	0.93	1.03
58.0	0.10	0.55	0.83	0.93	1.04
58.5	0.10	0.55	0.83	0.94	1.04
59.0	0.10	0.55	0.84	0.94	1.05
59.5	0.10	0.56	0.84	0.95	1.05
60.0	0.10	0.56	0.85	0.95	1.06
60.5	0.10	0.56	0.85	0.96	1.06
61.0	0.10	0.57	0.86	0.96	1.07
61.5	0.10	0.57	0.86	0.97	1.07
62.0	0.10	0.57	0.87	0.97	1.08
62.5	0.10	0.58	0.87	0.98	1.08
63.0	0.10	0.58	0.88	0.98	1.09
63.5	0.10	0.58	0.88	0.99	1.09
64.0	0.10	0.59	0.89	0.99	1.10
64.5	0.10	0.59	0.89	1.00	1.10
65.0	0.10	0.59	0.90	1.00	1.11
65.5	0.10	0.60	0.90	1.01	1.11
66.0	0.10	0.60	0.91	1.01	1.12
66.5	0.10	0.60	0.91	1.02	1.12
67.0	0.10	0.61	0.92	1.02	1.13
67.5	0.10	0.61	0.92	1.03	1.13
68.0	0.10	0.61	0.93	1.03	1.14
68.5	0.10	0.62	0.93	1.04	1.14
69.0	0.10	0.62	0.94	1.04	1.15
69.5	0.10	0.62	0.94	1.05	1.15
70.0	0.10	0.63	0.95	1.05	1.16
70.5	0.10	0.63	0.95	1.06	1.16
71.0	0.10	0.63	0.96	1.06	1.17
71.5	0.10	0.64	0.96	1.07	1.17
72.0	0.10	0.64	0.97	1.07	1.18
72.5	0.10	0.64	0.97	1.08	1.18
73.0	0.10	0.65	0.98	1.08	1.19
73.5	0.10	0.65	0.98	1.09	1.19
74.0	0.10	0.65	0.99	1.09	1.20
74.5	0.10	0.66	0.99	1.10	1.20
75.0	0.10	0.66	1.00	1.10	1.21
75.5	0.10	0.66	1.00	1.11	1.21
76.0	0.10	0.67	1.01	1.11	1.22
76.5	0.10	0.67	1.01	1.12	1.22
77.0	0.10	0.67	1.02	1.12	1.23
77.5	0.10	0.68	1.02	1.13	1.23
78.0	0.10	0.68	1.03	1.13	1.24
78.5	0.10	0.68	1.03	1.14	1.24
79.0	0.10	0.69	1.04	1.14	1.25
79.5	0.10	0.69	1.04	1.15	1.25
80.0	0.10	0.69	1.05	1.15	1.26
80.5	0.10	0.70	1.05	1.16	1.26
81.0	0.10	0.70	1.06	1.16	1.27
81.5	0.10	0.70	1.06	1.17	1.27
82.0	0.10	0.71	1.07	1.17	1.28
82.5	0.10	0.71	1.07	1.18	1.28
83.0	0.10	0.71	1.08	1.18	1.29
83.5	0.10	0.72	1.08	1.19	1.29
84.0	0.10	0.72	1.09	1.19	1.30
84.5	0.10	0.72	1.09	1.20	1.30
85.0	0.10	0.73	1.10	1.20	1.31
85.5	0.10	0.73	1.10	1.21	1.31
86.0	0.10	0.73	1.11	1.21	1.32
86.5	0.10	0.74	1.11	1.22	1.32
87.0	0.10	0.74	1.12	1.22	1.33
87.5	0.10	0.74	1.12	1.23	1.33
88.0	0.10	0.75	1.13	1.23	1.34
88.5	0.10	0.75	1.13	1.24	1.34
89.0	0.10	0.75	1.14	1.24	1.35
89.5	0.10	0.76	1.14	1.25	1.35
90.0	0.10	0.76	1.15	1.25	1.36
90.5	0.10	0.76	1.15	1.26	1.36
91.0	0.10	0.77	1.16	1.26	1.37
91.5	0.10	0.77	1.16	1.27	1.37
92.0	0.10	0.77	1.17	1.27	1.38
92.5	0.10	0.78	1.17	1.28	1.38
93.0	0.10	0.78	1.18	1.28	1.39
93.5	0.10	0.78	1.18	1.29	1.39
94.0	0.10	0.79	1.19	1.29	1.40
94.5	0.10	0.79	1.19	1.30	1.40
95.0	0.10	0.79	1.20	1.30	1.41
95.5	0.10	0.80	1.20	1.31	1.41
96.0	0.10	0.80	1.21	1.31	1.42
96.5	0.10	0.80	1.21	1.32	1.42
97.0	0.10	0.81	1.22	1.32	1.43
97.5	0.10	0.81	1.22	1.33	1.43
98.0	0.10	0.81	1.23	1.33	1.44
98.5	0.10	0.82	1.23	1.34	1.44
99.0	0.10	0.82	1.24	1.34	1.45
99.5	0.10	0.82	1.24	1.35	1.45
100.0	0.10	0.83	1.25	1.35	1.46

Table 3.42 Fuel cycle costs for plants with 12-day outages for the first 3 years with fuel purchase interest rates increased to 10%.

Fuel cycle cost \$/MWh	All-nuclear		All-nuclear		All-nuclear		All-nuclear	
	Fuel Cycle Cost including interest	fuel cycle cost excluding interest	Fuel Cycle Cost including interest	fuel cycle cost excluding interest	Fuel Cycle Cost including interest	fuel cycle cost excluding interest	Fuel Cycle Cost including interest	fuel cycle cost excluding interest
4.0	1.54	1.31	1.44	1.21	n/a	n/a	n/a	n/a
5.0	1.58	1.33	1.48	1.23	n/a	n/a	n/a	n/a
6.0	1.73	1.40	1.53	1.26	0.27	0.27	0.26	0.26
8.0	1.97	1.46	1.66	1.46	0.46	0.46	0.46	0.46
9.0	1.93	1.50	1.64	1.44	0.46	0.46	0.47	0.47
10.0	1.95	1.71	1.64	1.38	0.50	0.50	0.50	0.50
11.0	1.93	1.87	1.63	1.33	0.71	0.71	0.72	0.72
12.0	1.93	1.94	1.63	1.35	0.70	0.70	0.72	0.72
13.0	1.93	2.00	1.63	1.39	0.70	0.70	0.73	0.73
14.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73
15.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73
16.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73
17.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73
18.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73
19.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73
20.0	1.93	1.98	1.64	1.41	0.71	0.71	0.73	0.73

Table 8.16a Fuel cycle costs for plants with 18-day outages for the first 3 years with fuel purchase interest rates assumed to 10%

Development with UPR	19 months Fuel Cycle Cost in \$/MWh	18 months Fuel Cycle Cost in \$/MWh	18 months Fuel Cycle Cost in \$/MWh	18 months Fuel Cycle Cost in \$/MWh	18 months Fuel Cycle Cost in \$/MWh	18 months Fuel Cycle Cost in \$/MWh
2.4	0.71	0.62	0.54	0.43	0.36	0.30
3.0	0.83	0.68	0.58	0.47	0.39	0.33
3.6	0.95	0.80	0.70	0.57	0.48	0.39
4.2	1.07	0.90	0.79	0.67	0.57	0.47
4.8	1.20	1.04	0.92	0.79	0.68	0.57
5.4	1.33	1.15	1.03	0.90	0.78	0.66
6.0	1.45	1.27	1.14	1.02	0.89	0.76
6.6	1.58	1.40	1.26	1.14	1.01	0.87
7.2	1.70	1.52	1.38	1.26	1.12	0.97
7.8	1.83	1.65	1.50	1.38	1.24	1.09
8.4	1.95	1.77	1.62	1.50	1.35	1.20
9.0	2.08	1.90	1.74	1.62	1.47	1.31
9.6	2.20	2.02	1.86	1.74	1.59	1.42
10.2	2.33	2.15	1.98	1.86	1.71	1.53
10.8	2.45	2.27	2.10	1.98	1.83	1.65
11.4	2.58	2.40	2.22	2.10	1.95	1.76
12.0	2.70	2.52	2.34	2.22	2.07	1.87
12.6	2.83	2.65	2.46	2.34	2.19	1.99
13.2	2.95	2.77	2.58	2.46	2.31	2.11
13.8	3.08	2.90	2.70	2.58	2.43	2.23
14.4	3.20	3.02	2.82	2.70	2.55	2.35
15.0	3.33	3.15	2.94	2.82	2.67	2.47
15.6	3.45	3.27	3.06	2.94	2.79	2.59
16.2	3.58	3.40	3.18	3.06	2.91	2.71
16.8	3.70	3.52	3.30	3.18	3.03	2.83
17.4	3.83	3.65	3.42	3.30	3.15	2.95
18.0	3.95	3.77	3.54	3.42	3.27	3.07
18.6	4.08	3.90	3.66	3.54	3.39	3.19
19.2	4.20	4.02	3.78	3.66	3.51	3.31
19.8	4.33	4.15	3.90	3.78	3.63	3.43
20.4	4.45	4.27	4.02	3.90	3.75	3.55
21.0	4.58	4.40	4.14	4.02	3.87	3.67
21.6	4.70	4.52	4.26	4.14	3.99	3.79
22.2	4.83	4.65	4.38	4.26	4.11	3.91
22.8	4.95	4.77	4.50	4.38	4.23	4.03
23.4	5.08	4.90	4.62	4.50	4.35	4.15
24.0	5.20	5.02	4.74	4.62	4.47	4.27
24.6	5.33	5.15	4.86	4.74	4.59	4.39
25.2	5.45	5.27	4.98	4.86	4.71	4.51
25.8	5.58	5.40	5.10	4.98	4.83	4.63
26.4	5.70	5.52	5.22	5.10	4.95	4.75
27.0	5.83	5.65	5.34	5.22	5.07	4.87
27.6	5.95	5.77	5.46	5.34	5.19	4.99
28.2	6.08	5.90	5.58	5.46	5.31	5.11
28.8	6.20	6.02	5.70	5.58	5.43	5.23
29.4	6.33	6.15	5.82	5.70	5.55	5.35
30.0	6.45	6.27	5.94	5.82	5.67	5.47
30.6	6.58	6.40	6.06	5.94	5.79	5.59
31.2	6.70	6.52	6.18	6.06	5.91	5.71
31.8	6.83	6.65	6.30	6.18	6.03	5.83
32.4	6.95	6.77	6.42	6.30	6.15	5.95
33.0	7.08	6.90	6.54	6.42	6.27	6.07
33.6	7.20	7.02	6.66	6.54	6.39	6.19
34.2	7.33	7.15	6.78	6.66	6.51	6.31
34.8	7.45	7.27	6.90	6.78	6.63	6.43
35.4	7.58	7.40	7.02	6.90	6.75	6.55
36.0	7.70	7.52	7.14	7.02	6.87	6.67
36.6	7.83	7.65	7.26	7.14	6.99	6.79
37.2	7.95	7.77	7.38	7.26	7.11	6.91
37.8	8.08	7.90	7.50	7.38	7.23	7.03
38.4	8.20	8.02	7.62	7.50	7.35	7.15
39.0	8.33	8.15	7.74	7.62	7.47	7.27
39.6	8.45	8.27	7.86	7.74	7.59	7.39
40.2	8.58	8.40	7.98	7.86	7.71	7.51
40.8	8.70	8.52	8.10	7.98	7.83	7.63
41.4	8.83	8.65	8.22	8.10	7.95	7.75
42.0	8.95	8.77	8.34	8.22	8.07	7.87
42.6	9.08	8.90	8.46	8.34	8.19	7.99
43.2	9.20	9.02	8.58	8.46	8.31	8.11
43.8	9.33	9.15	8.70	8.58	8.43	8.23
44.4	9.45	9.27	8.82	8.70	8.55	8.35
45.0	9.58	9.40	8.94	8.82	8.67	8.47
45.6	9.70	9.52	9.06	8.94	8.79	8.59
46.2	9.83	9.65	9.18	9.06	8.91	8.71
46.8	9.95	9.77	9.30	9.18	9.03	8.83
47.4	10.08	9.90	9.42	9.30	9.15	8.95
48.0	10.20	10.02	9.54	9.42	9.27	9.07
48.6	10.33	10.15	9.66	9.54	9.39	9.19
49.2	10.45	10.27	9.78	9.66	9.51	9.31
49.8	10.58	10.40	9.90	9.78	9.63	9.43
50.4	10.70	10.52	10.02	9.90	9.75	9.55
51.0	10.83	10.65	10.14	10.02	9.87	9.67
51.6	10.95	10.77	10.26	10.14	9.99	9.79
52.2	11.08	10.90	10.38	10.26	10.11	9.91
52.8	11.20	11.02	10.50	10.38	10.23	10.03
53.4	11.33	11.15	10.62	10.50	10.35	10.15
54.0	11.45	11.27	10.74	10.62	10.47	10.27
54.6	11.58	11.40	10.86	10.74	10.59	10.39
55.2	11.70	11.52	10.98	10.86	10.71	10.51
55.8	11.83	11.65	11.10	10.98	10.83	10.63
56.4	11.95	11.77	11.22	11.10	10.95	10.75
57.0	12.08	11.90	11.34	11.22	11.07	10.87
57.6	12.20	12.02	11.46	11.34	11.19	10.99
58.2	12.33	12.15	11.58	11.46	11.31	11.11
58.8	12.45	12.27	11.70	11.58	11.43	11.23
59.4	12.58	12.40	11.82	11.70	11.55	11.35
60.0	12.70	12.52	11.94	11.82	11.67	11.47
60.6	12.83	12.65	12.06	11.94	11.79	11.59
61.2	12.95	12.77	12.18	12.06	11.91	11.71
61.8	13.08	12.90	12.30	12.18	12.03	11.83
62.4	13.20	13.02	12.42	12.30	12.15	11.95
63.0	13.33	13.15	12.54	12.42	12.27	12.07
63.6	13.45	13.27	12.66	12.54	12.39	12.19
64.2	13.58	13.40	12.78	12.66	12.51	12.31
64.8	13.70	13.52	12.90	12.78	12.63	12.43
65.4	13.83	13.65	13.02	12.90	12.75	12.55
66.0	13.95	13.77	13.14	13.02	12.87	12.67
66.6	14.08	13.90	13.26	13.14	12.99	12.79
67.2	14.20	14.02	13.38	13.26	13.11	12.91
67.8	14.33	14.15	13.50	13.38	13.23	13.03
68.4	14.45	14.27	13.62	13.50	13.35	13.15
69.0	14.58	14.40	13.74	13.62	13.47	13.27
69.6	14.70	14.52	13.86	13.74	13.59	13.39
70.2	14.83	14.65	13.98	13.86	13.71	13.51
70.8	14.95	14.77	14.10	13.98	13.83	13.63
71.4	15.08	14.90	14.22	14.10	13.95	13.75
72.0	15.20	15.02	14.34	14.22	14.07	13.87
72.6	15.33	15.15	14.46	14.34	14.19	13.99
73.2	15.45	15.27	14.58	14.46	14.31	14.11
73.8	15.58	15.40	14.70	14.58	14.43	14.23
74.4	15.70	15.52	14.82	14.70	14.55	14.35
75.0	15.83	15.65	14.94	14.82	14.67	14.47
75.6	15.95	15.77	15.06	14.94	14.79	14.59
76.2	16.08	15.90	15.18	15.06	14.91	14.71
76.8	16.20	16.02	15.30	15.18	15.03	14.83
77.4	16.33	16.15	15.42	15.30	15.15	14.95
78.0	16.45	16.27	15.54	15.42	15.27	15.07
78.6	16.58	16.40	15.66	15.54	15.39	15.19
79.2	16.70	16.52	15.78	15.66	15.51	15.31
79.8	16.83	16.65	15.90	15.78	15.63	15.43
80.4	16.95	16.77	16.02	15.90	15.75	15.55
81.0	17.08	16.90	16.14	16.02	15.87	15.67
81.6	17.20	17.02	16.26	16.14	15.99	15.79
82.2	17.33	17.15	16.38	16.26	16.11	15.91
82.8	17.45	17.27	16.50	16.38	16.23	16.03
83.4	17.58	17.40	16.62	16.50	16.35	16.15
84.0	17.70	17.52	16.74	16.62	16.47	16.27
84.6	17.83	17.65	16.86	16.74	16.59	16.39
85.2	17.95	17.77	16.98	16.86	16.71	16.51
85.8	18.08	17.90	17.10	16.98	16.83	16.63
86.4	18.20	18.02	17.22	17.10	16.95	16.75
87.0	18.33	18.15	17.34	17.22	17.07	16.87
87.6	18.45	18.27	17.46	17.34	17.19	16.99
88.2	18.58	18.40	17.58	17.46	17.31	17.11
88.8	18.70	18.52	17.70	17.58	17.43	17.23
89.4	18.83	18.65	17.82	17.70	17.55	17.35
90.0	18.95	18.77	17.94	17.82	17.67	17.47
90.6	19.08	18.90	18.06	17.94	17.79	17.59
91.2	19.20	19.02	18.18	18.06	17.91	17.71
91.8	19.33	19.15	18.30	18.18	18.03	17.83
92.4	19.45	19.27	18.42	18.30	18.15	17.95
93.0	19.58	19.40	18.54	18.42	18.27	18.07
93.6	19.70	19.52	18.66	18.54	18.39	18.19
94.2	19.83	19.65	18.78	18.66	18.51	18.31
94.8	19.95	19.77	18.90	18.78	18.63	18.43
95.4	20.08	19.90	19.02	18.90	18.75	18.55
96.0	20.20	20.02	19.14	19.02	18.87	18.67
96.6	20.33	20.15	19.26	19.14	18.99	18.79
97.2	20.45	20.27	19.38	19.26	19.11	18.91
97.8	20.58	20.40	19.50	19.38	19.23	19.03
98.4	20.70	20.52	19.62	19.50	19.35	19.15
99.0	20.83	20.65	19.74	19.62	19.47	19.27
99.6	20.95	20.77	19.86	19.74	19.59	19.39
100.2	21.08	20.90	19.98	19.86	19.71	19.51
100.8	21.20	21.02	20.10	19.98	19.83	19.63
101.4	21.33	21.15	20.22	20.10	19.95	19.75
102.0	21.45	21.27	20.34	20.22	20.07	19.87
102.6	21.58	21.40	20.46	20.34	20.19	19.99
10						

Table 2-36 Fuel cycle costs for plants with 15-day outages for the first 3 years with fuel purchase interest rates normalized to 12%.

Normalized fuel cycle costs, \$/MWh	Quarter		Summer		Winter		Midwinter		2d monthly		12 monthly	
	availability,	costs/MWh	availability,	costs/MWh	availability,	costs/MWh	availability,	costs/MWh	availability,	costs/MWh	availability,	costs/MWh
4.0	9.23	9.74	9.23	9.23	9.23	9.23	9.23	9.23	9.23	9.23	9.23	9.23
8.0	9.48	9.74	9.73	9.73	9.73	9.73	9.73	9.73	9.73	9.73	9.73	9.73
12.0	9.66	9.89	9.89	9.89	9.89	9.89	9.89	9.89	9.89	9.89	9.89	9.89
16.0	9.86	9.95	9.95	9.95	9.95	9.95	9.95	9.95	9.95	9.95	9.95	9.95
20.0	10.07	9.94	9.94	9.94	9.94	9.94	9.94	9.94	9.94	9.94	9.94	9.94
25.0	10.37	9.88	9.88	9.88	9.88	9.88	9.88	9.88	9.88	9.88	9.88	9.88
30.0	10.69	9.80	9.80	9.80	9.80	9.80	9.80	9.80	9.80	9.80	9.80	9.80
35.0	11.03	9.69	9.69	9.69	9.69	9.69	9.69	9.69	9.69	9.69	9.69	9.69
40.0	11.34	9.61	9.61	9.61	9.61	9.61	9.61	9.61	9.61	9.61	9.61	9.61
45.0	11.61	9.52	9.52	9.52	9.52	9.52	9.52	9.52	9.52	9.52	9.52	9.52
50.0	11.83	9.43	9.43	9.43	9.43	9.43	9.43	9.43	9.43	9.43	9.43	9.43
55.0	12.06	9.34	9.34	9.34	9.34	9.34	9.34	9.34	9.34	9.34	9.34	9.34
60.0	12.26	9.25	9.25	9.25	9.25	9.25	9.25	9.25	9.25	9.25	9.25	9.25

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I certify that I have read this study and that in my opinion it conforms to acceptable standards of scholarly presentation and is fully adequate, in scope and quality, as a dissertation for the degree of Doctor of Philosophy.


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